

PERFORMANCE AND NO_x MODELLING IN A
DIRECT INJECTION STRATIFIED CHARGE ENGINE

by

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Submitted to the Department of Mechanical Engineering on April 25, 1978
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ABSTRACT

A model has been developed to predict the performance and NO_x emission of the Texaco stratified charge engine. This complete engine cycle program starts from engine geometry, valve and fuel injection timing, fuel characteristics and operating conditions and includes the following phases: valve overlap, intake, compression, combustion, expansion and exhaust.

The fuel mixing process is described by a jet mixing model and the equations are solved in a cylindrical coordinate system with a non-uniform pressure field. The jet shape changes were calculated for the jet impingement effect against a solid wall. The air motion inside the cylinder is determined by a detailed model to specify the field for the fuel jet.

During combustion fuel jet is divided into many elements and the combustion process of each element is analyzed as a mixing process between the jet and surrounding air, entrainment into a flame front and subsequent combustion.

For heat transfer the walls of the combustion chamber are divided into five regions; intake valve, exhaust valve, cylinder head, cylinder wall and piston top. Each region is assumed to have a different temperature and different gas velocity.

Nitric oxide emissions are calculated by using the extended Zel'dovich kinetic scheme, with the steady state assumption for the N concentration and equilibrium values used for H, O, O₂ and OH concentrations.

The model computes combustion rates, heat transfer and NO_x based on the same jet mixing assumptions without appeal to separate mixing processes at each stage.

Comparison of the model prediction with the available experimental data shows reasonably good agreement.

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SYMBOLS

A	= heat transfer area
Bore	= cylinder bore diameter
b	= jet radius in free jet
b_c	= jet radius when contacting with wall
C_p	= specific heat at constant pressure
E	= internal energy
H	= specific enthalpy
h	= distance from cylinder head to piston top
L_{cnr}	= length of connecting rod
M	= mass
N	= engine speed
Nu	= Nusselt number
P	= pressure
Q	= heat transfer to system
R	= radial distance of jet location
R_c	= radius of piston cup
Re	= Reynolds number
R_g	= gas constant
R_p	= radius of piston
R_{cr}	= radius of crank
s	= distance along the jet trajectory
S_e	= plume surface area
T	= temperature
u	= jet velocity

u_e	= turbulent eddy entrainment velocity
V	= volume
V_c	= piston cup volume
v_i	= parallel component of cross flow to u
v_n	= normal component of cross flow to u
v_r	= radial component of jet (swirl) velocity
v_z	= vertical component of jet (swirl) velocity
w	= angular velocity of jet (swirl)
W	= work done by system
X_f	= mass fraction of fuel in jet
Z	= axial distance of jet location
α	= entrainment parameter for the parallel flow
β	= entrainment parameter for the normal flow
ρ	= density
ϕ	= equivalence ratio
θ	= tangential component of jet location
θ_i	= fuel injection timing
θ_j	= jet contacting angle with wall (see Fig. 4)
θ_{cr}	= crank angle (0 at top dead center)
λ	= Taylor microscale
t_c	= characteristic reaction time for the microscale

Subscripts

i = element number i

in = inflow

out = outflow

e = entrained gas in the plume

b = burned gas in the plume

u = unburned gas in the plume

∞ = the gas surrounding the jet

I Introduction

The name, Texaco Controlled Combustion System (TCCS) is used to describe a spark ignited, direct injection, stratified charge engine. The combustion chamber is a deep cup in the piston; relatively higher air swirl is used. This engine may be thought of as a cross between the homogeneous charge, spark-ignition gasoline engine, and the heterogeneous charge, compression-ignition diesel engine. However, since combustion timing is controlled by fuel injection rates; the combustion process more nearly approximates that of an open chamber diesel engine. This engine concept appears to have the well controlled, soft combustion of the spark-ignition engine and, thereby, the lightweight structure of the gasoline engine. The TCCS concept also demonstrates excellent fuel economy, broad fuel tolerance, (multi-fuel capability) and relatively low emissions. The basic conceptual details behind the Texaco Controlled Combustion System are described below while additional hardware details can be found in the references on the TCCS engine (1-4).

TCCS Engine Description

The Texaco Controlled Combustion System, as illustrated in Fig. 1, requires coordination of air swirl, fuel-injection and positive ignition. The high air swirl is obtained from a shrouded inlet valve and is amplified during compression by being forced into a deep narrow

combustion chamber. The combustion chamber is essentially a cup having a cylindrical upper section with toroidal bottom cast into the head of the piston. The diameter of the cup is approximately one half of the cylinder diameter.

The high pressure injection system is based on standard diesel practice and uses a special version of a standard Roosa Master Pencil Nozzle. The distinguishing feature of this nozzle is a special flat seat and a single-hole orifice instead of the more usual conical seating, multi-hole sac-tip design. Valve opening pressure is usually set at 1500-2000 psi. For full load, fuel injection duration corresponds approximately to the time for one air swirl and the overall fuel-air ratio is near stoichiometric. At lower loads, obtained by decreased fuel injection duration and quantity, the operation is lean of stoichiometric and over all air to fuel ratio approaches 100:1 at idle conditions.

The usual diesel engine problems of long ignition delay, high rates of pressure rise and high peak pressures with low cetane fuels are avoided in TCCS operation by providing a positive ignition source. The Texaco Ignition System (TTIS) is a high energy, multi-spark unit with controlled duration. The ignition is triggered near the start of injection and continues through part or all of the injection process. The problems of spontaneous ignition and octane requirement associated with conventional gasoline engines is eliminated with TCCS since the residence time of combustible fuel-air mixtures is extremely short.

The TCCS mode of operation thus results in unique characteristics;

high part-load thermal efficiency at lean mixtures and inherently low hydrocarbon and carbon monoxide emissions resulting from excess air operation and controlled combustion rates. In addition, with the high pressure injection system, a wide range of fuel volatility can be tolerated. High compression ratio and/or inlet super charging can be used to produce good operation and performance on low cost fuels. These characteristics, in addition to quick warm-up and excellent driveability are significant factors in achieving an automotive engine with good performance and low exhaust emissions.

The purpose of the research work to be described in the following pages has been to develop a model to predict the performance of the TCCS, stratified charge engine given the engine geometry, operating parameters and the fuel properties. Once the model is shown to be effective in predicting the performance and NO_x , it can then be used as a design tool. With the brief description of the geometry and the mode of operation of the engine given above, we will now proceed to a discussion of the model.

II. Direct Injection Engine Simulation Model

1. Background

In the direct fuel injection engine, a distribution of temperature and equivalence ratio exists inside the combustion chamber. Since formation of NO_x is very much dependent on the local equivalence ratio and temperature, the key problem for this engine simulation is to define the spacial and temporal distribution of these parameters.

Early diesel engine combustion models include work by Lyn (6) and he developed an empirical calculation of the heat release rate by using triangles to simulate mixing and combustion of successive burned elements. Shahed, et. al. (7) integrated this idea with assumptions that have been widely used in spark ignition engine models (8,9) to compute NO_x . In this model, the fuel is assumed to mix with a stoichiometric amount of air before combustion and the mixed gas is divided into many packaged elements which are not mixing with each other. The temperature distribution inside the combustion chamber was explained by the different combustion time of each element. Bastress (34) took into consideration the distribution of equivalence ratio inside the combustion chamber, but this model is not based on physical mixing and combustion processes.

Following this work much effort was placed on developing physical arguments to compute the heat release rate proposed by Lyn. Shipinski (10), Whitehouse (11) and Bracco (12) have explained this delay by using fuel droplet evaporation models. But it is apparent that the combustion

process in direct injection engines cannot be predicted only by evaporation time.

Spray formation and mixing in engines was studied using continuum models by Adler (13) and Rife (14). Rife concludes that the motion of the fuel jet can be satisfactorily analyzed with such a model, but this model was not integrated into a combustion calculation.

Hiroyasu (15) made a complete heterogeneous mixture combustion model by assuming a simple cone shaped spray model and a more extensive jet mixing model, which included the effects of cross flow and jet tip shape, was developed by Chiu (16). These models do not include any adjustments of the fuel jet on the wall of the combustion.

Much of the work on heterogeneous combustion is based on gas turbine engine models. Stochastic techniques appear to be a powerful method (17, 18) for including the mixing phenomena in a statistical way. Further, the mixing rates have a physical basis. However, the models lack the geometric detail required for design and consequently have somewhat limited utility. In addition, these models require an enormous computing time in the case of reciprocating engines because of the way the combustion chamber air motion changes with crank angle. It is also possible that air motion inside the reciprocating engine is complicated enough to require more than a single mixing parameter.

In previous work, a model of the TCCS engine was developed by Jain (19). In our first extension of this model to compute NO_x , the

combustion chamber is divided into two areas; one a hot burned gas area, the other cold air. Each zone was considered to have uniform equivalence ratio and temperature. NO_x was calculated by using extended Zel'dovich equations. Values for the (NO_x) concentration obtained from this calculation are very low and this result was assumed to be due to the following reasons:

- a) During the rapid combustion process, fixed equivalence ratio (1.4) for the combustion zone was assumed. (NO_x) concentration and one way reaction rates decrease sharply as equivalence ratio goes above 1.1 ~ 1.2.
- b) The model assumed temperature constant inside the plume thereby making the (NO_x) concentration even lower, when compared with the actual case where a temperature distribution is known to exist.

Consequently we focused our attention on a new model that would include the mixing process through appeal to the equations of motion for a turbulent jet.

2. The New Model

The model divides the complete engine cycle into the following periods:

- i) valve overlap period
- ii) intake period
- iii) compression period
- iv) combustion period
- v) expansion period
- vi) exhaust period

Also the engine cycle is divided into the following items based on physical phenomena:

- i) gas exchange
- ii) heat transfer
- iii) air motion inside the cylinder
- iv) fuel jet dynamics
- v) heat release
- vi) NO_x formation
- vii) friction loss

The great benefit of this program is to be able to calculate the jet

dynamics coupled with the surrounding air motion, as a basis for calculation of the heat release rate, the NO_x formation and heat transfer between jet elements and combustion wall.

The computer program is based on the following assumptions;

- i) Temperatures in the cylinder are functions of time and location.
- ii) Pressures in the cylinder are functions of time only.
- iii) The charge is assumed homogeneous during intake, compression and exhaust process. (During combustion, the fuel jet is divided into 7-15 elements and each element has a different location and different equivalence ratio.)
- iv) The individual elements in the gas mixture are homogeneous but each has two different temperature zones, i.e., burned and unburned mixture. The unburned gas is composed of a low temperature mixture of air, non-reacting fuel and residual gases. The combustion zone is composed of high temperature unburned mixture and combustion products.
- v) There is mixing between jet elements and their environment, but no mixing between jet elements themselves.
- vi) Quasi-steady adiabatic and isentropic flow is assumed for mass flows past the valves.
- vii) The intake and exhaust manifolds are treated as infinite plenums having specified pressure and temperature histories, except during reversed flow past the intake valve, when plug flow is assumed to occur.

viii) Heat transfer is predicted with a model based on concepts introduced by Woschni(20) that have been extended to use local velocities in the combustion chamber.

ix) Thermodynamic characteristics of gas are based on a model proposed by Martin and Heywood(21).

x) Nitric oxide emissions are calculated by using the extended Zel'dovich kinetic scheme, with the steady state assumption for the N concentration and equilibrium values used for H, O, O₂, and OH concentrations in the adiabatic core.

3. Systems and Thermodynamic Equations

The early complete engine cycle simulation by Borman(22) assumed that the combustion gas as one uniform mixed element. In our model air and fuel are divided into many elements and every element has the same set of system and thermodynamic equations. A schematic of our model is shown in Fig. 2. Every element is viewed as an open system. *

i) State equation:

$$P V_i = M_i R_{gi} T_i$$

$$\frac{\dot{P}}{P} + \frac{\dot{V}_i}{V_i} = \frac{\dot{M}_i}{M_i} + \frac{\dot{T}_i}{T_i} \quad (3-1)$$

$$R_{gi} = R_{gi}(T_i, P, \phi_i) - \text{constant during each computing interval}$$

ii) Mass conservation:

$$\dot{M}_i = \dot{M}_{in_i} - \dot{M}_{out_i} \quad (3-2)$$

iii) Energy conservation for open system:

$$\dot{E}_i = \dot{Q}_i - \dot{W}_i + \dot{M}_{in_i} H_{in_i} - \dot{M}_{out_i} H_{out_i} \quad (3-3)$$

*All symbols are defined on pages 10 and 11.

iv) Internal energy equations:

$$E_i = M_i H_i - PV_i$$

$$\dot{E}_i = \dot{M}_i H_i + M_i \dot{H}_i - \dot{P}V_i - P\dot{V}_i \quad (3-4)$$

v) Work definition:

$$\dot{W}_i = \dot{P}V_i \quad (3-5)$$

vi) Enthalpy definition:

$$\dot{H}_i = C_{pi} \dot{T}_i$$

$$C_{pi} = C_{pi}(T_i, P, \phi_i) - \text{constant during each computing interval} \quad (3-6)$$

vii) Volume constraint:

$$\dot{V}_1 + \dot{V}_2 + \dots + \dot{V}_n = \dot{V} \quad (3-7)$$

viii) From geometry:

$$\dot{V} = R_{cr} \times \sin\theta_{cr} + L_{cnr} \times \frac{(R_{cr}/L_{cnr})^2 \times \sin\theta_{cr} \times \cos\theta_{cr}}{\sqrt{1 - (R_{cr} \times \sin\theta_{cr}/L_{cnr})^2}} \quad (3-8)$$

$$\times \text{Bore}^2 \times \frac{\pi}{4} \times \frac{d\theta_{cr}}{dt}$$

Values of $\dot{Q}_i$, M_{in_i} and M_{out_i} are given from several subprograms in advance before these differential equations will be solved. Total number of unknowns is N elements $\times$ 6 values ($\dot{E}_i$, $\dot{M}_i$, $\dot{H}_i$, $\dot{V}_i$, $\dot{W}_i$ and $\dot{T}_i$) + 2 ($\dot{P}$ and $\dot{V}$). Since the total number of differential equations is N elements $\times$ 6 (Eq.(1) $\sim$ Eq.(6)) + (Eq. (17) and Eq. (8)), these differential equations can be solved.

In the computer program these differential equations are solved according to the following procedure:

We get $\dot{V}_i$ from Eq. (1) $\sim$ Eq. (6)

$$\begin{aligned} \dot{V}_i = & \frac{V_i}{M_i C_{pi} T_i} (\dot{Q}_i + M_{in_i} H_{in_i} - M_{out_i} H_{out_i} - (M_{in_i} - M_{out_i}) H_i) \\ & + \frac{M_{in_i} - M_{out_i}}{M_i} V_i + \left(\frac{V_i^2}{M_i C_{pi} T_i} - \frac{V_i}{P} \right) \dot{P} \end{aligned} \quad (3-9)$$

Substituting $\dot{V}_i$ in Eq. (7) by Eq. (9), we get

$$\dot{P} = (\dot{V} - A)/B \quad (3-10)$$

where

$$\begin{aligned} A = \sum_{i=1}^n \frac{V_i}{M_i C_{pi} T_i} (\dot{Q}_i + M_{in_i} H_{in_i} - M_{out_i} H_{out_i} - (M_{in_i} - M_{out_i}) H_i) \\ + \frac{M_{in_i} - M_{out_i}}{M_i} V_i \end{aligned} \quad (3-11)$$

$$B = \sum_{i=1}^n \left(\frac{V_i^2}{M_i C_{pi} T_i} - \frac{V_i}{P} \right) \quad (3-12)$$

4. Jet Model

From the study of diesel combustion in a rapid compression machine by Rife and Heywood(14), it can be concluded that the fuel jet breaks into droplets near the nozzle orifice and the relative velocity of droplets in the jet flow is small. This means the mixing between packaged jet elements themselves is not important and only mixing between jet elements and surrounding air is taken into consideration. From the characteristics lengths analysis by Jain(19) he concluded that most of the droplets can evaporate before reaching the spark plug. Thus the model that fuel ignition is initiated by the spark plug and heat release is controlled only by mixing is now justified.

The mixing model is based on the turbulent entrainment assumptions of Hoult and Weil(23). The rate of entrainment for turbulent plumes introduced by Hoult and Weil have been modified to include the effects of large density variations, as suggested by Ricou and Spalding(24) and Escudier(25).

For the application of these turbulent entrainment theories to reciprocal engines, three more new aspects were added to them.

1) The NO_x value is not determined only by the present gas characteristics, but also it is very much dependent on the previous histories of gas characteristics. For this purpose jet model is solved by using the packaging method in order to identify every jet element at any instant.

2) All the previous jet models were set in a two-dimensional cartesian coordinate system. However, a cylindrical coordinate system is much more appropriate for reciprocal engines. The most important difference between these two systems is that the pressure field is not constant any more in the cylindrical coordinate system, especially in high swirl ratio engines. Jet elements, thus, are affected by the surface forces from the non-uniform pressure field and these surface forces have the same magnitude but opposite direction of the centrifugal forces when the jet elements have the same density and angular velocity as the surrounding air.

3) Restrictions of the combustion wall were taken into account. The cross section geometry of the jet was assumed to be in the shape of a D (Fig. 4) when it is contacting with the wall with the same centerline position and cross section area of the cylindrical jet. This consideration proved to have a good advantage for determining jet trajectory and heat transfer rate between jet elements and the combustion wall.

Let us consider a jet element "1" into a quiescent atmosphere of

element " ∞ " in the absence of any chemical reaction (Fig. 3). Then, the general equations of the jet model reduce to the following.

i) Conservation of mass

when jet is not contacting with the wall

$$\frac{1}{\frac{ds}{dt}} \cdot \frac{1}{dt}(\rho \pi b^2 u) = (\rho/\rho_\infty)^{1/2} \rho_\infty 2\pi b (\alpha |u-v_i| + \beta |v_n|) \quad (4-1)$$

when jet is contacting with the wall

$$\frac{1}{\frac{ds}{dt}} \cdot \frac{1}{dt}(\rho \pi b^2 u) = (\rho/\rho_\infty)^{1/2} \rho_\infty 2\pi b_c (1 - \frac{\theta_j}{2\pi}) \cdot (\alpha |u-v_i| + \beta |v_n|) \quad (4-1)$$

θ_j : jet contacting angle with the wall (see Fig. 4)

$$\text{Max. of } \theta_j = \pi$$

ii) Conservation of angular momentum

$$\frac{d}{dt}(\rho \pi b^2 u R w) = R w_s \frac{d}{dt}(\rho \pi b^2 u) - \rho \pi b^2 u v_r w \quad (4-2)$$

w_s : angular velocity of swirl

$\rho \pi b^2 u v_r w$: coriolis force

iii) Conservation of radial direction momentum

$$\frac{d}{dt}(\rho \pi b^2 u v_r) = \rho \pi b^2 u R \omega^2 - \rho_\infty \pi b^2 u R \omega_s^2 + v_{R\infty} \frac{d}{dt}(\rho \pi b^2 u) \quad (4-3)$$

$\rho \pi b^2 u R \omega^2$: centrifugal force

$\rho_\infty \pi b^2 u R \omega_s^2$: force arising from pressure gradient swirling flow

iv) Conservation of vertical direction momentum

$$\frac{d}{dt}(\rho \pi b^2 u v_z) = v_{z\infty} \frac{d}{dt}(\rho \pi b^2 u) \quad (4-4)$$

v) From geometry

$$u \frac{du}{dt} = R^2 \omega \frac{d\omega}{dt} + R \omega^2 \frac{dR}{dt} + v_r \frac{dv_r}{dt} + v_z \frac{dv_z}{dt} \quad (4-5)$$

$$\frac{dR}{dt} = v_r \quad (4-6)$$

vi) Conservation of fuel

$$\frac{d}{dt}(\rho \pi b^2 u X_f) = 0 \quad (4-7)$$

vii) Jet is in the combustion chamber

$$\text{Jet location } (R, \theta, Z) \leq \text{combustion chamber} \quad (4-8)$$

viii) For contacting angle θ_j

$$\pi b^2 = \pi b_c^2 \times \left(1 - \frac{\theta_j}{2\pi}\right) + \frac{b_c^2}{2} \sin\theta_j \quad (4-9)$$

5. Air Motion Surrounding the Jet

Calculation of gas velocity surrounding the jet is required to define the jet trajectory and mixing ratio between the jet and gas. A first order calculation was made by M. Martin(21). This model is limited to the regions close to the cylinder wall or piston by the assumptions and the model can be extended to the whole region inside the cylinder for our purpose. Since an exact solution including viscous effects is difficult and time-consuming, several assumptions are necessary for simplification of this model.

i) The combustion chamber is divided into three regions (Fig. 6);

Inside each region, axial velocity is uniform on the same horizontal plane, radial velocity and angular velocity is uniform on the same radius.

ii) In region (3) there is no radial velocity.

This assumption is necessary in order to avoid a large velocity discontinuity at the piston cup edge due to a large area discontinuity there.

iii) Boundary conditions.

Axial velocity = 0 at cylinder head,
 radial velocity = 0 at cylinder wall,
 and axial velocity is the same as piston at piston surface.

iv) Swirl at bottom center is solid body rotation.

v) Angular momentum is not conserved.

After precisely checking the pictures (26) of the rapid compression machine it was found that the swirl amplitude (the ratio of swirl at TDC to swirl at BDC) decreases when swirl magnitude goes up. Under normal Texaco engine operation (swirl ratio is 3.65 x rpm at BDC), this swirl decaying is about 10%. The following equation is used for estimating swirl decaying:

$$\frac{\text{swirl momentum decayed}}{\text{initial swirl momentum}} = C_{DE} \times w^2 \times \text{Time}$$

C_{DE} : swirl decaying factor 6.5×10^{-6} for Texaco engine

w : angular velocity (rad/sec)

Time: time since intake valve closes (sec)

(1) Calculation of Radial Velocities (Fig. 6)

(a) $\underline{R_c < r < R_p}$

$$\frac{dM_2}{dt} = - \frac{dM_1}{dt} = 2\pi r h \rho \bar{v}_r \quad (5-1)$$

$$M_1 = \pi(R_p^2 - r^2) h \rho \quad (5-2)$$

$$M_2 = (\pi r^2 h + V_c) \rho \quad (5-3)$$

M_i : the mass in control volume i

t : time

ρ : density of the charge

V_c : piston cup volume

Combining (5-1), (5-2) and (5-3)

$$(\pi r^2 h + V_c) \rho' + \pi r^2 \rho h' = - \pi(R_p^2 - r^2) (h' \rho + \rho' h)$$

$$\rho' = -\left(\frac{h'}{K_1 + h}\right) \rho \quad (5-4)$$

$$\text{when } K_1 = \frac{V_c}{\pi R_p^2} \quad (5-5)$$

$$\text{Let } X = \frac{h}{K_1} \quad (5-6)$$

Then solving for ρ in terms of initial conditions at time t_o yields

$$\rho(t) = \rho(t_o) \left(\frac{X(t_o) + 1}{X(t) + 1} \right) \quad (5-7)$$

From Eq. (5-1) and (5-2) we have

$$\bar{v}_r = \frac{-\frac{dM_1}{dt}}{2\pi r h \rho} = \frac{-\pi(R_p^2 - r^2)(h'\rho + \rho'h)}{2\pi r h \rho}$$

Using (5-4) and letting

$$v_p = \frac{dh}{dt} = \text{piston velocity (upward velocity has negative sign)}$$

We find

$$\bar{v}_r(r, t) = - \left(\frac{r}{2K_1} \right) \left[\left(\frac{R_p^2}{r^2} - 1 \right) \frac{v_p(t)}{X(t)(1+X(t))} \right] \quad (5-8)$$

(b) $0 < r < R_c$

The radial velocity inside the piston cup is assumed to be zero.

$$\frac{dM_2}{dt} = - \frac{dM_1}{dt} = 2\pi r h \rho \bar{v}_r \quad (5-9)$$

$$k_2 = V_c / (\pi R_c^2) \quad (5-10)$$

$$M_1 = \pi(R_p^2 - r^2) h\rho + \pi(R_c^2 - r^2) K_2\rho \quad (5-11)$$

$$M_2 = \pi(h + k_2)r^2\rho \quad (5-12)$$

Combining (5-9), (5-11) and (5-12)

$$\begin{aligned} \pi(h + k_2)r^2\rho' + \pi r^2\rho h' &= -\pi(R_p^2 - r^2) (h'\rho + h\rho') \\ &\quad - \pi(R_c^2 - r^2) k_2\rho' \end{aligned}$$

$$\rho' = - \left(\frac{h'}{k_1 + h} \right) \rho \quad (5-13)$$

From Eq. (5-9) and (5-12) we have

$$\bar{v}_r(r,t) = \left(\frac{r}{2k_1} \right) \frac{\left(\frac{k_2}{k_1} - 1 \right) v_p(t)}{X(t) (1 + X(t))} \quad (5-14)$$

(2) Calculation of Axial Velocities

(a) 0 < Z < h

$$-\frac{dM_1}{dt} = \frac{dM_2}{dt} = \pi R_p^2 \bar{v}_z \rho \quad (5-15)$$

$$M_1 = \pi R_p^2 \rho Z \quad (5-16)$$

$$M_2 = \pi R_p^2 \rho (h-Z) + V_c \rho \quad (5-17)$$

We assume

$$\bar{v}_{z1}(Z,t) = v_p Z/h \quad \text{for } R_c < r < R_p \quad (5-18)$$

From (5-15), (5-16), (5-17) and (5-18) we have

$$\bar{v}_{z2}(Z,t) = v_p Z/h \left\{ 1 - \left(\frac{R_p}{R_c} \right)^2 \frac{1}{(X(t) + 1)} \right\} \quad \text{for } 0 < r < R_c \quad (5-19)$$

(b) $h < Z$

$$- \frac{dM_1}{dt} = \frac{dM_2}{dt} = \pi R_c^2 \bar{v}_z \rho \quad (5-20)$$

$$M_1 = \pi R_p^2 h + \pi R_c^2 (Z-h) \quad (5-21)$$

$$M_2 = \pi R_c^2 (k_2 - (Z-h)) \quad (5-22)$$

From (5-20), (5-21) and (5-22) we have

$$\bar{v}_z(Z,t) = \frac{k_1 - k_2 + Z}{k_1 + h} v_p \quad (5-23)$$

(3) Calculation of Angular Velocity

The gas angular velocity inside the cylinder is assumed to be a solid body rotation.

From momentum equation

$$\begin{aligned}
 & \underbrace{\int_0^{R_p} \int_0^h \int_0^{2\pi} \rho w r^3 d\theta dz dr}_{\text{momentum in region (1)}} + \underbrace{\int_0^{R_c} \int_0^{k_2} \int_0^{2\pi} \rho w r^3 d\theta dz dr}_{\text{momentum in region (2)}} \\
 &= (1 - \text{DECAY}) \times \left[\underbrace{\int_0^{R_p} \int_0^h \int_0^{2\pi} \rho_o w_o r^3 d\theta dz dr + \int_0^{R_c} \int_0^{k_2} \int_0^{2\pi} \rho_o w_o r^3 d\theta dz dr}_{\text{initial momentum}} \right] \quad (5-24)
 \end{aligned}$$

DECAY: swirl decaying ratio

From Eq. (5-24)

$$\begin{aligned}
 w(t) &= (1 - \text{DECAY}) \times \frac{\rho_o}{\rho} \times \frac{k_2 R_c^4 + h_o R_p^4}{k_2 R_c^4 + h R_p^4} w_o \\
 &= (1 - \text{DECAY}) \times \frac{(h + k_1)}{(h_o + k_1)} \times \frac{k_2 R_c^4 + h_o R_p^4}{k_2 R_c^4 + h R_p^4} w_o \quad (5-25)
 \end{aligned}$$

Figure 7 and Fig. 8 are the calculation results using these assumptions. At -50 BTDC gas movement is dominated by the piston velocity and swirl. The radial velocity is almost negligible. At - 30 BTDC, the radial velocity begins to grow as the gas in the squish area is forced into the piston cup. At -10 BTDC, the piston is almost stopped and the radial velocity, especially at the edge of the piston cup, is very high. Squish effect can be computed from this study. This more detailed study in general confirms the basic conclusions of Martin but provides more detailed specification of the flows for jet mixing analysis.

6. Combustion Model

From the observation of pictures in the rapid compression machine it was found that the unburned gas mixture hitting the spark plug has a small plume first and this plume grows, entraining surrounding unburned gas mixture. The main flame can be seen a little bit downstream from the spark plug and this ignition delay time is about 0.7 - 0.8 msec at 2000 rpm. These phenomena are also verified by log P-log V diagrams shown in Marsh thesis(27). A mixing and chemical induction time seems to be associated with this delay and the order of magnitude is similar to the delay in a spark ignition engine.

To explain the combustion delay mentioned above, an analytical model for combustion reaction time was developed. In this model a fuel-air

element starts to burn when it hits the spark plug but the fuel in the jet element doesn't burn instantaneously because of finite flame speed and a typical induction period. In the early stages of combustion growth, this burning nucleus is so small that this stage can be treated as if there were no combustion. The schematic of this model applied to the TCCS engine is shown in Fig. 9.

i) Entrainment of unburned mixture

The entrainment of the surrounding gas mixture into the burning nucleus has been treated with an analysis based on the work of Blizard and Keck(28) which relates the turbulent eddy entrainment velocity to the engine speed.

The mass rate of entrainment of surrounding gas mixture can be given as

$$\frac{dM_e}{dt} = \sqrt{\rho_u \rho_b} * S_e * U_e \quad (6-1)$$

where S_e is plume surface area and U_e the turbulent eddy entrainment velocity. In the Blizard and Keck model, the entrainment velocity is based on the velocity of the inlet jet. However, in the TCCS geometry, entrainment into the spark nucleus is dominated by the velocity of the fuel jet

$$U_e \approx 0.22u \quad (6-2)$$

ii) Combustion delay

Tabaczynski(29) computed a characteristic reaction time (τ) for a large eddy using a characteristic reaction time (τ_c) defined for an eddy of the order of the turbulent microscale. The rate of mass burned in an individual eddy is assumed to be proportional to the mass of unburned gas that exists in the plume

$$\frac{dM_b}{dt} = \frac{M_u}{\tau_c} = \frac{M_e - M_b}{\tau_c}$$

M_e : entrained gas in the plume

M_b : burned gas in the plume

M_u : unburned gas in the plume

$\tau_c = \lambda/Se$ characteristic reaction time for the microscale

λ : Taylor microscale

$$\lambda = 0.17 \times \frac{\text{intake valve lift}}{\text{compression ratio}} \quad (\text{Ref. (28) and (30)})$$

Se : laminar flame speed (Ref. (28))

7. NO_x Model

The NO_x formation model is based on the same model as combustion mentioned before which is composed of unburned gas mixture outside flame front, burning zone and burned gas. But the temperatures of these zones are defined by only two typical temperatures: burned and unburned gas temperatures, by decoupling the burning zone into these two temperature zones. Figure 12 shows the mass histories of these zones during the period from the fuel injection to fully developed plume. As can be seen, the burning zone is very thin and disappears quickly, and this zone is proved not to have much effect on NO_x amount by computer simulation. This model also calculates the transferred amount of NO_x between elements by mixing. The NO formation model described by Lavoie, Heywood and Keck (32), and Komiyama and Heywood (8) is used, i.e., NO formation is governed by the extended Zel'dovich mechanism:



The hydrocarbon oxidation reactions are fast relative to the NO formation process and a reasonable approximation is that the species O, O₂, H, OH and N₂ are in equilibrium. A steady-state assumption is made for [N]. The rate of change of NO mass fraction {NO} due to chemical reaction;

$$\frac{d\{NO\}}{dt} = \frac{2M_{no}}{\rho} \frac{(1 - (\{NO\}/\{NO\}_e)^2)R_1}{(1 + K\{NO\}/\{NO\}_e)} \quad (7-4)$$

{NO} = NO mass fraction

M_{no} = molecular weight of NO

ρ = gas density

$$R_1 = K_{+1} (O)_e (N_2)_e = K_{-1} (N)_e (NO)_e$$

()_e = mole concentration in equilibrium

$$K = \frac{R_1}{R_2 + R_3} = \frac{K_{-1} (NO)_e}{K_{+2} (O_2)_e + K_{+3} (OH)_e}$$

8. Heat Transfer Model

Heat transfer calculation of the TCCS engine seems to require a more complicated model than that of the spark ignition engine, because the heterogeneous mixture causes a large temperature distribution inside the combustion chamber, and also heat transfer between the jet and piston top has an important effect on the early stage of combustion like the impingement effect. The wall inside the TCCS engine, thus, is divided into five regions as many diesel engines are so, i.e., piston top, cylinder wall, cylinder head, intake valve and exhaust valve (see Fig. 10). These temperatures are estimated as 650°K, 600°K, 650°K, 500°K and 700°K respectively. Each wall of the combustion chamber is in contact with the hot, burned gas plume while the remaining are in contact with relatively cold unburned gas mixture.

All the necessary data for the heat transfer calculation like the heat transfer area of the jet elements and gas velocity at the wall are provided by the jet model calculation.

The conventional engine heat transfer correlations of Woschni(20) have been used to model the heat transfer process. The Nusselt number is expressed as;

$$Nu = 0.035 Re^{0.8} \quad (8-1)$$

Using Woschni's relationships for gas velocities, density, viscosity and thermal conductivity, the convective heat transfer coefficient is expressed as;

$$\mu = 7014 B_{ore}^{-0.2} P^{0.8} G^{-0.53} [C_1 + 100C_2 \frac{VT_o}{P_o V_o} (P - P_{is}) + C_3 v_s]^{0.8} \quad (8-2)$$

$$Q = C\mu A(T - T_w) \quad (8-3)$$

B_{ore} : bore

P : pressure

T : temperature

A : heat transfer area

N : engine speed

V : total volume

v_s : swirl velocity

P_o, T_o and V_o : pressure, temperature and volume when intake valve closes

P_{is} : when compression and expansion are isentropic

Woschni used an average piston speed ($\frac{SN}{30}$) as a gas velocity at the wall in his equations but the swirl velocity has a much higher magnitude than the piston speed for the Texaco engine and the swirl velocity term (V_s) was added to them. Heat transfer is not assumed to occur between jet elements and air.

III Comparison of Simulation Predictions with Experimental Data and Conclusions

Experimental works were performed on a TCCS engine by Marsh (27) and Fly (33). A 3-7/8" x 3-7/8" single cylinder engine designed by Texaco has been set up at the Sloan Automotive Laboratory at MIT to carry out experimental investigations on the TCCS, stratified charge concept. A brief description of the engine set up and cross-cut distillate fuel characteristics are given in Table 1-3. Additional details regarding the engine set up, data taking and data reduction can be found in their theses (27) (33).

The following comparisons of calculation results with experimental data were conducted while changing injection timing and equivalence ratio;

- i) Mass fraction burned (Figs. 15,16)
- ii) Cylinder pressure (Figs. 17,18)
- iii) NO versus injection timing (Fig. 19)
- iv) Volumetric efficiency, indicated mean effective pressure and peak pressure versus injection timing (Fig. 20)
- v) Exhaust temperature versus injection timing (Fig. 21)
- vi) NO concentration histories in each element (Fig. 23) (prediction only).
- vii) Swirl effects on indicated mean effective pressure and NO (Fig. 24) (prediction only).

As shown in these figures, every parameter except exhaust temperature was predicted accurately by this simulation model. The

major conclusions which have been drawn from this study are:

1. Ignition delays were calculated successfully by the travelling time from fuel nozzle to spark plug and induction time of unburned mixture to the burning zone.
2. The burning rate was accurately predicted by the jet mixing process based on turbulent entrainment assumptions.
3. Good agreement in cylinder pressure during compression and expansion process means that the heat transfer amount between gas and wall was accurately estimated by the model, which calculates the local gas velocities and jet contacting areas with the wall based on the Woschni correlations.
4. NO_x values were predicted within practical errors. NO_x concentration is very sensitive to the mixing process. The figure of NO_x concentration histories in each element shows that exhaust NO_x can be reduced drastically by rapid mixing after the spark plug.
5. The model predicted higher exhaust temperatures than actual data. Heat transfer calculations from gas to port seems to be necessary for precise exhaust temperature prediction.

6. Higher swirl ratio has a good effect on NO concentrations at high equivalence ratios due to the rapid cooling of burned gas. At low equivalence ratios, however, higher swirl ratio has an unfavorable effect on NO concentration due to the coincidence of higher gas temperatures and peak cylinder pressures.

7. Some more detailed calculation about air motion inside the cylinder is recommended to get more accurate NO prediction over wide range engine operations.

8. It is recommended that this model be applied for calculating another size engine performance to check this model validity.

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TABLE 1
Engine Specifications

Dimensions	
bore	3.875 in.
stroke	3.875 in.
connecting rod	6.625 in.
clearance volume	4.570 in. ³

Valve Timings		
	Opens	Closes
inlet valve	10 BTCD (1)	55 ABDC (2)
	0 (2)	45 (1)
exhaust valve	55 BBDC (1)	10 ATDC (2)
	45 (2)	0 (1)

(1) at 0.006 in. valve lift

(2) valve face flush with head

TABLE 2
Summary of Instrumentation

<u>Temperatures</u>		
Air Orifice Inlet	Water Outlet	Bearing Oil
Air Inlet	Exhaust	Fuel Inlet
Water Inlet	Crankcase Oil	Fuel Returns

Instrument - All Points

Chromel - Alumel Thermocouple

Omega DS - 500 Digital Readout

Resolution 1^oF

<u>Pressures</u>		
	Method	Resolution
Inlet Air	Water Manometer	.1 in.
Crankcase Vacuum	Water Manometer	.1 in.
Oil Pressure	Panel Gage	2 PSI
Exhaust	Mercury Manometer	.1 in.
Dynamometer Load	Mercury Manometer	.1 in.
Injection Line	Kistler 601 Piezoelectric transducer, Kistler 504E	30 PSI*
	Charge Amplifier	
Combustion Chamber	Kistler 609A Piezoelectric Transducer, Kistler 503D Charge Amplifier	.2 PSI**

TABLE 3

Summary of Fuel Properties

	Cross-cut Distillate
Molecular Wt.	125
H:C Ratio	1.825
Specific Gravity	.80
Boiling Point °F	106-648
Lower Heating Value (Btu/lbm)	18038
Stoichiometric F/A Ratio	.0694
FIA - %	
Aromatics	29.5
Olefins	3.0
Saturates	67.5
Octane No. RON	76.6
Cetane No.	28.3

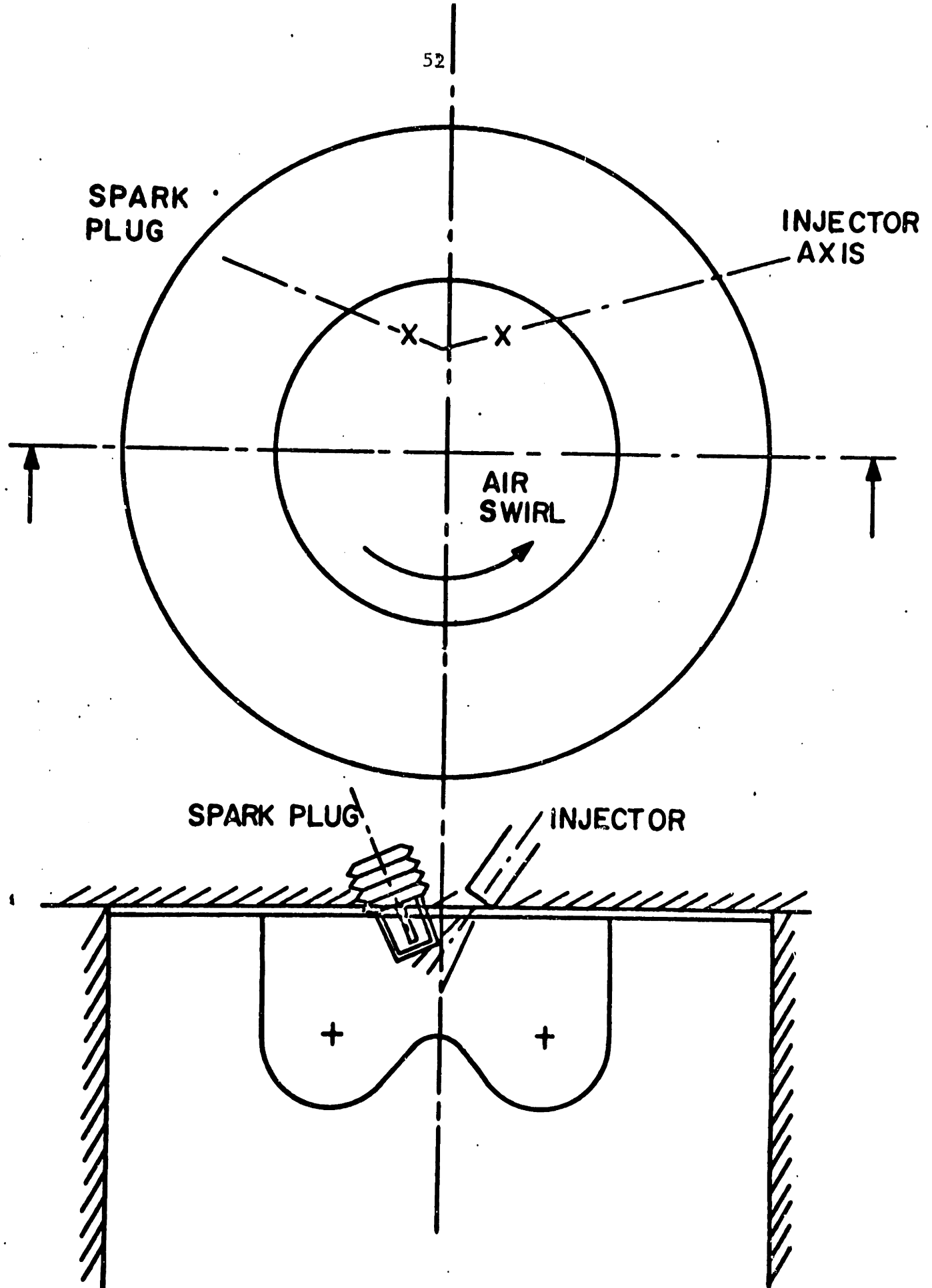


Fig. 1 TEXACO CONTROLLED COMBUSTION
SYSTEM (SCHEMATIC)

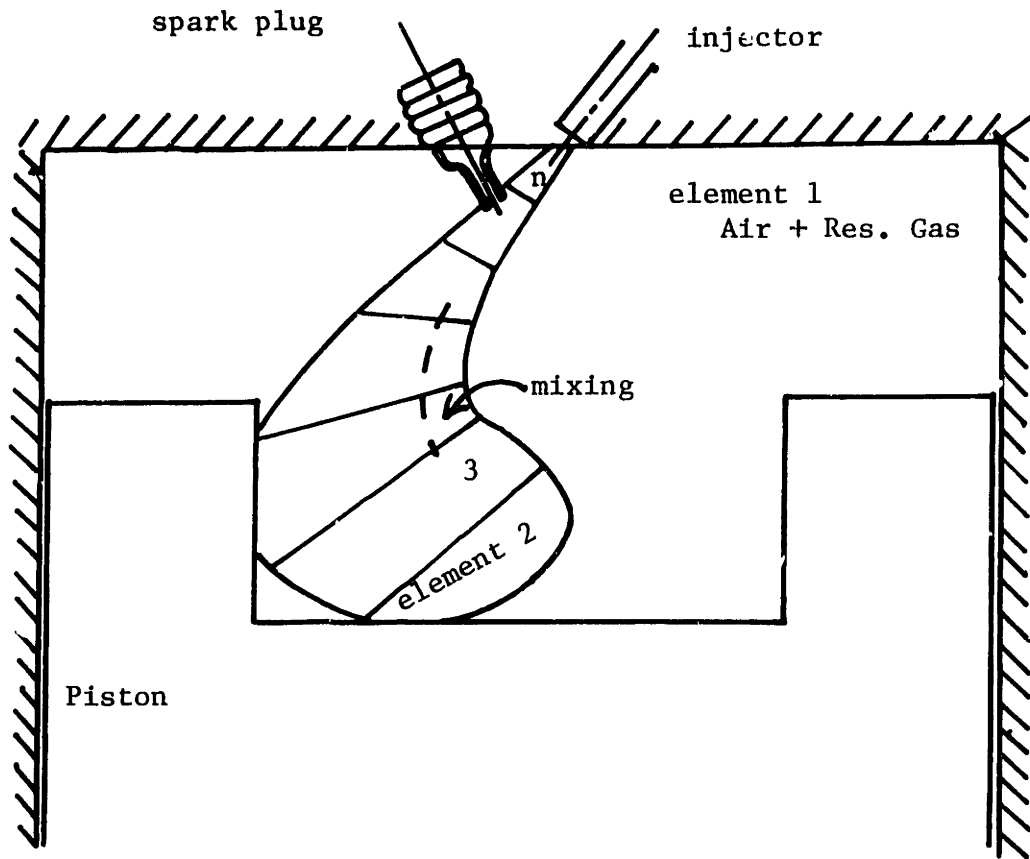
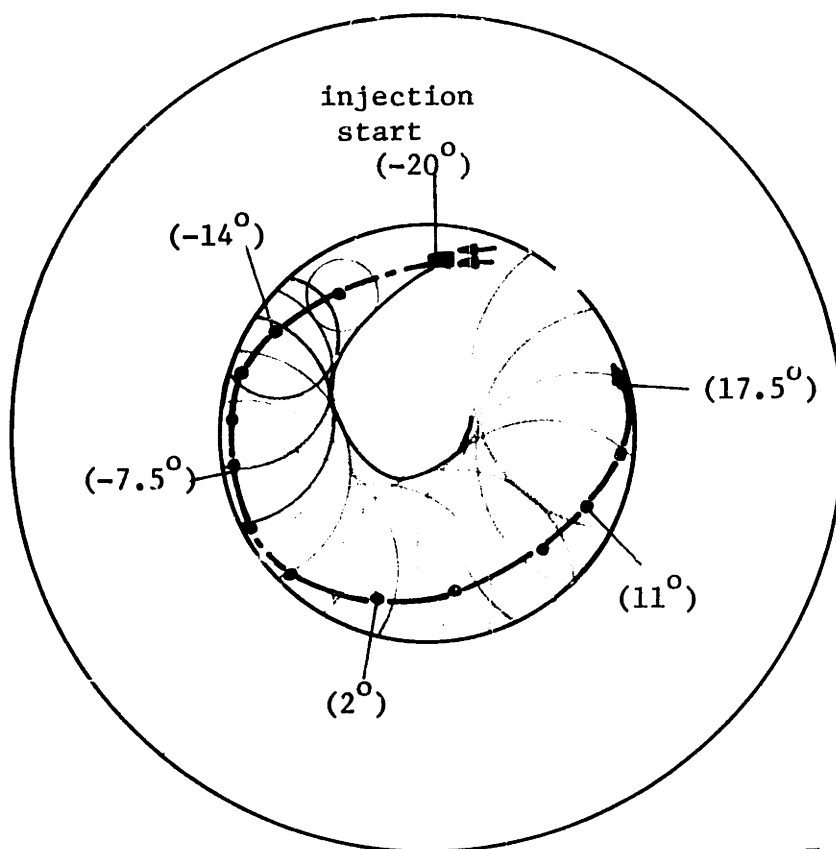
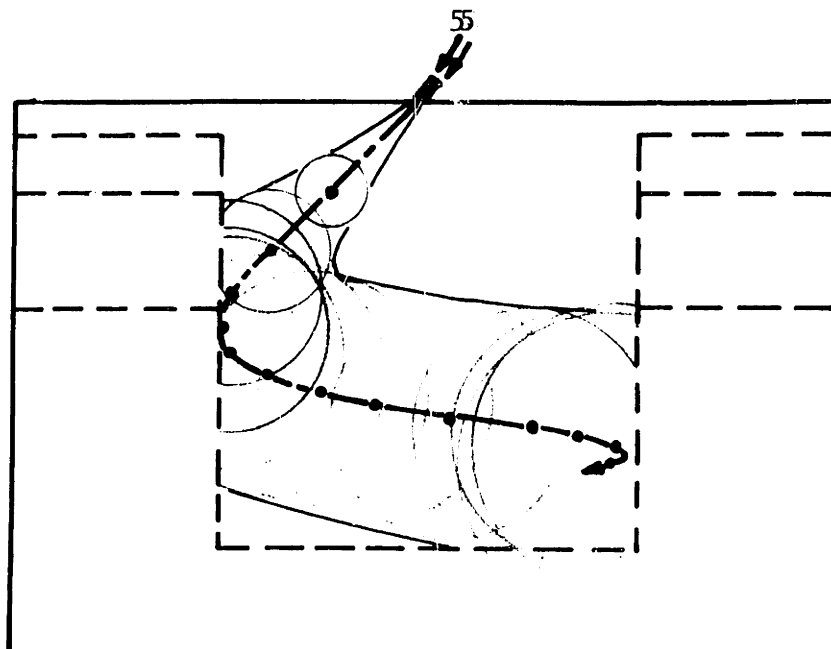


Fig. 2 System Model



Engine Speed = 2000 rpm

Swirl Ratio = 3.65 x Engine
Speed (at B)

$$\phi = 0.545$$

Fig. 5 Calculation Results of Jet Model
(First Jet Element Trajectory)

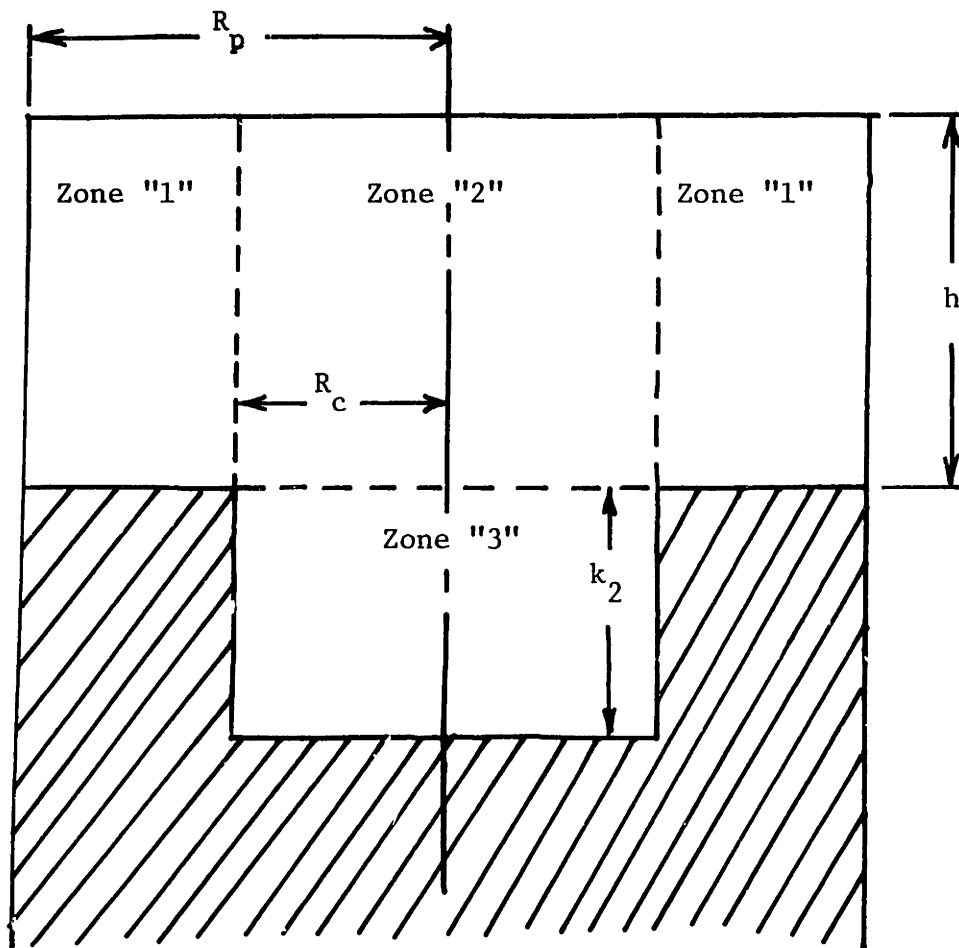
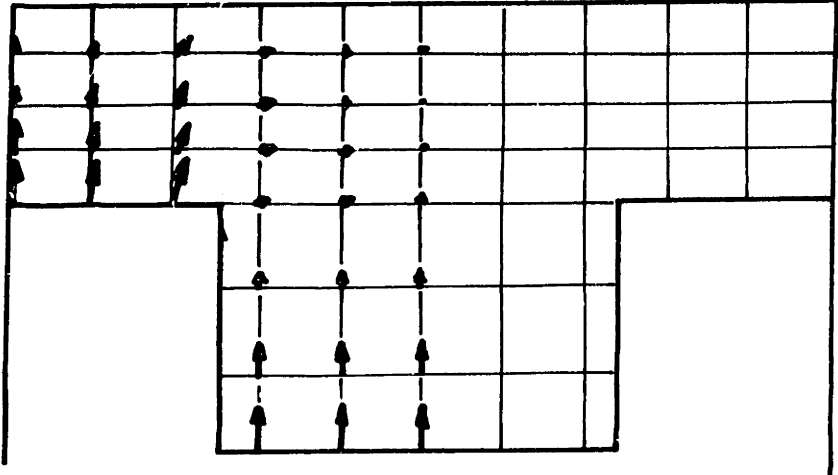


Fig. 6 Model of Air Motion Calculation

RPM = 2500 rpm
 SCALE 20 m/s $\rightarrow$ 1 cm
 (velocity)

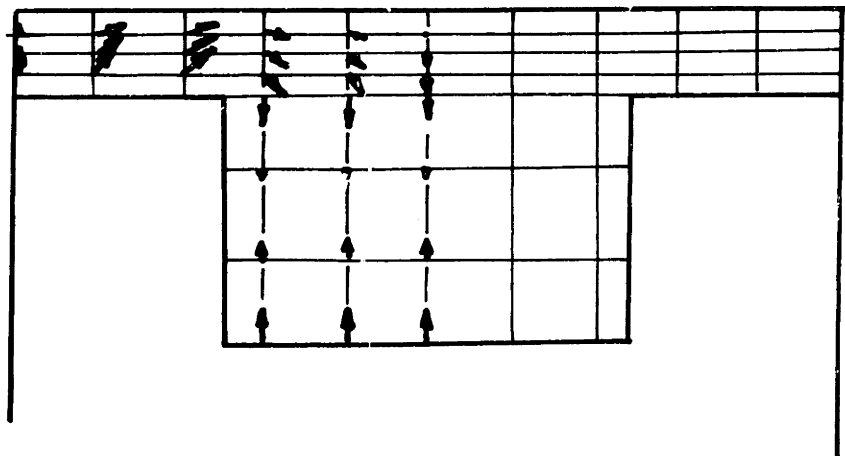
i) at -50° before TDC

piston speed
 = 11.8 m/s



ii) at -30° before TDC

piston speed
 = 8.1 m/s



iii) at -10° before TDC

piston speed
 = 2.9 m/s

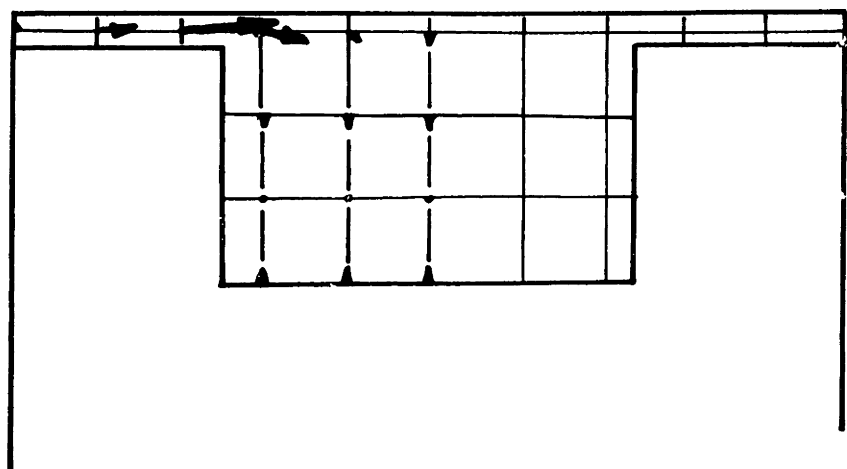


Fig. 7 Air Motion by Calculation

(Radial and Axial Components)

RPM = 2500 rpm

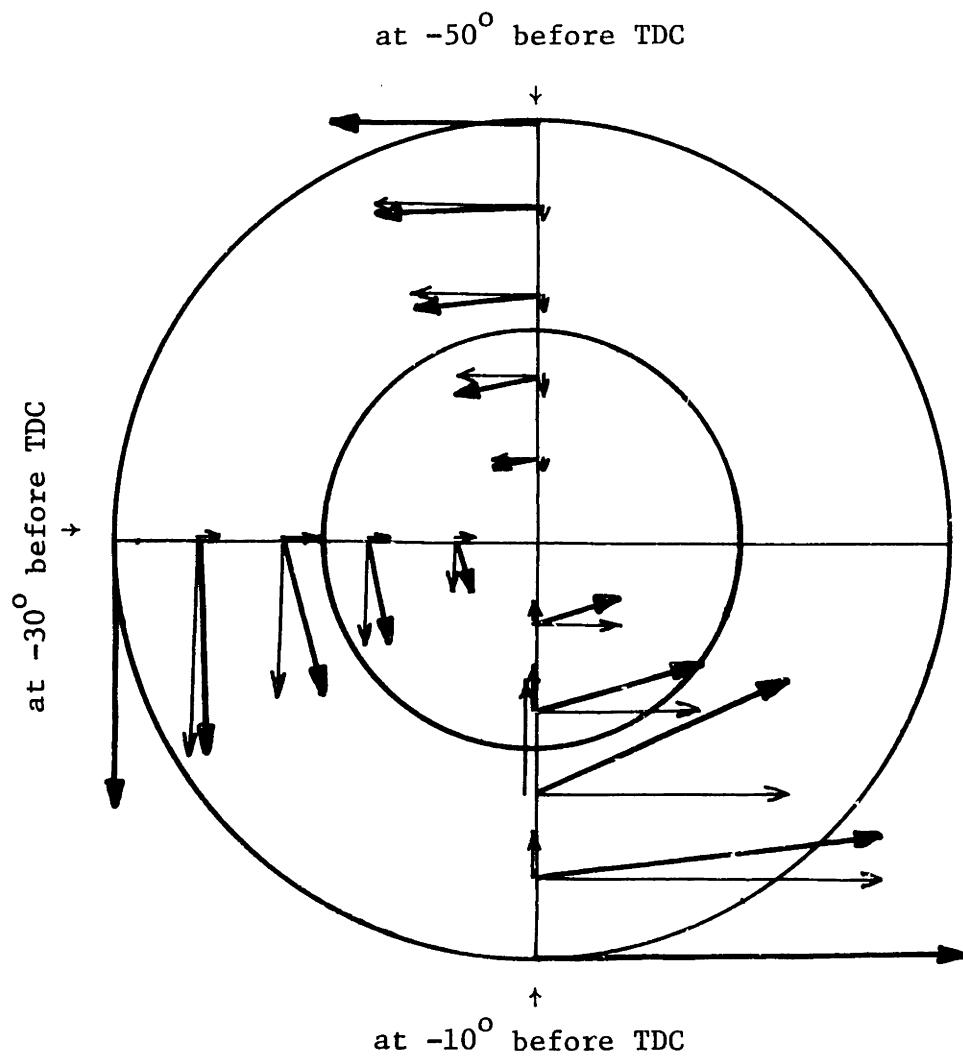
Scale 20m/s $\rightarrow$ 1 cm (velocity)

Fig. 8 Air Motion (Prediction)
(Radial and Tangential Components)

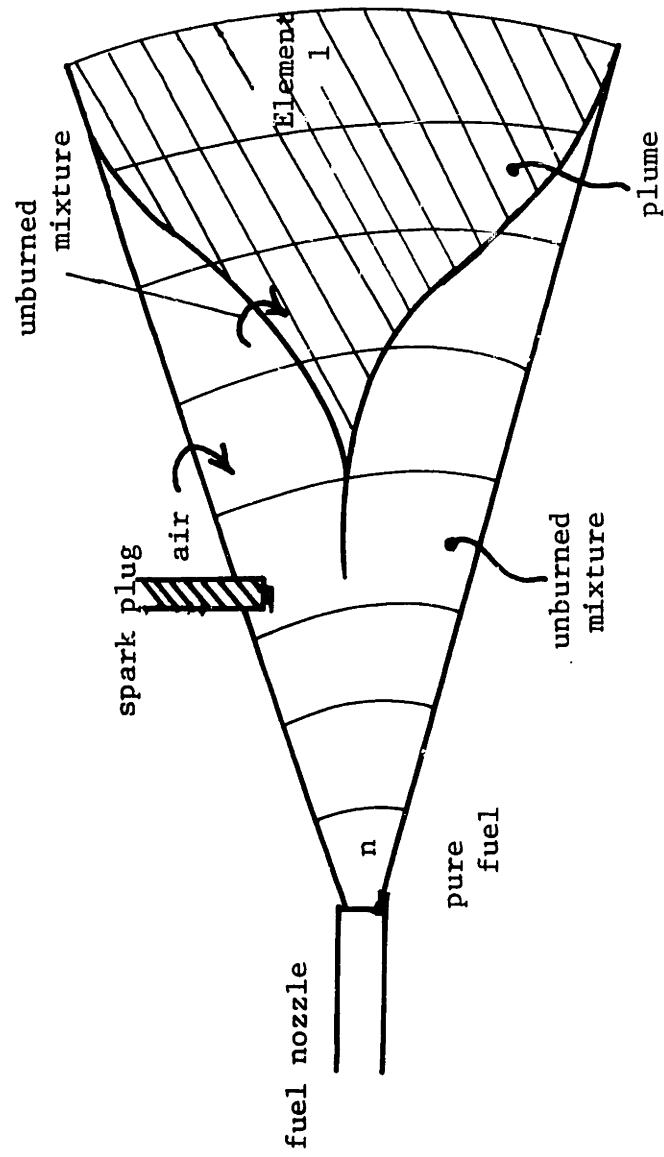


Fig. 9 The Schematic of Ignition Model

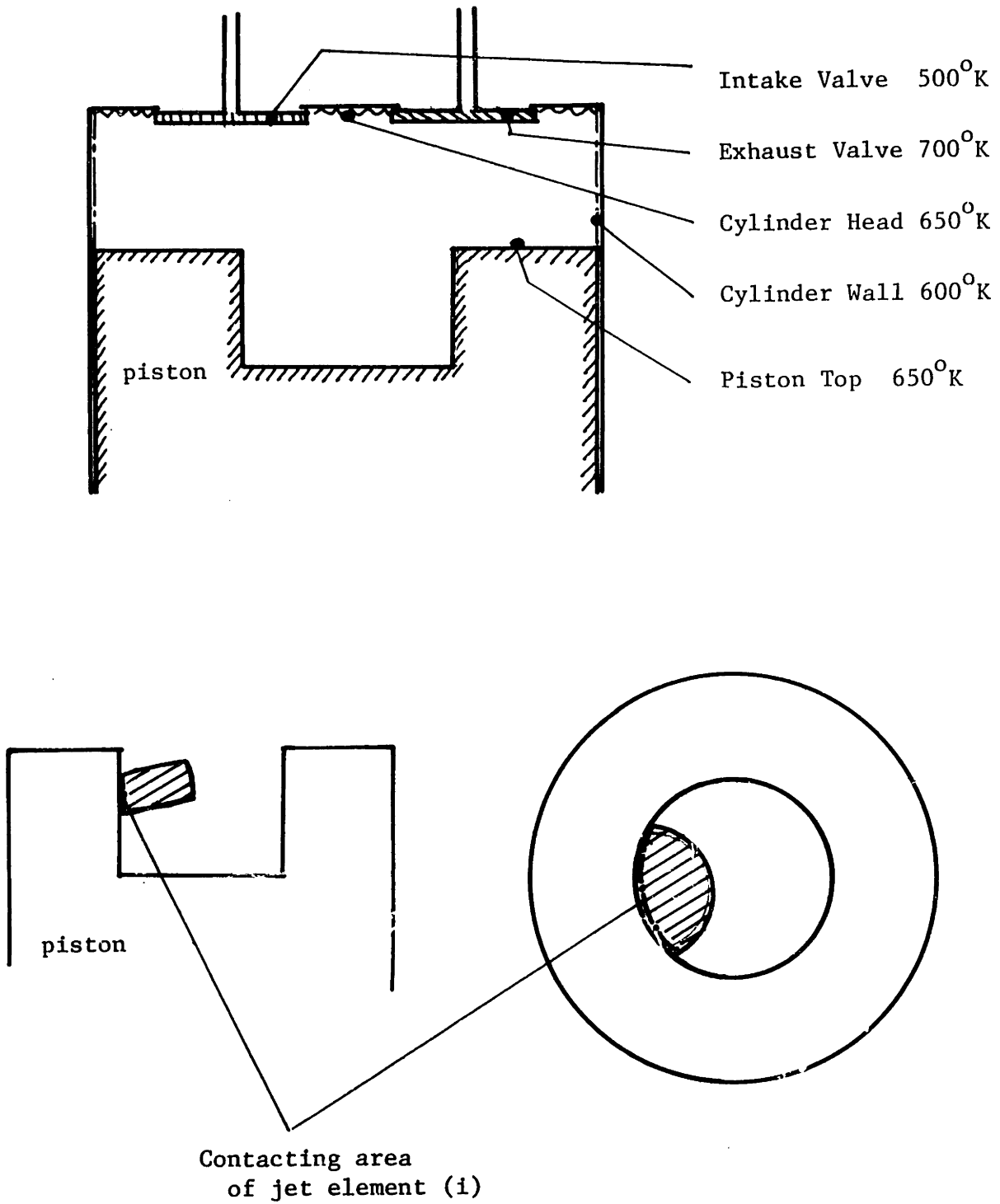


Fig. 10 Heat Transfer Model

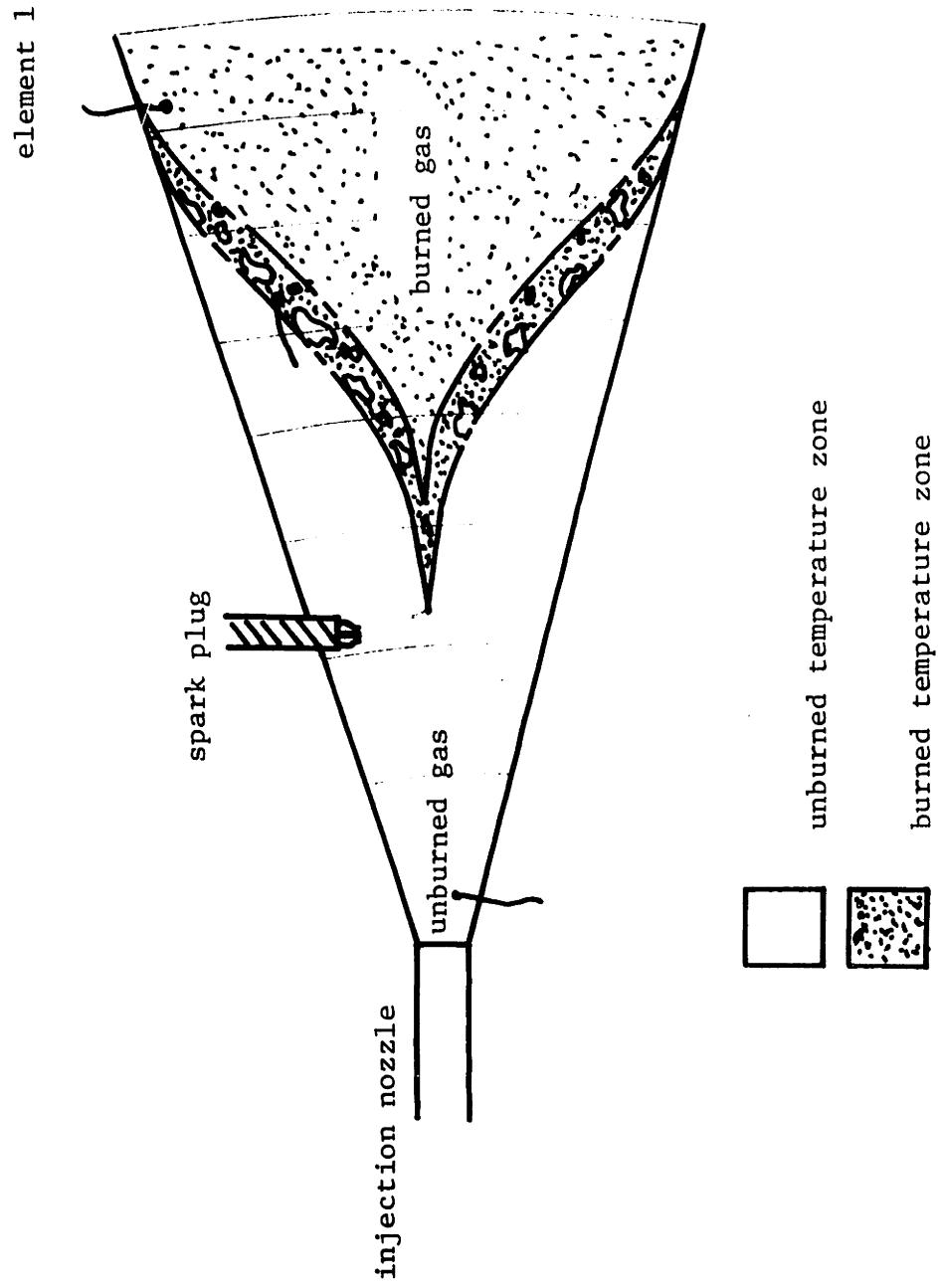


Fig. 11 The Schematic of NO_x Model

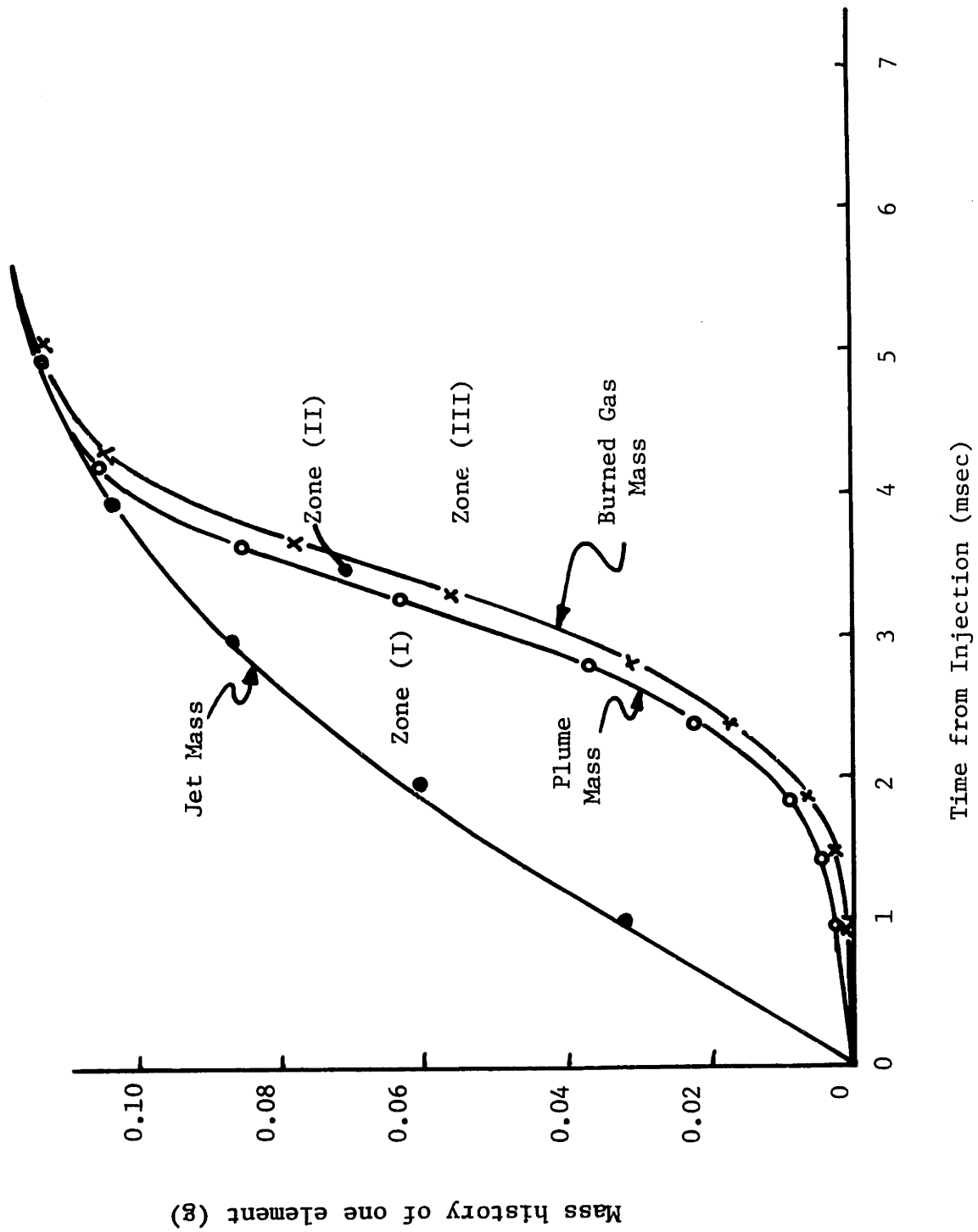


Fig. 12 Mass History of One Element (prediction)

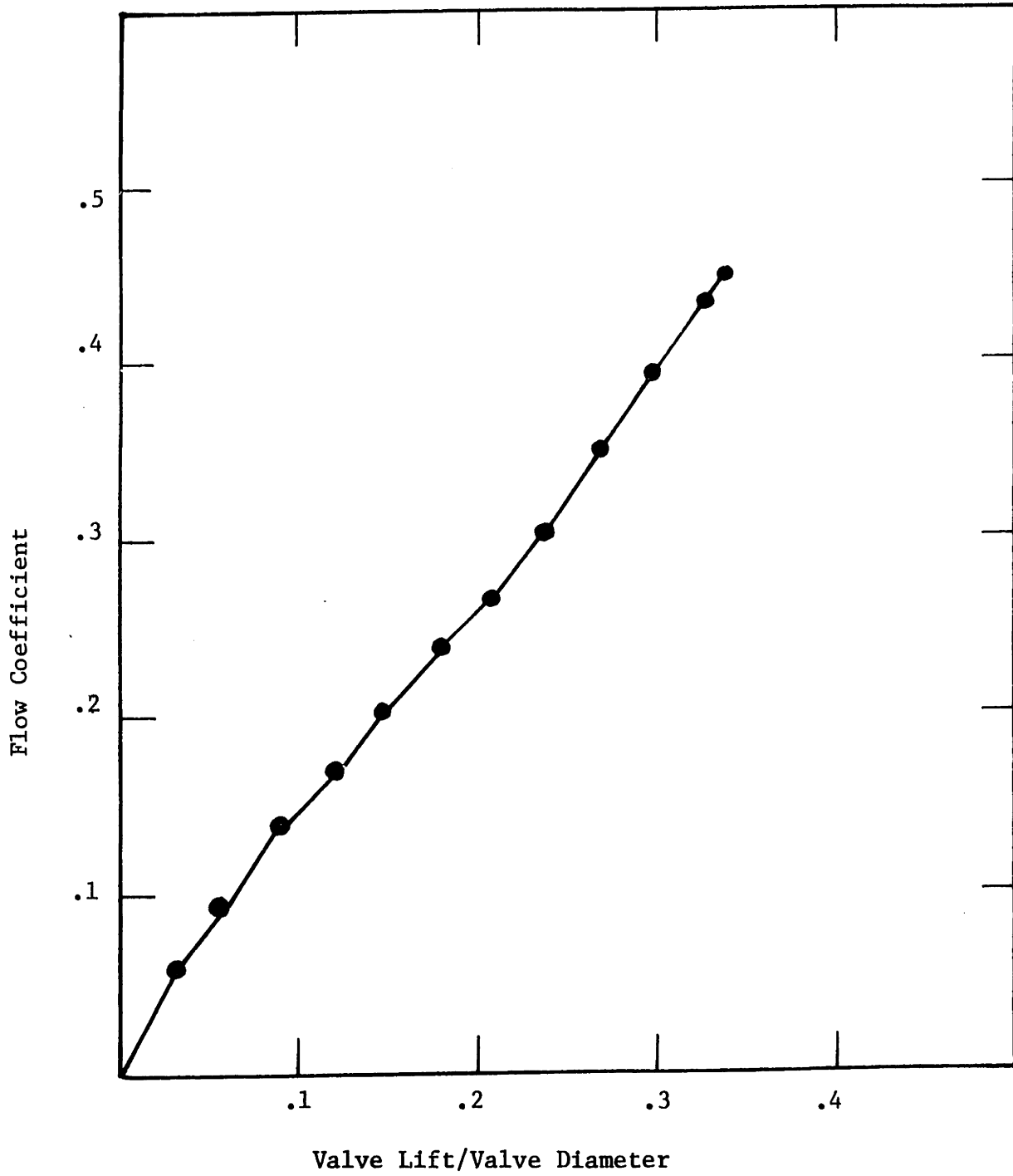


Fig. 13 Valve Flow Coefficient for the Intake Valve

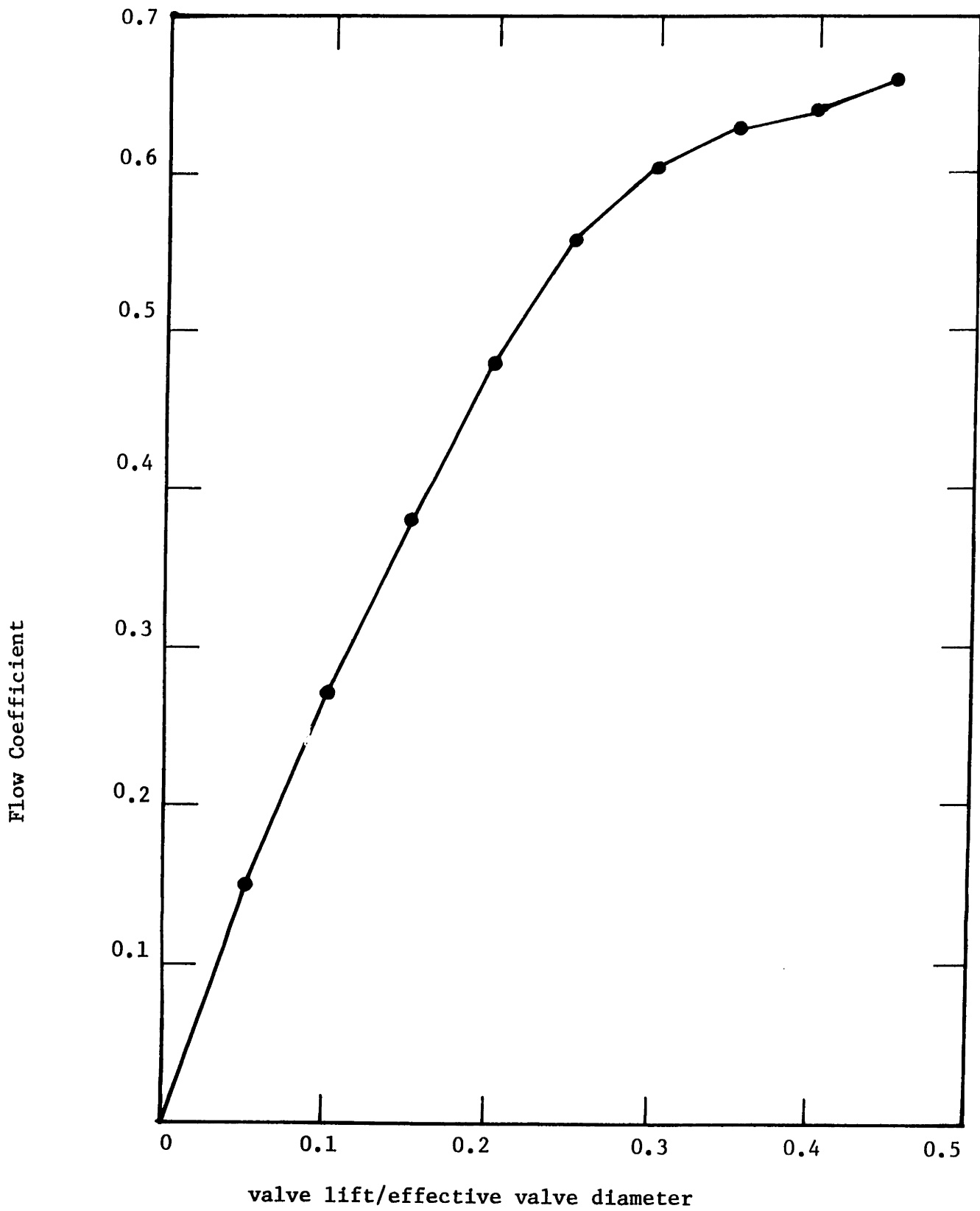


Fig. 14 Valve Flow Coefficient for the Exhaust Valve

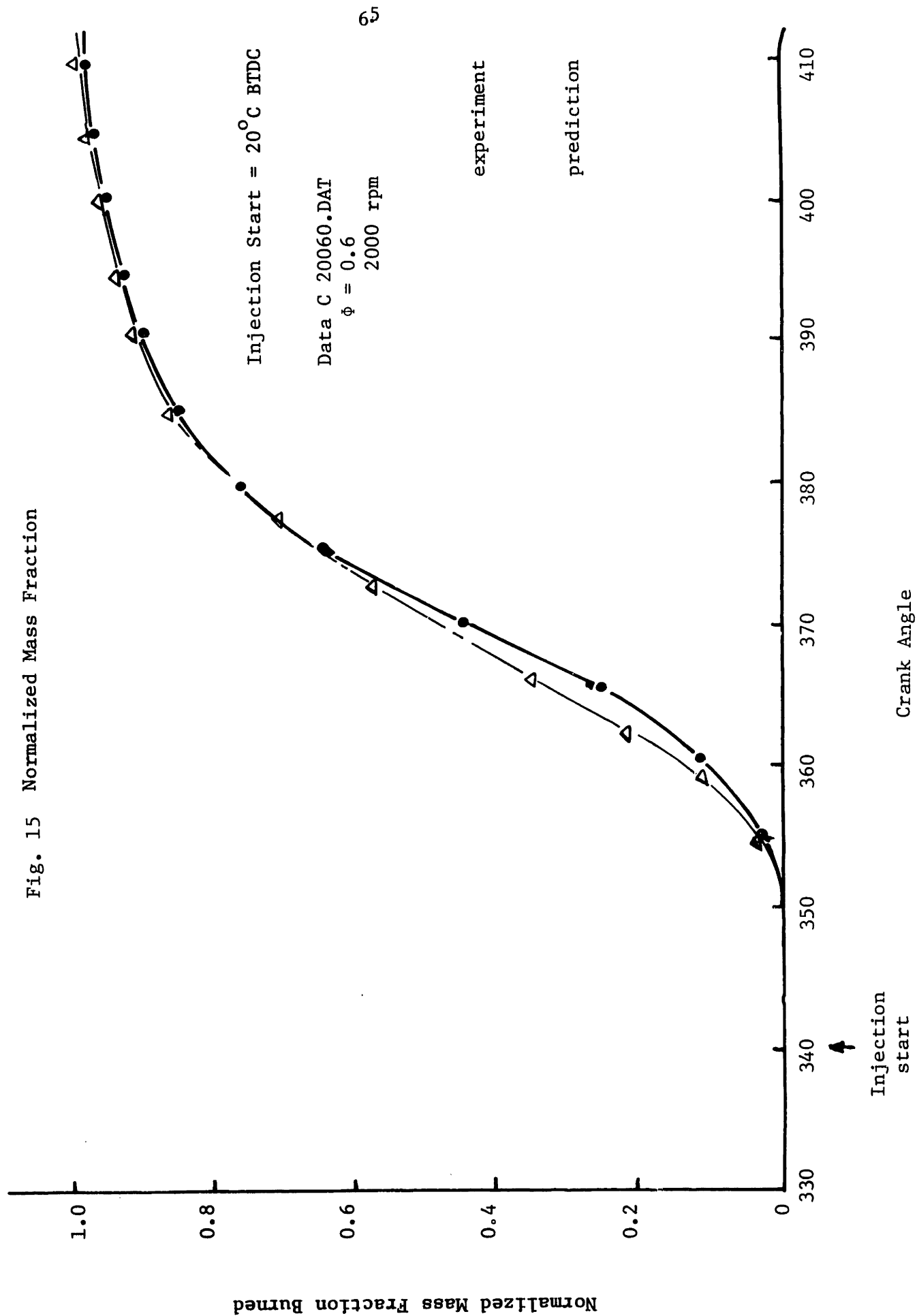
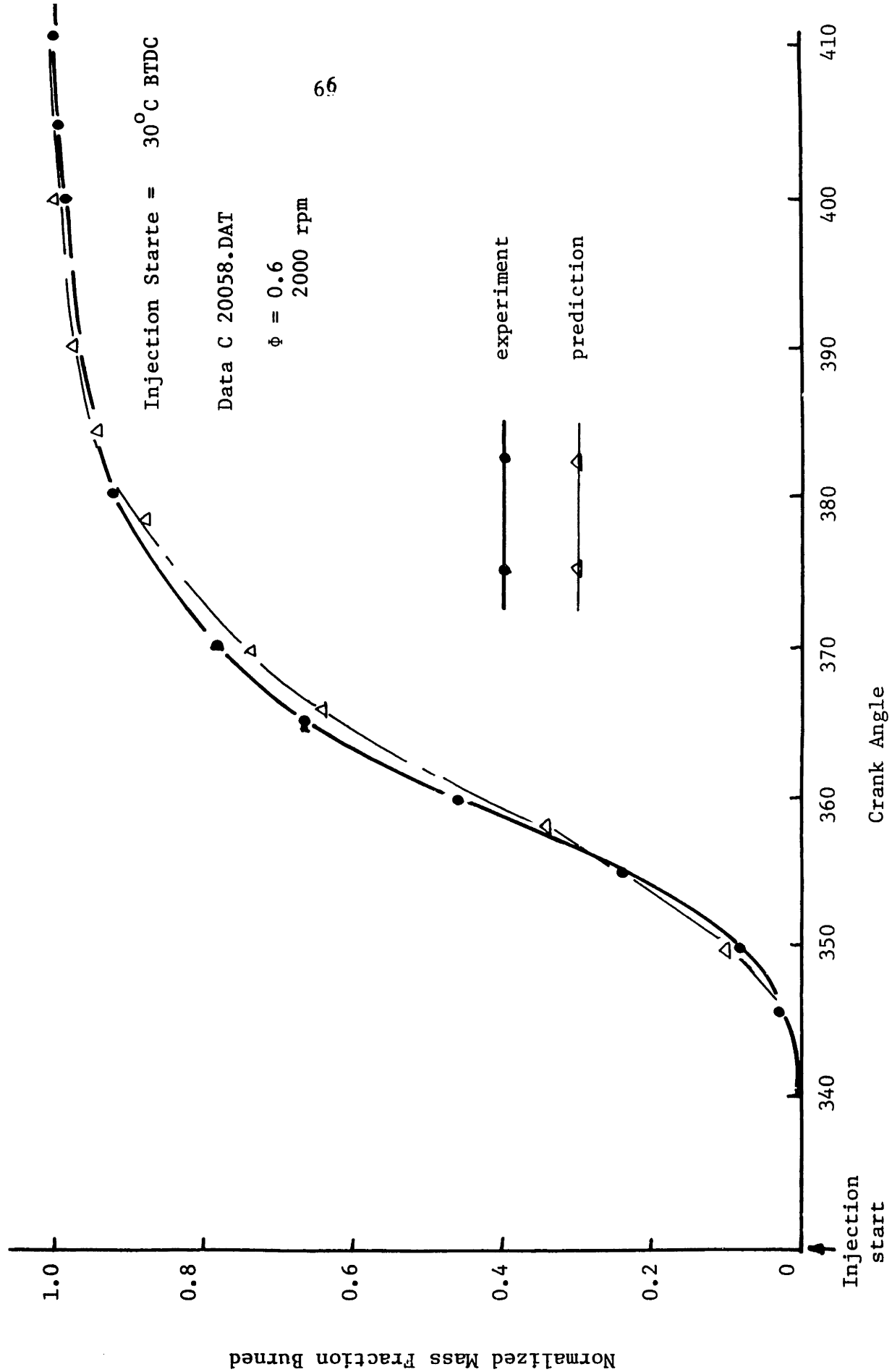


Fig. 16 Normalized Mass Fraction Burned

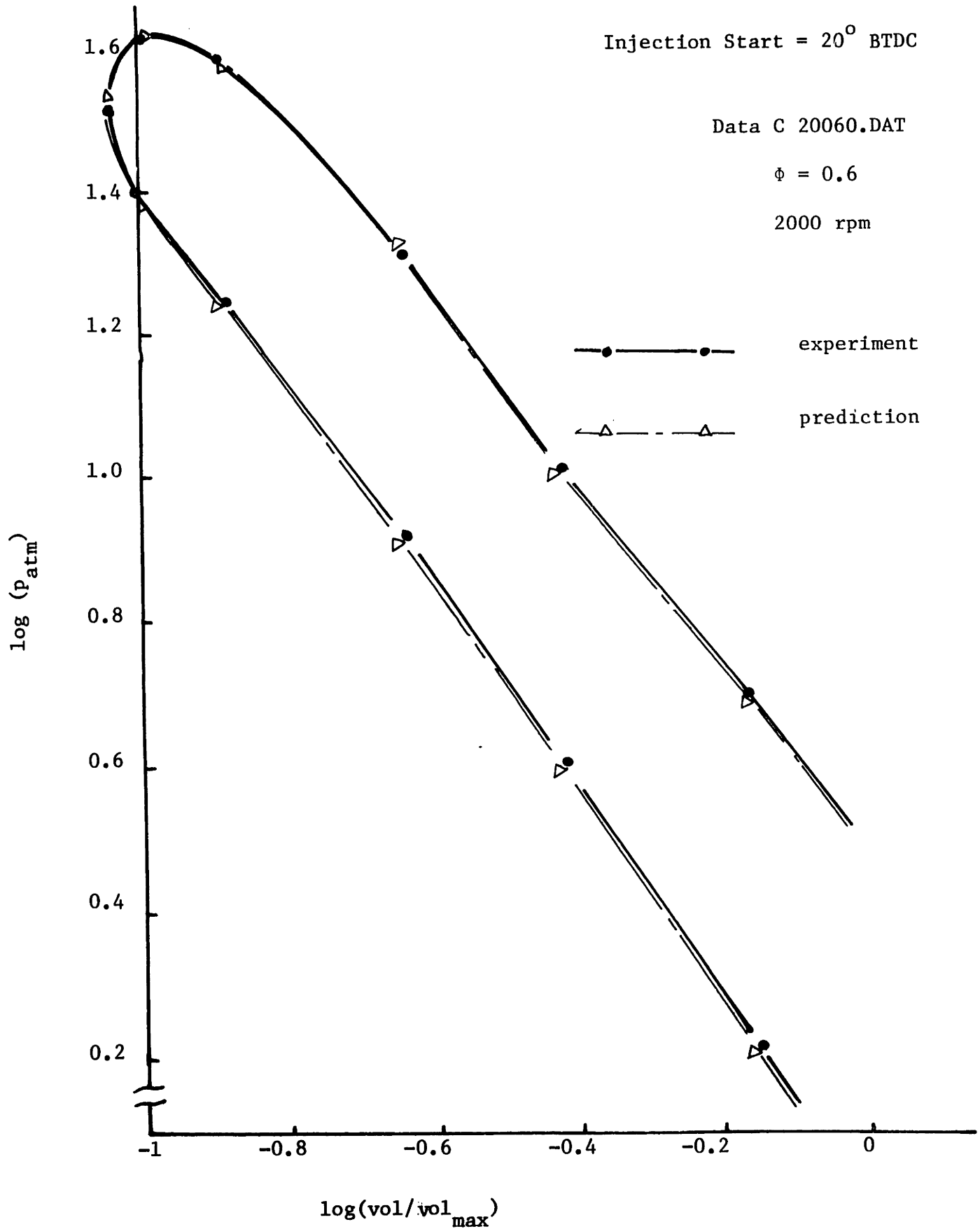


Injection Start = 20° BTDC

Data C 20060.DAT

 $\phi = 0.6$

2000 rpm

Fig. 17 $\log P - \log V$ Diagram ($\theta_1 = -20^{\circ}$)

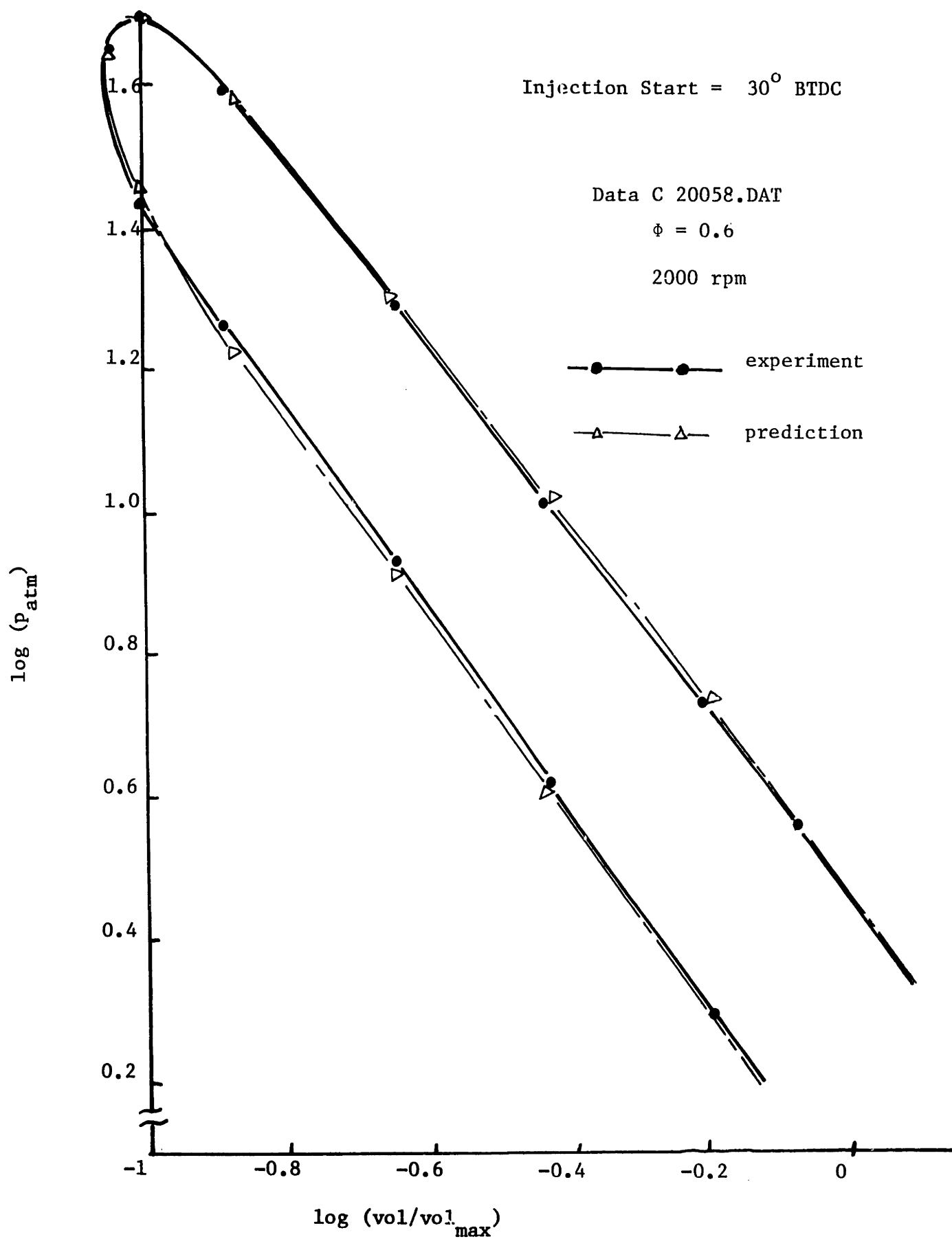


Fig. 18 log P - log V Diagram ($\theta_1 = -30^\circ$)

$\phi = 0.6$

2000 rpm

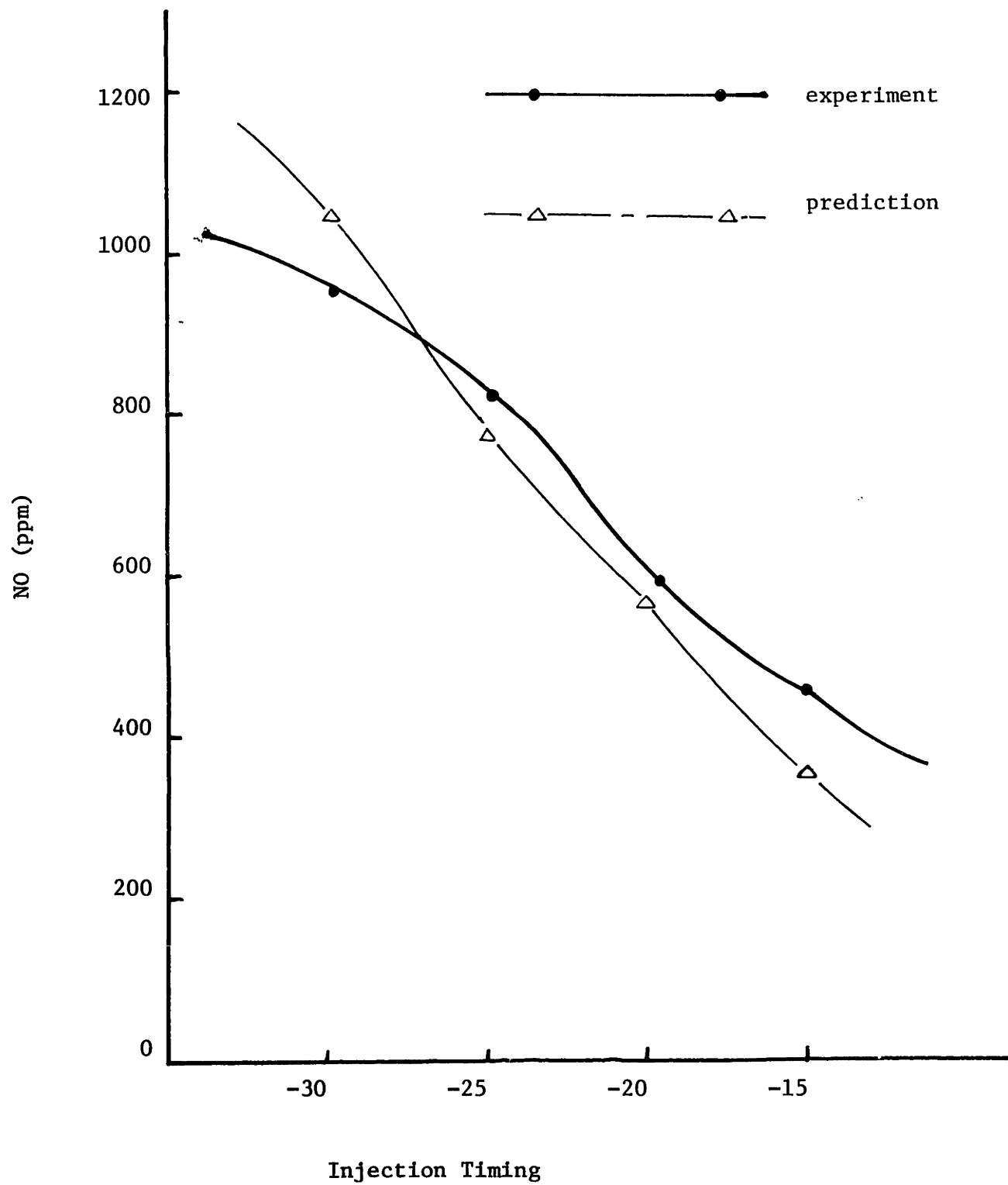


Fig. 19 Exhaust NO

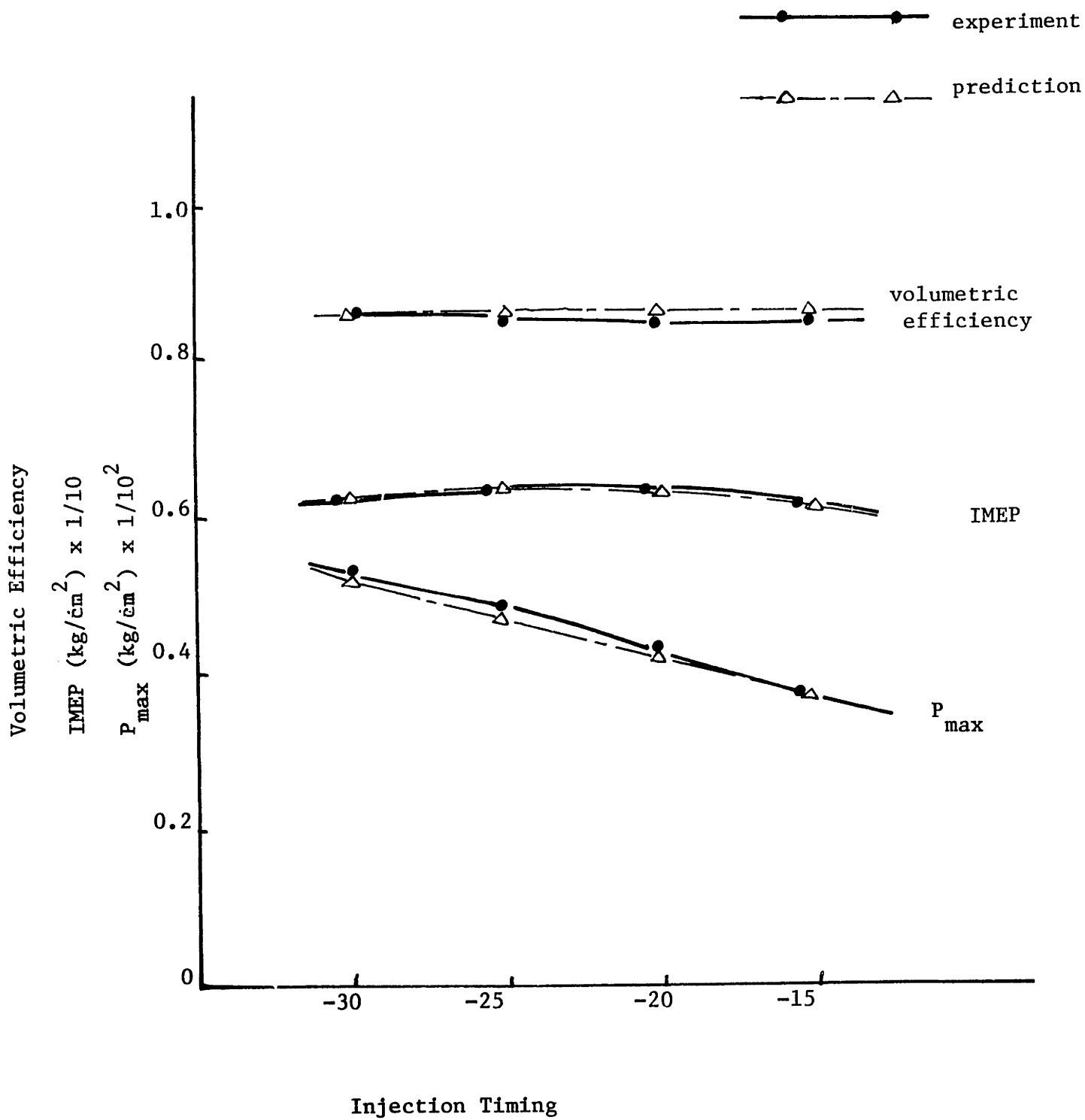


Fig. 20 Volumetric Efficiency, IMEP and $P_{\max}$

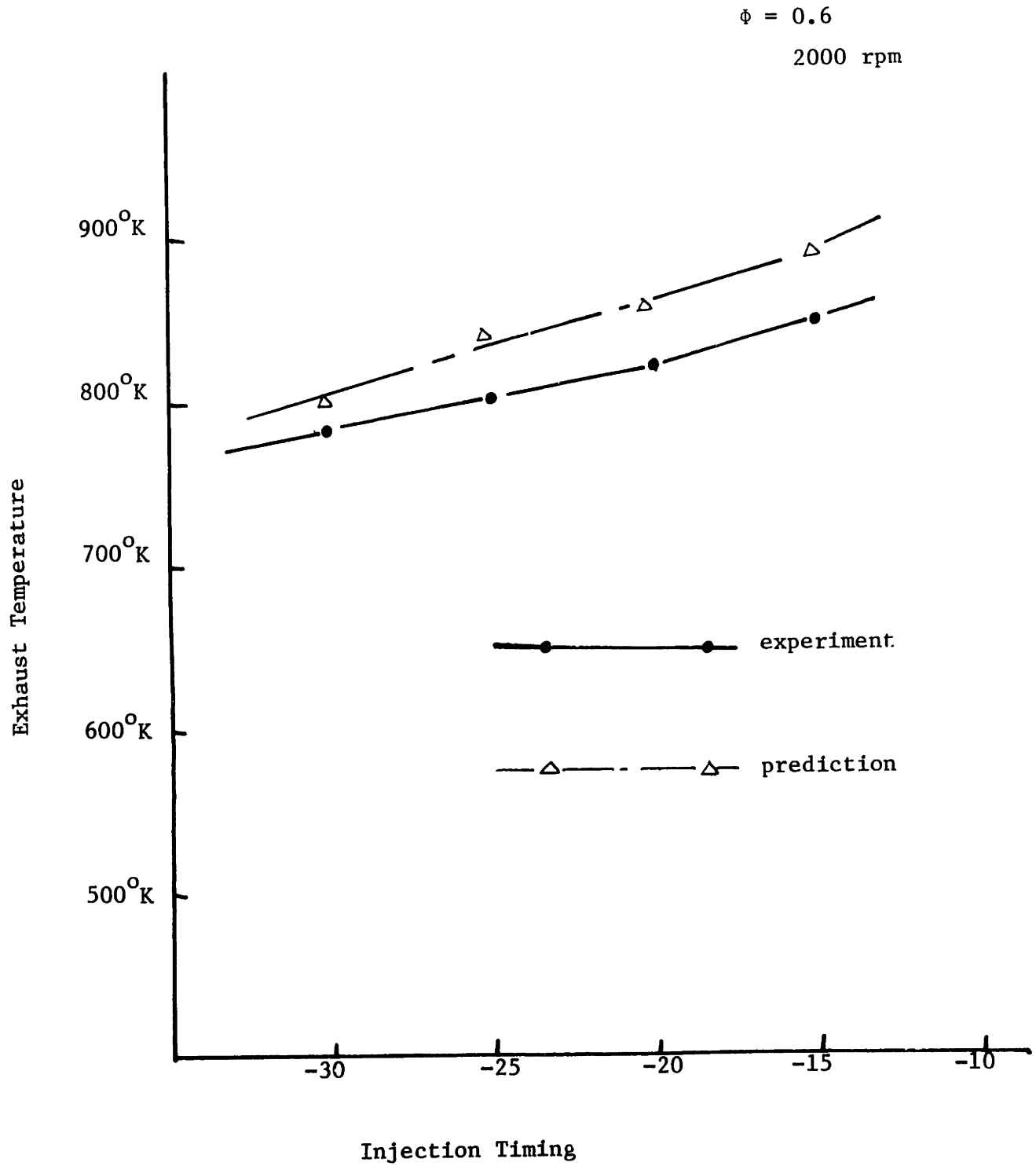


Fig. 21 Exhaust Temperature

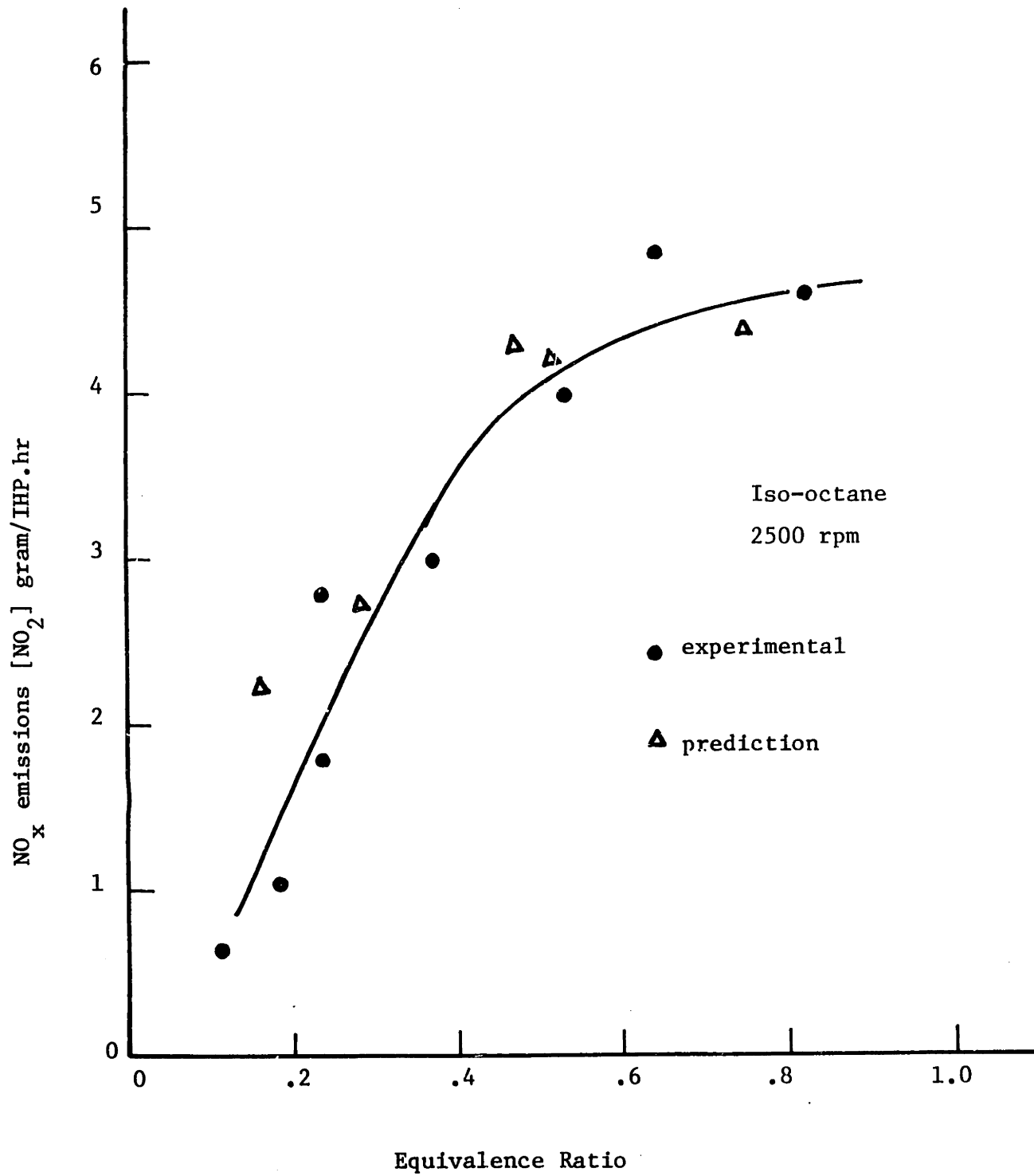


Fig. 22 NO_x vs. Equivalence Ratio

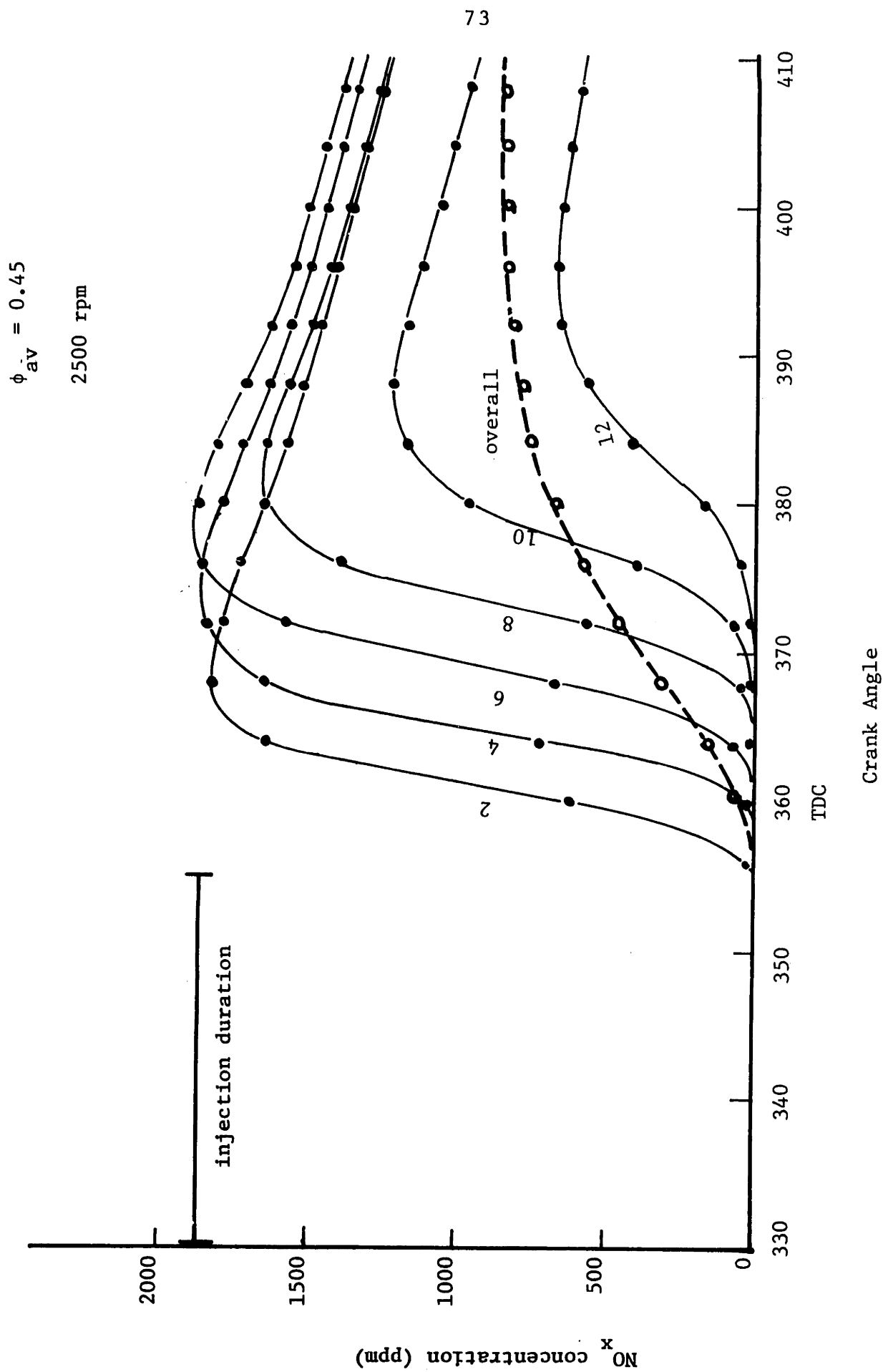


Fig. 23 NO Concentration in Each Element

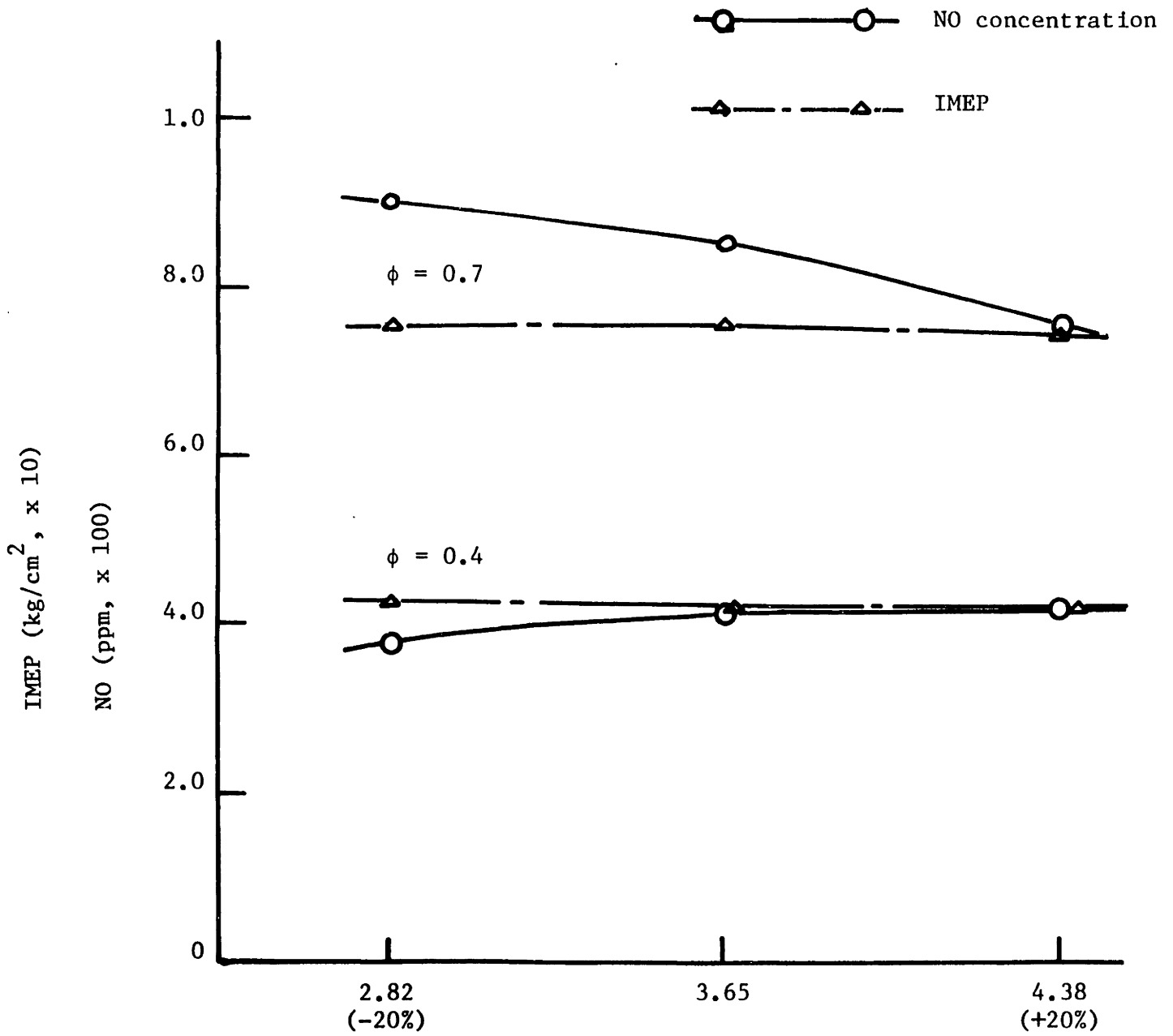


Fig. 24 The Effects of Swirl Ratio on Indicated Mean Effective Pressure and NO Concentration

Appendix A

Gas Exchange Process

During a discussion of exhaust and intake phases in the model description, it was seen that a knowledge of discharge-coefficient and the effective flow areas for both exhaust and intake valves were required. In this section, the experimental data on engine port steady flow tests (obtained from Texaco) will be reported.

Figure 13 and 14 shows the results from the tests mentioned above for the intake and exhaust port in the form of a plot of flow coefficient vs. valve lift to effective valve diameter ratio (L/D).

The mass flow rates through exhaust and intake valves have been treated as quasi-steady flow through a restriction. The governing equations can be written as follows:

$$\dot{M} = C_v A_v \left(\frac{RT_o}{P_o} \right) (\gamma RT_o)^{1/2} \left\{ \frac{2}{\gamma-1} \right\} \left[\left(\frac{P_2}{P_o} \right)^{2/\gamma} - \left(\frac{P_2}{P_o} \right)^{\frac{\gamma+1}{2(\gamma-1)}} \right]^{1/2}$$

For choked flow, with the condition for choked flow being:

$$\frac{P_o}{P_s} > \left(\frac{\gamma+1}{2} \right)^{\frac{\gamma}{\gamma-1}}$$

and

$$\dot{M} = C_v A_v \left(\frac{P_{oc}}{RT_{oc}} \right) (\gamma RT_o)^{1/2} \left\{ \left[\frac{2}{\gamma+1} \right]^{\frac{\gamma+1}{2(\gamma-1)}} \right\}^{1/2}$$

where C_v = valve discharge coefficient
 A_v = valve flow area
 P_o, T_o = upstream stagnation pressure and temperature
 P_2 = downstream static pressure

The logic to take care of the reverse flows through the valves has been put into the computer program. When there is reverse flow into the intake system (during valve overlap), the mass that flows past the intake valve is recorded. Its composition and temperature while in the intake system are assumed to be the same as those in the combustion chamber gas when intake valve opens. It has been assumed that, before any fresh charge can enter the chamber, all the mass that left the chamber during reverse flow is pulled back in first. For NO_x calculation NO_x mass transfer through the intake valve is taken into consideration.

Appendix B

Friction Loss

The following procedure for determining FMEP for a conventional spark ignition engine is taken from Bishop(33). The equations have been empirically correlated with data from engines ranging from single to eight cylinders, 4:1 to 17:1 compression ratio, and 0.75 to 2.5 bore to stroke ratio.

1. $FMEP_{\text{misc \& pumps}} = 0.39(N/1000)^{1.5}$
2. $FMEP_{\text{cam gear}} = [30 - (4N/1000)]GH^{1.75}/B^2S$
3. $FMEP_{\text{bearing}} = (KB/S)N/1000$
4. $FMEP_{\text{crank case}} = \Sigma \text{ Eqns. 1,2,3}$
5. $FMEP_{\text{blowby}} = [(P_a - P_1)/14.2]^{1/2} [1.72 R_c^{0.4} - (0.49 + 0.015 R_c) (N/1000)^{1.185}]$
6. $V_p/1000 = SN/6000$
7. $FMEP_{\text{viscous piston}} = (21.93M/BS) V_p/1000$

8. $FMEP_{\text{static ring tension}} = 2.11 S_n / B^2$
9. $FMEP_{\text{ring gas pressure}} = [(P_a - P_l) / 14.2] [2.35 S / B^2] [0.088 R_c + 0.182 R_c (1.33 - (0.121 V_P / 1000))]]$
10. $FMEP_{\text{total}} = \Sigma \text{ Eqns. } 4, 5, 7, 8, 9$

Symbols

- B: cylinder bore diameter (in)
- C: number of cylinder
- D: total engine displacement (in³)
- G: number of intake valves per cylinder
- H: intake valve head diameter (in)
- K: journal bearing size coefficient
- M: equivalent length of piston skirt (projected area of skirt ÷ cylinder bore diameter)
- N: revolutions per minute of crankshaft
- P_a : dry atmospheric pressure (psia)
- P: intake manifold vacuum (positive, when less than atmospheric pressure) (psig)
- R_c : compression ratio
- S: piston stroke (in)

V_p : mean piston velocity (ft/min)

n: total number of piston rings per cylinder

Appendix C

Thermodynamic Properties (hydrocarbon-air combustion)

The thermodynamic properties of the unburned and burned gases must be determined continuously during the entire cycle analysis. In most cases, the assumption of local chemical equilibrium can be justified and; in principal, for a given pressure and temperature, the mass action equations could be solved directly for species concentrations from which the desired thermodynamic properties could be derived. Alternatively, the species concentration which minimized the Gibbs free energy of the system could be calculated. Both approaches are quite involved and the calculations are expensive and time-consuming.

Our calculations use a computational method which is based on curve fitting data obtained from detailed thermochemical calculations to a functional form obtained from a consideration of carbon-air combustion.

This method was developed by M. Martin(21) and additional work done by S.D. Hires(34).

The following effects are taken into consideration by this method:

- i) Fuel vapor coefficient for unburned, air and residual gas mixtures.
- ii) Chemical dissociation effect above 1000°K for burned gases.

I Composition

. unburned gas

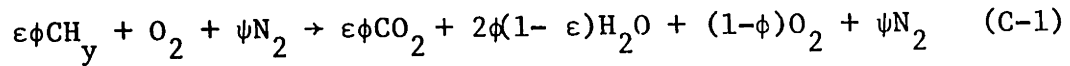
- i) fuel vapor
- ii) burned gas (residual gas)
- iii) air

. burned gas

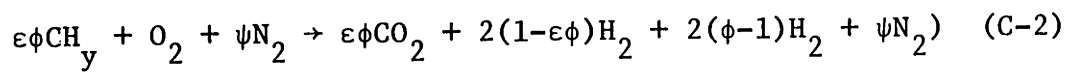
- i) burned gas

II Combustion reaction equations (hydrocarbon-air, under 1000°K)

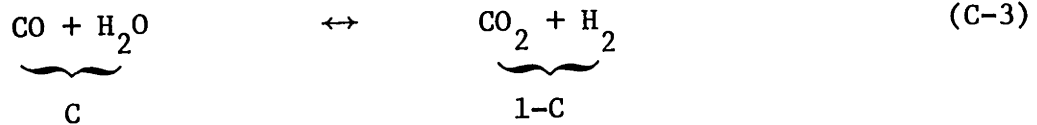
i) lean mixtures ($\phi < 1$)



ii) rich mixtures ($\phi > 1$)



and water gas reaction



This reaction is in equilibrium with equilibrium constant $K(T)$.

"C" is obtained by solving the following equation for its positive root.

$$(1-K) C^2 + 2[1-\epsilon\phi + K(\phi-1 + \epsilon\phi)]C - 2K\epsilon\phi(\phi-1) = 0 \quad (C-4)$$

$K(T)$ is determined by curve fitting JANAF Table data(35) over the temperature range 400-3200^oK and is given by:

$$\ln(K(T)) = 2.743 - 1.761/t - 1.611/t^2 + 0.2803/t^3 \quad (C-5)$$

where

$$t = T/1000 \quad (T = {}^{\circ}\text{K})$$

The coefficients for species are shown in Table C-1.

TABLE C-1

i	Species	$\phi \leq 1$	$\phi > 1$
1	CO ₂	$\epsilon\phi$	$\epsilon\phi - C$
2	H ₂ O	$2(1-\epsilon)\phi$	$2(1-\epsilon\phi) + C$
3	CO	0	C
4	H ₂	0	$2(\phi-1) - C$
5	O ₂	$1-\phi$	0
6	N ₂	ψ	ψ
sum		$(1-\epsilon) + 1 + \psi$	$(2-\epsilon)\phi + \psi$

where

ψ = the molar N:O ratio of the product

y = the molar H:C ratio of the fuel

$\epsilon = 4/(4+y)$

ϕ = the fuel-air equivalence ratio

III Grams of product per mole of O_2 reactant

$$\tilde{M} = \phi(8\epsilon+4) + 32 + 28\psi \quad (C-6)$$

IV Specific enthalpy and specific heat at constant pressure

$$\tilde{M} C_p = \sum_{i=1}^6 x_i \sum_{j=1}^4 (a_{ij} t^{j-1} + a_{5j}/t^2) \quad (C-7)$$

$$\tilde{M} h = \sum_{i=1}^6 x_i \sum_{j=1}^4 (a_{ij} t^j/j - a_{5j}/t + a_{6j}) \quad (C-8)$$

The coefficients a_{ij} are obtained by curve fitting JANAF Table data to the above functional form. The values of a_{ij} are given in Table C-2. The resultant C_p is in cal/g - $^{\circ}K$ and h is in Kcal/g.

TABLE C-2

Coefficients for Polynomial Fit to Thermodynamic Properties

Coefficients for $100^{\circ}\text{K} < T < 500^{\circ}\text{K}$

i	Species	a_{i1}	a_{i2}	a_{i3}	a_{i4}	a_{i5}	a_{i6}^*
1	CO_2	4.7373	16.653	-11.232	2.8280	.006767	-93.75793
2	H_2O	7.8097	- .20235	3.4187	-1.1790	.001436	-57.0800
3	CO	6.9738	- .82383	2.9420	-1.1762	.0004132	-27.196
4	H_2	6.9919	.16170	- .21821	.29682	-.016252	- .11819
5	O_2	6.2957	2.3884	- .031479	- .32674	.004359	.103637
6	N_2	7.0922	- 1.2958	3.2069	-1.2022	-.0003458	- .013967
7	$\text{C}_8\text{H}_{18}^{**}$	- .55313	181.62	-97.787	20.402	-.03095	-60.518

Coefficients for $500^{\circ}\text{K} < T < 6000^{\circ}\text{K}$

i	Species	a_{i1}	a_{i2}	a_{i3}	a_{i4}	a_{i5}	a_{i6}^*
1	CO_2	11.940	2.0886	- .47029	.037363	-.58945	-97.1418
2	H_2O	6.1391	4.6078	- .93560	.066695	.03358	-56.6259
3	CO	7.0996	1.2760	- .28775	.022356	-.15987	-27.7346
4	H_2	5.5557	1.7872	- .28813	.019515	.16118	.76498
5	O_2	7.8658	.68837	- .031944	-.002687	-.20139	- .89346
6	N_2	6.8078	1.4534	- .32899	.025610	-.11895	- .33184
7	$\text{C}_8\text{H}_{18}^{**}$	.55313	181.62	-97.787	20.402	-.03095	-60.518

*picked to give enthalpy datum at 0°K

**The coefficients apply to 2,2,4 trimethyl pentene (iso-octane). Different equations may be needed for different fuels.

V) Molecular weight of the burned mixture

$$\bar{M} = \begin{cases} \sim M / ((1-\epsilon)\phi + 1 + \psi) & \phi \leq 1 \\ \sim M / ((2-\epsilon)\phi + \psi) & \phi > 1 \end{cases}$$

APPENDIX D Computer Program

C 5. HEATP
 C 6. INPUT
 C 7. CALCU
 C 8. DELTA
 C 9. QCAL
 C 10. JET
 C 11. VGAS
 C 12. CONT
 C 13. ENT
 C 14. VOLCY
 C 15. HPRD
 C 16. CLDPRD
 C 17. DEPIVS
 C 18. DNDOT
 C 19. FOT3
 C 20. TWODIM
 C 21. UPRD
 C 22. PTCHEM
 C 23. NXNSOL
 C 24. FRICT FRICTIONS

C
 C

COMMON/EPROP/ IECHF(100),EFUEL(100),EANGL(100),FMWT(100),
 1 DHFUEL(100),DHLOS(100),DIEMAS(100),DIEMAS(100),
 1 ERGAS(100),ECP(100),FENTH(8,100),FMASS(8,100),EEQUI(8,100),
 1 EVOL(8,100),ETEMP(8,100),PCYL(8)
 COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,IF
 COMMON /STAT1/ PPM,JLAST,NJET,PHIO,FGX
 COMMON /TIMIG/ AINT0,AEXT0,AINTC,AFXTC,AFUELS,AFUFLE
 COMMON /GEOMT/ STROKE,BORE,CONL,VOLFAH,VCUP,RCUP,CYLN
 COMMON /SIJ1/ STGINT,STGEXT,STOEXT
 COMMON /HETPS/ NDIVID,TMETAL(10),QHTRC(10),ARF(10)
 COMMON /HETRI/ PRASE,TRASE,VRASE,COHT1,COHT2,COHT,RHR(10)
 COMMON /SIJ2/ TTGINT,TTGEXT,TTOEXT,TTQHT(10),TOHT(10),PS
 COMMON /FUELP/ FUEL,FXCAL,ZM,ZN,PSI,SAFC,VACAL
 COMMON /JETS/ RJET(50),HJET(50),AJET(50),BJET(50),THER(50),
 1 VRJET(50),VZJET(50),WJET(50),VJET(50),AINJ(50),RHJET(50),
 2 PITCH(50)
 COMMON /PLIME/ PMASS(50),BMASS(50),RPLUM(50),HRMASS(50)
 COMMON /JETDAT/ WSWIR,ALPHA,BETA,PHGAS
 COMMON /SUGAS/ FSWIR,WSWIR,SDECAY
 COMMON/CONR/ PPLUM0,FNTIR,RLFSP,ASPAR,TSCALF
 COMMON /OSDPE/ LPT,INP,LINCO,LINFST,ITEL,LITEL
 COMMON /NOXSP/ CONNO(100),PPMNO(100),WNO(100),SUMOM(100),PPMEXT
 DIMENSION ZMOFR(5),TMSPI(100)
 REAL*4 MRA2
 COMMON /FUEL/ AF(6),FMW,CX,HY,OZ,QLQVER
 COMMON/OXDANT/XI/CMPSTN/X(7),WRA2
 COMMON/CONTL/ ASTIN,ASTOL,ASTCR,ASTEX,ASTOV,PRININ,PRINCL,PRINEX,
 1 PRINOV
 COMMON/INFLO/ NINEF,XINEF(20),YINEF(20),AREIND,PINT,TINT,GINT,
 1 EQUINT,AREINT,XINV
 COMMON/EXFLO/NEXFF,XEYFF(20),YEYFF(20),AREEXD,PEXT,TEXT,GEXT,
 1 IGLFT,ILFT,DEXT,QFLOW,ELEFT,AREEXT,XEXV
 COMMON /AMRJE/ TAMR,PAVR
 COMMON /FRIOT/ RSKTPT,FCDE,RINGN,FMEP(10)
 DIMENSION HATEMP(50),PLTEMP(50),PLENT(50)
 DIMENSION YTEMP(10),YCP(10)
 DIMENSION YPCM(2),YPCM(2)

C

```

C DATA OF SPECIFIC HEAT AT CONSTANT PRESSURE VS TEMPERATURE
C DATA OF TEMPERATURE
C DATA XTEMP/
1 500.,1000.,1500.,2000.,2250.,2500.,2750.,3000.,3250.,3500./
C DATA OF SPECIFIC HEAT AT CONSTANT PRESSURE
C DATA YCP/
1 0.26,0.3,0.34,0.37,0.43,0.51,0.72,0.84,1.24,1.6/
C
C
C CARD READER AND LINE PRINTER
C INP=5
C LPT=6
C
C JCOND=1 VALVE OVERLAP PERIOD
C JCOND=2 INTAKE PROCESS
C JCOND=3 COMPRESSION PERIOD
C JCOND=4 COMBUSTION AND EXPANSION PERIOD
C JCOND=5 EXHAUST PROCESS
C
9001 CONTINUE
C ASTEP=2.0
C PSI=3.76
C
C INITIALIZE COMBUSTION CONDITION
C IECHE=1 NOT YET BURNED
C IECHE=2 PLUME IS DEVELOPING IN THE JET
C IECHE=3 PLUME IS FULLY DEVELOPED
C DO 1010 I=1,100
C IECHE(I)=1
C COMMO(I)=0.
1010 CONTINUE
C EPMAX=10.
C MAXITS=15
C JLAST=1
C LITFL=1
C RESFRK=0.
C
C INPUT SUBROUTINE
C CALL INPUT
C
C
C NOCUL=0 PERFORMANCE ONLY
C NOCUL=1 (NO) CALCULATION WILL BE DONE
C NOCUL=1
C DO YOU WANT NOX CALCULATION?
C READ(INP,302) NOCUL,PPMEXT
C
C CALCULATION STARTING CRANK ANGLE AND ENDING CRANK ANGLE
C READ(INP,23) ANGLES,ALAST
C DEL=ZN/ZM
C EFUEL(1)=0.
C ENTIN1=ENT(TINT,FOUJINT,SAFC)
C IF=1
C ANGLE=ANGLES
C ANGLE1=ANGLES
C CALL VOLCY(ANGLE,EVOL(2,1),DVCYL,STROKE,BORE,CONL,VCLFAR,VCIIP)
C VCULO=EVOL(2,1)
C FENTH(2,1)=ENT(ETEMP(2,1),EEQUI(2,1),SAFC)
C ENTIN2=EENTH(2,1)

```

```

      CALL HPRD(PCYL(2),ETEMP(2,1),FFQHT(2,1),DEL,PST,DJM,DUM,DUM,DUM,
1  DUM,DUM,EMWT(1),FRGAS(1),CVRG,DUM)
      FCP(1)=FRGAS(1)/41.443+CVHG
      FMASS(2,1)=PCYL(2)*EVOL(2,1)/(FRGAS(1)*ETEMP(2,1))

```

C

C INITIAL CONDITION

```

100 TTGINT=0.
    TTGEXT=0.
    TTOEXT=0.
    IGLEFT=0
    TMAX=0.
    PMAX=0.
    PS=0.
    PSIN=0.
    PSEX=0.
    JCOND=0
    ENTINT=ENTIN2
200 CONTINUE
    DO 10 I=1,NDIVID
    TQHT(I)=0.
10 TQHT(I)=0.

```

C

C SWIRL DECAYING FACTOR FSWIR=1. AT THE TIME OF INTAKE VALVE CLOSING

```

    FSWIR=1.
3000 CONTINUE
    PCYLO=PCYL(2)

```

C

CALL OPERA

C

C PUNGE KUTTA METHOD

```

    CALL PUNGF(ENTINT)
    ANGLE1=ANGLE1+ASTEP
    TTGINT=TTGINT+STGINT*ASTEP
    TTGEXT=TTGEXT+STGEXT*ASTEP
    TTOEXT=TTOEXT+STOEXT*ASTEP
    DO 3900 I=1,NDIVID
3900 TQHT(I)=TQHT(I)+TQHT(I)*ASTEP

```

C

C CHECK THE INTAKE FLOW

```

    IF(JCOND.GE.3) GO TO 570
    IF(TTGINT.GT.0.) GO TO 572

```

C

C INTAKE FLOW IS RESIDUAL GAS

```

    ENTINT=ENTIN2
    GO TO 570

```

C

C INTAKE FLOW IS FRESH AIR

```

572 ENTINT=ENTIN1
570 CONTINUE
    CALL VOLCY(ANGLE1,VCYLN,DVCYL,STROKE,BDRF,CONL,VCLER,VCUP)
    DPS=((PCYL(2)+PCYLO)/2.-PAMB)*(VCYLN-VCYLO)*CYLN*RPM/900000.
    VCYLO=VCYLN
    PS=PS+DPS
    IF(JCOND=2) 580,580,590
580 PSIN=PSIN+DPS
    GO TO 530
590 IF(JCOND=5) 530,595,530
595 PSEX=PSEX+DPS
530 DO 16 I=1,NDIVID
16 TQHT(I)=TQHT(I)+TQHT(I)*ASTEP

```

```

      IF (IGLFFT) 500,500,510
500  GLEFFT=GLEFT-STGEXT
      IF (GLEFFT) 520,520,510
520  IGLFFT=1
510  CONTINUE
      IF (JCOND.NF.4) GO TO 4500
C
C  COMBUSTION ROUTINE
C
C  ESTIMATE THE PLUME TEMPERATURE
      DO 3700 I=1,IF
      IF (IECHE(I).EQ.2) GO TO 3400
      URTEMP(I)=FTEMP(2,I)
      PLTEMP(I)=FTEMP(2,I)
      PLENT(I)=FENTH(2,I)
      GO TO 3700
3400  ENTJET=FENTH(2,1)
      CALL TWODIM(10,XTEMP,YCP,PLTEMP(I),PLCP1)
      PLCP=PLCP1
      ENTPL=(EENTH(2,1)*EMASS(2,1)-ENTJET*(EMASS(2,1)-PMASS(1)))/
1  PMASS(1)
      DPLT=(ENTPL-PLENT(I))/PLCP
      DO 3820 J=1,3
      PLT=PLTEMP(I)+DPLT
      TDUM2=PLTEMP(I)+DPLT/3.
      TDUM3=PLTEMP(I)+DPLT*2./3.
      TDUM4=PLTEMP(I)+DPLT
      CALL TWODIM(10,XTEMP,YCP,TDUM2,CPDUM2)
      CALL TWODIM(10,XTEMP,YCP,TDUM3,CPDUM3)
      CALL TWODIM(10,XTEMP,YCP,TDUM4,CPDUM4)
      DPLT=(ENTPL-PLENT(I))*(1./PLCP1+2./CPDUM2+2./CPDUM3+1./CPDUM4)/6.
3820  CONTINUE
      PLENT(I)=ENTPL
      PLTEMP(I)=PLT
3700  CONTINUE
      IF (NOCUL.FO.0) GO TO 4500
C
C  CALCULATION OF NOX CHANGE BY MASS TRANSFER
C
      DO 4012 I=2,IF
      CONNO(I)=CONNO(I)+CONNO(1)*SUMDM(I)/(EMASS(2,1)-SUMDM(1))
4012  CONTINUE
      CONNO(1)=CONNO(1)+CONNO(1)*SUMDM(1)/(EMASS(2,1)-SUMDM(1))
      DO 4010 I=1,IF
      TMSPI(I)=EMASS(2,1)/EMWT(I)
      IF (IECHE(I).EQ.1) GO TO 4020
      IF (IECHE(I).EQ.3) GO TO 4040
      PLSPI=PMASS(I)/EMWT(I)
      GO TO 4050
4040  PLSPI=TMSPI(I)
4050  CONTINUE
      CALL EQIB(PLTEMP(I),PCYL(2),FFQUI(2,I),IFLAG,ZMOFR)
      IF (PLTEMP(I).GT.2400.) GO TO 4022
      IJNOM=1
      GO TO 4024
4022  IJNOM=4
4024  ASTNO=ASTEP/FLOAT(IJNOM)
      DO 4026 IJNO=1,IJNOM
      CALL DMOST(PLTEMP(I),PCYL(2),PLSPI,ZMOFR,IIFLAG,CONNO(I),
1  DCONNO)

```

```

CONNO(I)=CONNO(I)+DCONNO*ASTNO/(RPM*6.)
4026 CONTINUE
4020 PCONNO(I)=1000000.*CONNO(I)/TMSPI(I)
WNO(I)=30.*CONNO(I)
4010 CONTINUE
TWSPI=0.
TCONNO=0.
TTMSPI=0.
TWNO=0.
DO 4030 I=1,IF
TCONNO=TCONNO+CONNO(I)
TTMSPI=TTMSPI+TMSPI(I)
TWNO=TWNO+WNO(I)
4030 CONTINUE
TRPM=1000000.*TCONNO/TTMSPI
4500 CONTINUE
LINECO=LINECO-1
IF(LINECO) 2000,2000,2010

C
C POINT OUT
2000 GO TO (2100,2200,2300,2400,2500),JCOVD
C
C VALVE OVERLAP PERIOD
2100 GGNT=STGINT*CYLN*6.*RPM
GGXT=STGEXT*CYLN*6.*RPM
HTRS1=-TQHTR(1)
HTRS2=-TTQHTR(1)
WRITE(LPT,2900) ANGLE1,PCYL(2),ETEMP(2,1),EVOL(2,1),PS,
1 FMASS(2,1),HTRS1,HTRS2,AREINT,GGNT,AREEXT,GGXT
GO TO 9100

C
C INTAKE PROCESS
2200 GGNT=STGINT*CYLN*6.*RPM
HTRS1=-TQHTR(1)
HTRS2=-TTQHTR(1)
WRITE(LPT,2910) ANGLE1,PCYL(2),ETEMP(2,1),EVOL(2,1),PS,
1 FMASS(2,1),HTRS1,HTRS2,AREINT,GGNT
GO TO 9100

C
C COMPRESSION PROCESS
2300 SPAT=WSWIR*180./(3.1416*6.*RPM)
HTRS1=-TQHTR(1)
HTRS2=-TTQHTR(1)
WRITE(LPT,2920) ANGLE1,PCYL(2),ETEMP(2,1),EVOL(2,1),PS,
1 FMASS(2,1),HTRS1,HTRS2,FSWIR,SRAT
GO TO 9100

C
C COMBUSTION PERIOD
C EXPANSION PERIOD
2400 CONTINUE
IF(IE.EQ.1) GO TO 2300
HTRS1=-TQHTR(1)
HTRS2=-TTQHTR(1)
TRATBU=0.
DO 2410 I=2,IF
2410 TRATBU=TRATBU+HFMASS(I)
TRATBU=TRATBU/FUFL
SPAT=WSWIR*180./(3.1416*6.*RPM)
IF(MOCUL.EQ.0) GO TO 5010
TWNQXX=TWNQ*10.**6

```



```

WRITE(LPT,2930) ANGLE1,PCYL(2),PS,FSWIR,SRAT,HTRS2
WRITE(LPT,2931) TRATH,VCYLV,PHIO,TPPM,TWNXXX,HTRS1
GO TO 5015
5010 WRITE(LPT,2930) ANGLE1,PCYL(2),PS,FSWIR,SRAT,HTRS2
WRITE(LPT,2932) TRATH,VCYLV,PHIO, HTRS1
5015 DO 5020 I=1,IF
HHL0S=HHL0S(I)
IF(NOCUL.EQ.0) GO TO 5022
IF(I.EQ.1) GO TO 5024

C
C NOX AND JET ELEMENT
AJF=AJET(I)*180./3.1416
ACQ=THEP(I)*180./3.1416
EMASMG=EMASS(2,I)*1000.
PMASMG=PMASS(I)*1000.
RMASMG=RMASS(I)*1000.
RATBU=HRMASS(I)/EFUFL(I)
WNOMMG=WNO(I)*10.**6
WRITE(LPT,2936) I,IFCHE(I),ETEMP(2,I),PLTEMP(I),RATBU
1 EMASMG, PMASMG, RMASMG, EVOL(2,I),EEQUI(2,I),ECP(I).
2 EENTH(2,I),PPMNO(I),WNOMMG,RJET(I),HJET(I),AJE,BJET(I),ACQ,HHL0S
GO TO 5020

C
C NOX AND AIR
5024 EMASMG=EMASS(2,I)*1000.
WNOMMG=WNO(I)*10.**6
WRITE(LPT,2937) I,IFCHE(I),ETEMP(2,I),
1 EMASMG, EVOL(2,I),EEQUI(2,I),ECP(I).
2 EENTH(2,I),PPMNO(I),WNOMMG, HHL0S
GO TO 5020

C
C PERFORMANCE AND JET
5022 IF(I.EQ.1) GO TO 5026
AJF=AJET(I)*180./3.1416
ACQ=THEP(I)*180./3.1416
EMASMG=EMASS(2,I)*1000.
PMASMG=PMASS(I)*1000.
RMASMG=RMASS(I)*1000.
RATBU=HRMASS(I)/EFUFL(I)
WRITE(LPT,2934) I,IFCHE(I),ETEMP(2,I),PLTEMP(I),RATBU
1 EMASMG, PMASMG, RMASMG, EVOL(2,I),EEQUI(2,I),ECP(I).
2 EENTH(2,I), RJET(I),HJET(I),AJE,BJET(I),ACQ,HHL0S
GO TO 5020

C
C PERFORMANCE AND AIR
5026 EMASMG=EMASS(2,I)*1000.
WRITE(LPT,2938) I,IFCHE(I),ETEMP(2,I),
1 EMASMG, EVOL(2,I),EEQUI(2,I),ECP(I).
2 EENTH(2,I), HHL0S
5020 CONTINUE
GO TO 4100

C
C EXHAUST PROCESS
2500 GGXT=STGEXT*CYLN*6.*PPM
HTRS1=-TQHTR(1)
HTRS2=-TQHTR(1)
WRITE(LPT,2940) ANGLE1,PCYL(2),ETEMP(2,1),EVOL(2,1),PS,
1 EMASS(2,1),HTRS1, HTRS2, AREFFT,GGXT
GO TO 2100
2900 FORMAT(1H, 'F5.1,

```

```

1      1X,F6.2,1X,F5.0,1X,F6.0,1X,F6.2,2X,F8.3,
1      E11.3 ,E11.3 ,1X,F6.2,1X,F7.2,2X,F6.2,1X,F7.2)
2910 FORMAT(1H ,F5.1,
1      1X,F6.2,1X,F5.0,1X,F6.0,1X,F6.2,2X,F8.3,
1      F11.3 ,F11.3 ,1X,F6.2,1X,F7.2 )
2920 FORMAT(1H ,F5.1,
1      1X,F6.2,1X,F5.0,1X,F6.0,1X,F6.2,2X,F8.3,
1      F11.3,F11.3,1X,F6.3,1X,F6.2)
2930 FORMAT(/,1X,F5.1,2X,IPRESS=,F6.2,1X,IPSE=,F6.1,1X,IPSWIP=,F6.3,
1      1X,ISRT=,F6.3,1X,ISUM.H.REJ=,E9.3)
2931 FORMAT(2X,5HTOTAL,14X,F7.3,21X,2F7.2,14X,F7.0,F7.0,30X,E9.2)
2932 FORMAT(2X,5HTOTAL,14X,F7.3,21X,2F7.2,14X, 44X,E9.2)
2934 FORMAT(2X,I2,1X,I2,2F7.0,F7.3,3F7.1,2F7.2,F7.3,F7.1,14X,
1      F6.1,F6.2,F6.0,F6.3,F6.0,E9.2)
2936 FORMAT(2X,I2,1X,I2,2F7.0,F7.3,3F7.1,2F7.2,F7.3,F7.1,F7.0,F7.2,
1      F6.1,F6.2,F6.0,F6.3,F6.0,E9.2)
2937 FORMAT(2X,I2,1X,I2, F7.0,14X,F7.1,14X,2F7.2,F7.3,F7.1,F7.0,
1      F7.0, 18X,12X,E9.2)
2938 FORMAT(2X,I2,1X,I2, F7.0,14X,F7.1,14X,2F7.2,F7.3,F7.1,
1      22X,12X,E9.2)
2940 FORMAT(1H ,F5.1,
1      1X,F6.2,1X,F5.0,1X,F6.0,1X,F6.2,2X,F8.3,
1      F11.3, E11.3 ,1X,F6.2,1X,F7.2)
9100 CONTINUE
      LTNFCO=LINFST
2010 IF(PMAX-PCYL(2)) 7000,7030,7030
7000 PMAX=PCYL(2)
      PMAXAN=ANGLE1
7030 CONTINUE
C
C IF THE TEMPERATURES OF EVERY ELEMENTS ARE BELOW TEMLOW(AROUND 1700K).
C THERE WILL BE NO CHANGE IN NO VALUE.
C WE WILL CONSIDER ONLY ONE AVERAGE ELEMENT.
      TEMLOW=2200.
      IF(JCOND.NE.4) GO TO 7300
      AAN=ANGLE1-(AFUELE+30.)
      IF(AAN.LT.0.) GO TO 7300
      IF(IE.F0.1) GO TO 7300
      IF(TEMP(2,2).GT.TEMLOW) GO TO 7300
      IF(TEMP(2,IE).GT.TEMLOW) GO TO 7300
C
C
C CALCULATE THE TOTAL MASS AND ENTHALPY
      TENTH=0.
      TMASS=0.
      DO 7320 I=1,IF
      TENTH=TENTH+FEENTH(2,I)*FMASS(2,I)
      TMASS=TMASS+EMASS(2,I)
7320 CONTINUE
C
C CALCULATE THE AVERAGE ENTHALPY
      AVENT=TENTH/TMASS
C
C CALCULATE THE AVERAGE TEMPERATURE
C FIRST FIND OUT THE ELEMENT WHICH ENTHALPY IS CLOSE TO THE
C AVERAGE ENTHALPY
      DEFTM=1000.
      IT=1
      DO 7330 I=1,IF
      DEFT=ABS(AVENT-FEENTH(2,I))
      IF(DEFT.LT.DEFT) GO TO 7330

```

```

      DENTM=DENT
      IT=1
7330 CONTINUE
C
C  DEFINE THE NEW PROPERTIES
      FTEMP(2,1)=FTEMP(2,IT)+(AVENT-FFNTH(2,IT))/FCP(IT)
      FFQUI(2,1)=PHIQ
      FFNTH(2,1)=AVFNT
      FMASS(2,1)=TMASS
      CALL HPROD(PCYL(2),FTEMP(2,1),FFQUI(2,1),DFL,PSI,ENTHLP,CSURP,
1 CSUST,RHO,DRHODT,DRHODP,EMWT(1),FRGAS(1),CVBG,FBGR)
      FCP(1)=FRGAS(1)/41.443+CVBG
      EVOL(2,1)=VCYLN
      IF=1
      WRITE(LPT,7340)
      WRITE(LPT,7342) PCYL(2),FTEMP(2,1),FFQUI(2,1),FFNTH(2,1),
1 FMASS(2,1)
      IF(NOCUL.EQ.0) GO TO 7331
C
C  NOX AMOUNT WILL BE DEFINED.
C  EXHAUST NOX ON MASS BASE
      ANOXEX=TWNQ*ITGINT/TMASS*8PM/120.
      WRITE(LPT,7450) TPRM,ANOXEX
7331 CONTINUE
      WRITE(LPT,7420)
      WRITE(LPT,7430)
7340 FORMAT(/,10X,***EXPANSION PROCESS IS CALCULATED AS ONE FLEMENT**
1*)
7342 FORMAT(15X,18HPRESSURE          = ,F10.2,'ATA',/,
1 15X,18HAV. TEMPERATURE = ,F10.1,'K DEG',/,
2 15X,18HAV. EQUI. RATIO = ,F10.3,/,
3 15X,18HAV. ENTHALPY      = ,F10.2,'CAL/G',/,
4 15X,18HTOTAL MASS        = ,F10.4,'G')
7420 FORMAT(/2X,4HTHEO.3X,4H P ,3X,4H T ,3X,4H V ,3X,4HWORK.
1 3X,7HCYL.MAS,3. 4H HEAT TRANSFER,7X,4HFSWR,3X,4HSP)
7430 FORMAT(2X ,4HDFG ,3X,4HATA ,3X,4H K ,2X,5HOM**3,3X,4H PS ,
1 3X,7H G ,3X,15H CAL/A CAL ,11X,3X,4HPRM)
7450 FORMAT(/,10X,***EXHAUST NOX***,/,
1 15X,15HNOX CONCEN. = ,F10.1,'PPM',/,
2 15X,15HTOTAL MASS = ,E12.3,'G')
7300 CONTINUE
      IF(ANGLE1-ALAST) 7040,7050,7050
7040 GO TO 3000
7050 CONTINUE
      ITFXT=1
      QMANI=ITQEXT/ITGEXT
      TEXT=700.
7240 DO=ENT(TEXT,FFQUI(2,1),SAFC)-QMANI
      PQ=DO/QMANI
      IF(ABS(RQ)-0.003) 7220,7220,7230
7230 IF(ITFXT-2) 7200,7210,7210
7200 ITFXT=2
      XPRM(1)=700.
      YPRM(1)=PQ
      TEXT=800.
      GO TO 7240
7210 CALL CONT(TEXT,PQ,0.,0.,XPRM,YPRM,ITFXT)
      ITFXT=ITFXT+1
      IF(ITFXT-20) 7240,7220,7220
7220 CONTINUE

```

```

      ITFL=ITFL+1
      WRITE(LPT,4090) TEXT
      GO TO 7060
7070 CONTINUE
      IF (ITFL-LITEL) 7260,7260,7060
7260 ANGLE1=ANGLE1-720.
      GO TO 100
7060 CONTINUE
      VSTROKE=BORF*HORE*STROKE/4.*3.1416
      CALL FRICT
      WRITE(LPT,4092) FMFP(2),FMFP(3),FMFP(4),FMFP(5),FMFP(6),
1 FMFP(7),FMFP(8),FMFP(1)
      AIMFP=PS/VSTROKE*7500000./(RPM/120.)
      PIMFP=PSIN/VSTROKE*7500000./(RPM/120.)
      PEMFP=PSFX/VSTROKE*7500000./(RPM/120.)
      RMFP=AIMFP-FMFP(1)
      RHP=RMFP*VSTROKE/7500000.*(RPM/120.)
      AISFC= FUEL*3600./PS*RPM/120.
      RSFC= FUEL*3600./RHP*RPM/120.
      WRITE(LPT,4000) PIMFP,PSIN
      WRITE(LPT,4010) PEMFP,PSFX
      WRITE(LPT,4020) AIMFP,PS,AISFC
      WRITE(LPT,4030) RMFP,RHP,RSFC
      RHERE=TTQHTR(1)/(FUEL*(FCAL-VACAL))
      PERMI=CYLN*RPM/2.
      DO 17 I=1,NDIVID
17 TTQHTR(I)=TTQHTR(I)*PERMI
      WRITE(LPT,4055)
      WRITE(LPT,4056) (TTQHTR(I),I=1,NDIVID),RHERE
      WRITE(LPT,4070) PMAX,PMAXAN
23 FORMAT(2F10.0)
301 FORMAT(I2)
302 FORMAT(12,F10.0)
4000 FORMAT(///,10X,'PIMFP=',1,F8.2,'G/CM**2',5X,'PSIN=',1,F8.2,'HP')
4010 FORMAT(1H ,10X,'PEMFP=',1,F8.2,'G/CM**2',5X,'PSFX=',1,F8.2,'HP')
4020 FORMAT(1H ,10X,'AIMFP=',1,F8.0,'G/CM**2',5X,'IHP=',1,F8.2,'HP',
1 5X,'AISFC=',1,F8.2,'G/HP.HR')
4030 FORMAT(1H ,10X,'RMFP=',1,F8.0,'G/CM**2',5X,'RHP=',1,F8.2,'HP',
1 5X,'RSFC=',1,F8.2,'G/HP.HR')
4055 FORMAT(1H ,10X,'HEAT REJECTION= CAL/MIN')
4056 FORMAT(1H , 9X,15HTOTAL H. REFJ = ,F10.4,/,
1 10X,15HCYL. LINER = ,F10.4,/,
2 10X,15HPISTON TOP = ,F10.4,/,
3 10X,15HPISTON CUP = ,F10.4,/,
4 10X,15HCYL. HEAD = ,F10.4,/,
5 10X,15HINT. VALVE = ,F10.4,/,
6 10X,15HFXH. VALVE = ,F10.4,/,
7 7X,18HHEAT REFJ./FUEL = ,F10.3)
4070 FORMAT(1H ,10X,'MAX CYL PRESS=',F10.1,'AT',F5.1,'DEG. CA')
4090 FORMAT(1H ,10X,'EXHAUST TEMPERATURE=',F8.1,'KDEG')
4092 FORMAT(///,10X,'PREDICTION OF THE FRICTION LOSS**',/,
1 5X,16HISC. AND PUMPS= , F12.3,7HG/CM**2,/,
1 5X,16HCAM GEAR = , F12.3,7HG/CM**2,/,
1 5X,16HREADING = , F12.3,7HG/CM**2,/,
1 5X,16HRLD. AY = , F12.3,7HG/CM**2,/,
1 5X,16HVISCOUS PISTON = , F12.3,7HG/CM**2,/,
1 5X,16HPISTON TENSION = , F12.3,7HG/CM**2,/,
1 5X,16HPISTON GAS PRESS = , F12.3,7HG/CM**2,/,
14X,'-----',/,
1 5X,16HTOTAL LOSS = , F12.3,7HG/CM**2)

```

```
4001 FORMAT(2X,2I2,7E12.4)
4010 FORMAT(//,F10.1)
4000 FORMAT(2X,2I2,9E12.4)
4050 FORMAT(2E12.4)
4080 FORMAT(6F10.2,2F10.0,3F10.4)
9000 READ(INP,301) NEXT0
      IF(NEXT0.EQ.1) GO TO 9001
      CALL EXIT
      END
```

SUBROUTINE DCAL

C
C

C CALCULATION OF HEAT RELEASE FOR EACH ELEMENT

```

COMMON/EPROP/ IECHF(100),EFUEL(100),EANGL(100),FMWT(100),
1 DHFUEL(100),DHLDS(100),DIEMAS(100),DOEMAS(100),
1 ERGAS(100),ECR(100),FENTH(8,100),FMASS(8,100),FEQUI(8,100),
1 FVOL(8,100),FTEMP(8,100),PCYL(8)
COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,IE
COMMON /STAT1/ RPM,JLAST,NJET,PHIO,EGR
COMMON /FUFLP/ FUEL,FKCAL,ZM,ZN,PSI,SAFC,VACAL
COMMON /JETS/ RJET(50),HJET(50),AJET(50),BJET(50),THER(50),
1 VRJET(50),VZJET(50),WJET(50),VJET(50),AINJ(50),RHJET(50),
2 PITCH(50)
COMMON /PLUME/ PMASS(50),RMASS(50),RPLUM(50),HRMASS(50)
COMMON /JFTDAT/ JSWIR0,ALPHA,BETA,RHGAS
COMMON/COMP/ RPLUM0,ENTUR,RLFSP,ASPARK,TSCALE
DFL=ZN/ZM
IF(IE.EQ.1) GO TO 300
DO 100 I=2,IE
  AJE=AJET(I)*180./3.1416

```

```

C HEAT RELEASE =0 UNLESS SPECIFIED LATER
  DHFUEL(I)=0.

```

C

```

C CHECK WHETHER THE FUEL ELEMENT REACHES THE SPARK PLUG OR NOT.
  IF(AJE.LT.ASPARK) GO TO 100
  IF(PMASS(I).GT.1.E-7) GO TO 400

```

C

```

C SET THE INITIAL PLUME MASS AND GURNED MASS
  RPLUM(I)=RPLUM0
  PMASS(I)=RHJET(I)*4./3.*3.1416*RPLUM0**3

```

C

```

C SCALE FACTOR
  PMASS(I)=PITCH(I)/2.*PMASS(I)
  RMASS(I)=PMASS(I)*2./3.
  IECHF(I)=2
400 DO 410 IP=1,10

```

C

```

C TURBULENT ENTRAINMENT RATE
  U2=FENTUR*VJET(I)
  DPMASS= SQRT(RHJET(I)*RHJET(I))*4.*3.1416*RPLUM(I)**2*U2
  DPMASS=DPMASS*ASTEP/(6.*RPM)/10.

```

C

```

C SCALE FACTOR
  DPMASS=DPMASS*PITCH(I)/2.

```

C

```

C EFFECT OF FLAME COMING BACK
  IF(IECHF(2).NE.3) GO TO 402
  DPMASS=DPMASS*2.

```

402 CONTINUE

```

  PMASS(I)=PMASS(I)+DPMASS
  IF(PMASS(I).LT.FMASS(2,I)) GO TO 420
  PMASS(I)=FMASS(2,I)
  IECHF(I)=3

```

420 TCHA=TSCALE/RLFSP

```

  DRMASS=(PMASS(I)-BMASS(I))/TCHA*ASTEP/(6.*RPM)/10.

```

C

```

  BMASS(I)=BMASS(I)+DRMASS

```

```

C NEXT EQUATION INCLUDES THE SCALE FACTOR ABOUT CALCULATION PITCH
  RPLUM(I)=(PMASS(I)*3./2/PITCH(I)/(RHJET(I)*4.*3.1416))**0.333

```

```

410 CONTINUE
  CALL UPROP(PCYL(1),FTEMP(1,I),FEQUI(2,I),DEL,PSI,0.,ENTAIR,
  1 DUM,DUM,DUM,DUM,DUM,DUM,DUM,DUM)
  CALL HPROP(PCYL(1),FTEMP(1,I),FEQUI(2,I),DEL,PSI,FNTGAS,
  1 DUM,DUM,DUM,DUM,DUM,DUM,DUM,DUM)
C
C INCLUDING THE FORMATION ENTHALPY
  XX=(ENTAIR-FNTGAS)*1000./FKCAL/FEQUI(2,I)*(SAFC+FEQUI(2,I))
  IF(XX-1.) 430,440,440
440 XX=1.
430 HRMASO=HRMASS(I)
  HRMASS(I)=FUEL(I)*RMASS(I)/EMASS(2,I)*XX
  DHFUEL(I)=(HRMASS(I)-HRMASO)*FKCAL/ASIEP
  TRMASS=TRMASS+HRMASS(I)
  TORMAS=TORMAS+DBMASS
100 CONTINUE
300 DHFUEL(1)=0.
  RETURN
  END

```

```

SUBROUTINE INPUT
COMMON/EPROP/ IECHF(100),EFUEL(100),EANGL(100),EMWT(100),
1 DHFUEL(100),DHLOS(100),DIEMAS(100),DOEMAS(100),
1 ERGAS(100),ECP(100),FENTH(8,100),FEMASS(8,100),EEQUI(A,100),
1 EVOL(A,100),FTEMP(A,100),PCYL(8)
COMMON /STAT1/ RPM,JLAST,NJET,PHIO,FSR
COMMON /TIMIG/ AINT0,AFXTO,AINTC,AFXTC,AFUELS,AFUELE
COMMON /GEOMT/ STROKE,BORE,CONL,VCLFAR,VCUP,RCUP,CYLN
COMMON /HETRS/ NDIVID,TMETAL(10),QHTRC(10),ARE(10)
COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,IF
COMMON /FUELP/ FUEL,FKCAL,ZM,ZN,PST,SAFC,VACAL
COMMON /JETS/ RJET(50),HJET(50),AJET(50),BJET(50),THER(50),
1 VRJET(50),VZJET(50),WJET(50),VJET(50),AINJ(50),RHJET(50),
2 PITCH(50)
COMMON /PLUME/ PMASS(50),BMASS(50),RPLUM(50),HRMASS(50)
COMMON /JETDAT/ WSWIR0,ALPHA,BETA,RHGAS
COMMON /SURGAS/ FSWIR,WSWIR,SDFCAY
COMMON/COMR/ RPLUM0,FNTIR,RLFSP,ASPARK,TSCALE
COMMON /OSQPE/ LPT,JNP,LINCO,LINEST,ITEL,LITEL
REAL*4 MBAR
COMMON /FUEL/ AF(6),FNW,CX,HY,OZ,QFLOWER
COMMON/OXDANT/XI/CMPSTN/X(7),MBAR
COMMON/CONTL/ ASTIN,ASTCL,ASTCR,ASTEX,ASTOV,PRININ,PRINCL,PRINEX,
1 PRINOV
COMMON/INFI O/ NINEF,XINEF(20),YINEF(20),AREIND,PINT,TINT,GINT,
1 EQUINT,ARFINT,XINV
COMMON/EXFLO/NEXF,XEXF(20),YEXF(20),AREEXD,PEXT,TEXT,GEXT,
1 ILEFT,TLFFT,QEXT,QFLOW,ELEFT,AREEXT,XEXV
COMMON /AMRJE/ TAMR,PAMR
COMMON /HETR1/ PRASE,TRASE,VRASE,COHT1,COHT2,COHT,=HR(10)
COMMON /FRIDT/ RSKIRT,FODE,RINGN,FMEP(10)
DIMENSION VINLI(20),XCOEI(20),YCOEI(20),YEXLI(20),XCOFE(20),
1 YCOEE(20)
JNP=5
LPT=6
RFSFRK=0.
DEL=ZN/ZM
WRITE(LPT,3000)
3000 FORMAT(1H1,2X,'**CYCLE SIMULATION FOR DIRECT INJECTION ENGINE**
1 VERSION 1***)
READ(INP,3010)
WRITE(LPT,3010)
3010 FORMAT(80H
1
WRITE(LPT,3020)
3020 FORMAT(1H,/,1H,33X,'TABLE OF INPUT DATA AND INITIAL ENGINE COND
ITIONS',/,5X,120(1H*))
C
C READ AND WRITE THE DATA OF ENGINE GEOMETRY
C
C STROKE=STROKE(CM)
C CONL=CONNECTING ROD(CM)
C VCLFAR=CLEARANCE VOLUME( EXCLUDING CUP VOLUME,CM**3)
C VCUP=CUP VOLUME( CM**3)
C RCUP= CUP RADIUS (CM)
C CYLN= NUMBER OF CYLINDER
C READ(INP,23) STROKE,BORE,CONL,VCLFAR,VCUP,RCUP,CYLN
C
C READ AND WRITE THE DATA OF VALVE AND FUEL INJECTION TIMING
C

```



```

C  AINTO=INTAKE VALVE STARTS TO OPEN(CRANK DEGREE, AROUND -10)
C  AEXTO=EXHAUST VALVE STARTS TO OPEN (AROUND 520)
C  AINTC=INTAKE VALVE STARTS TO CLOSE(AROUND 200)
C  AEXTC=EXHAUST VALVE STARTS TO CLOSE(AROUND 10)
C  AFUELS=FUEL INJECTION STARTS (AROUND 330)
C  AFUELE= FUEL INJECTION ENDS (AROUND 355)
C  READ(INP,23) AINTO,AEXTO,AINTC,AEXTC,AFUELS,AFUELE

C
C  READ AND WRITE FUEL PROPERTIES
C
C  ZM= CHEMICAL FORMULA, NUMBER OF H
C  ZN= CHEMICAL FORMULA, NUMBER OF C
C  SAFC= CHEMICALLY CORRECT AIR-FUEL RATIO
C  FKCAL= LOWER HEATING VALUE OF THE FUEL
C  VACAL=LATENT HEAT VALUE (CAL/G)
C  READ(INP,23) ZM,ZN,SAFC,FKCAL,VACAL
C  CX=ZN
C  HY=ZM
C  QLOWER=FKCAL/1000.
C  AF(1)=-0.553
C  AF(2)=182.
C  AF(3)=-97.8
C  AF(4)=20.4
C  AF(5)=-0.0309
C  AF(6)=-60.5
C  XI=3.76
C  ENW=0.
C  OZ=0.

C
C  READ AND WRITE THE DATA OF THE ENGINE OPERATING CONDITION
C
C  FUEL=TOTAL FUEL AMOUNT/ 1 SHOT (GRAM)
C  RPM=ENGINE SPEED (RPM)
C  EGR=EXHAUST GAS RECIRCULATION
C  READ(INP,23) FUEL,RPM,EGR

C
C  HOW MANY REGIONS WILL YOU TAKE FOR HEAT TRANSFER AREA?(NDIVID=6)
C  NDIVID=6

C
C  ELEMENT 1 IS FOR TOTAL
C  NDIVID=NDIVID+1

C
C  READ AND WRITE THE DATA OF THE TEMPERATURE INSIDE ENGINE
C
C  TR= TEMPERATURE OF PISTON TOP
C  TINT= TEMPERATURE OF INTAKE VALVE
C  TEXV= TEMPERATURE OF EXHAUST VALVE
C  TW= TEMPERATURE OF CYLINDER WALL
C  TCYLH= TEMPERATURE OF CYLINDER HEAD
C  READ(INP,23) TP,TINV,TEXV,TW,TCYLH
C  TMETAL(2)=TW
C  TMETAL(3)=TP
C  TMETAL(4)=TP
C  TMETAL(5)=TCYLH
C  TMETAL(6)=TINV
C  TMETAL(7)=TEXV

C
C  CALCULATIONS FOR THE DISTANCES FROM THE CENTER POINT
C  THESE DATA WILL BE USED TO CALCULATE THE VELOCITIES AT THE WALL
C  RWR(2)=RORF/2.
C  RWR(3)=(RORF/2.+RCUP)/2.

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      PHR(4)=RCUP
      PHR(5)=RORF/(2.*1.414)
      PHR(6)=RORF/4.
      PHR(7)=RORF/4.

C
C  HEAT TRASFER COEFFICIENTS
C
C  COHT1,COHT2= HEAT TRANSFER COEFFICIENT
C  COHT1=2.28
C  COHT2=0.0032
C  COHT=ADJUSTING TOTAL HEAT TRANSFER AMOUNT(MAYBE 1)
C  READ(INP,23) COHT1,COHT2,COHT

C
C  READ AND WRITE THE DATA OF INITIAL JET CONDITIONS
C
C  AINJV=JET DIRECTION ANGLE FROM VERTICAL LINE (DEGREE)
C  AINJT=JET DIRECTION ANGLE FROM TANGENTIAL LINE (DEGREE)
C  RINIT= JET RADIAL LOCATION WHEN FUEL IS INJECTED (CM)
C  RINIT= JET INITIAL RADIUS (CM)
C  READ(INP,23) AINJV,AINJT,RINIT,RINIT
C  AINJV= AINJV*3.1416/180.
C  AINJT= AINJT*3.1416/180.

C
C  READ AND WRITE DATA OF AIR ENTRAINMENT PARAMETER
C
C  WSRAT0= SWIRL RATIO AT RDC (*RPM)
C  ALPHA= ENTRAINMENT PARAMETER FOR PARALLEL VELOCITY DIFFERENCE
C  (0.11 IS RECOMMENDED)
C  BETA= ENTRAINMENT PARAMETER FOR NORMAL VELOCITY DIFFERENCE
C  (BETA=0.6 IS RECOMMENDED)
C  RHFUEL= DENSITY OF FUEL (GRAM/CM**3)
C  RHGAS= DENSITY OF SURROUNDING GAS (GRAM/CM**3)
C  SDECAY = SWIRL DECAYING FACTOR (6.5E-6 IS RECOMMENDED FOR
C  TCCS ENGINE)
C  READ(INP,23) WSRAT0,ALPHA,BETA,RHFUEL,RHGAS,SDECAY
C  WSWIR0=3.1416/180.*RPM*6.*WSRAT0

C
C  READ DATA OF COMBUSTION PARAMETER
C
C  RPLUM0= INITIAL PLUME RADIUS(CM)
C  ENTUR= TURBULENCE ENTRAINMENT PARAMETER
C  RLFSF= LAMINAR FLAME SPEED(CM/SFC)
C  ASPARK=SPARK PLUG LOCATION FROM FUEL INJECTION NOZZLE(DEG)
C  READ(INP,23) RPLUM0,ENTUR,RLFSF,ASPARK

C
C  DATA OF INTAKE AND EXHAUST SYSTEM
C  DINV= DIAMETER OF INTAKE VALVE
C  SINV=MAXIMUM LIFT OF INTAKE VALVE
C  XINV=NUMBER OF INTAKE VALVE
C  DEXV= DIAMETER OF EXHAUST VALVE
C  SEXV= MAXIMUM LIFT OF EXHAUST VALVE
C  XEXV=NUMBER OF EXHAUST VALVE
C  READ(INP,23) DINV,SINV,DEXV,SEXV,XINV,XEXV
C  APEIND=3.1416*DINV*SINV*XINV
C  APFEXD=3.1416*DEXV*SEXV*XEXV
C  ARE(3)=3.1416/4.*(RORF*ROPE-RCUP*RCUP*4.)
C  ARE(4)=VCUP*2./RCUP
C  ARE(6)=3.1416/4.*DINV*DINV
C  ARE(7)=3.1416/4.*DEXV*DEXV

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      ARE(5)=3.1416/4.*BORE*BORE-ARE(6)-ARE(7)
C
C
C DATA OF FRICTIONS
C RSKIRT= EQUIVALENT LENGTH OF PISTON SKIRT( PROJECTED ARE OF SKIRT
C / CYLINDER BORE DIAMETER)
C FCOE= JOURNAL BEARING SIZE COEFFICIENT
C RINGN= TOTAL NUMBER OF PISTON RINGS PER CYLINDER
C PFAD(INP,23) RSKIRT,FCOE,RINGN
C READ DATA OF VALVE LIFT VS. NORMALIZED CRANK ANGLE FOR INTAKE VALVE
  READ(INP,301) NINEF
  READ(INP,301) NINCO
  READ(INP,23) (XINEF(I),I=1,NINEF)
  READ(INP,23) (YINLI(I),I=1,NINEF)
  READ(INP,23) (XCOEI(I),I=1,NINCO)
  READ(INP,23) (YCOEI(I),I=1,NINCO)
  DO 1000 I=1,NINEF
    VLIFR=SINV*YINLI(I)/DINV
    CALL TWODIM(NINCO,XCOEI,YCOEI,VLIFR,COEF)
    YINEF(I)=YINLI(I)*COEF
  1000 CONTINUE
C READ DATA OF VALVE LIFT VS. NORMALIZED CRANK ANGLE FOR EXHAUST VALVE
  READ(INP,301) NEXEF
  READ(INP,301) NEXCO
  READ(INP,23) (XEXEF(I),I=1,NEXEF)
  READ(INP,23) (YEXLI(I),I=1,NEXEF)
  READ(INP,23) (XCOEE(I),I=1,NEXCO)
  READ(INP,23) (YCOEE(I),I=1,NEXCO)
  DO 1010 I=1,NEXEF
    VLIFR=SEXV*YEXLI(I)/DEXV
    CALL TWODIM(NEXCO,XCOEE,YCOEE,VLIFR,COEF)
    YEXEF(I)=YEXLI(I)*COEF
  1010 CONTINUE
C
C HOW MANY ELEMENTS DO YOU WANT TO DIVIDE THE INJECTED FUEL INTO ?
C 10 ELEMENTS ARE RECOMMENDED
  READ(INP,301) NJET
C
C AMBIENT CONDITION
C TAMR= AMBIENT TEMPERATURE
C PAMR= AMBIENT PRESSURE
  READ(INP,23) TAMR,PAMR
C
C INTAKE AND EXHAUST PRESSURE
C PINT=INTAKE PRESSURE (ATA)
C PEHT=EXHAUST PRESSURE (ATA)
  READ(INP,23) PINT,PEHT,TINT
C
C COMPUTING INCREMENT
  READ(INP,23) ASTIN,ASTCL,ASTCR,ASTEX,ASTOV
C
C PRINT CONTROL DATA
  READ(INP,23) PRININ,PRINCL,PRINEX,PRINOV
C
C INITIAL ENGINE CONDITION
  READ(INP,23) PCYL(2),FTEMP(2,1),FEQUI(2,1),TEXT
  ELEFT=FEQUI(2,1)
  TLEFT=ETEMP(2,1)
C
C COMPRESSION RATIO

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DISP=3.1416*BORE*ROPE/4.*STROKE
CR=(VCLEAR+VCUP+DISP)/(VCUP+VCLEAR)
C
C TAYLOR MICRO SCALE
TSCALE=SINV/CR*0.17
VINIT=FUFL/RHFUEL/(3.1416*BINIT**2*(AFUELE-AFUELS))*(6.*RPM)
WRITE(6,5200)
WRITE(6,5210) VINIT
5200 FORMAT(2X,'INITIAL JET SPEED')
5210 FORMAT(10X,'VINIT=',F12.1,'CM/SEC')
C
C SET THE INITIAL CONDITIONS FOR ALL JET ELEMENTS
ASTCB=(AFUELE-AFUELS)/FLOAT(NJET)
ASTEP=ASTCB
NMJET=NJET+1
DO 100 I=2,NMJET
  RJET(I)=BINIT
  THER(I)=0.
  VJET(I)=VINIT
  WJET(I)=VINIT*SIN(AINJV)*COS(AINJT)/RINIT
  VRJET(I)=-VINIT*SIN(AINJV)*SIN(AINJT)
  VZJET(I)=VINIT*COS(AINJV)
  RJET(I)=RINIT
  HJET(I)=0.
  AJET(I)=0.
  RHJET(I)=RHFUEL
  RPLUM(I)=RPLUM0
  PMASS(I)=0.
  BMASS(I)=0.
  HRMASS(I)=0.
  AINJ(I)=AFUELS+FLOAT(I-2)*ASTEP
C NEXT ASSUMPTION( FFQUI=3. ) WAS MADE FOR GETTING APPROPRIATE
C THERMODYNAMIC PROPERTIES
FFQUI(2,I)=3.
ND=AFUELE-((FLOAT(I)-1.)*ASTEP+AFUELS)
IF(ND.LT.0.) GO TO 90
EMASS(2,I)=3.1416*BINIT**2.*VINIT*ASTEP/(6.*RPM)*RHFUEL
EFUEL(I)=EMASS(2,I)
PITCH(I)=ASTEP
GO TO 100
90 EMASS(2,I)=3.1416*BINIT**2.*VINIT*(AFUELE-((FLOAT(I)-2.)*ASTEP+
1 AFUELS))/(6.*RPM)*RHFUEL*ASTEP
EFUEL(I)=EMASS(2,I)
PITCH(I)=AFUELE-((FLOAT(I)-2.)*ASTEP+AFUELS)
GO TO 110
100 CONTINUE
110 CONTINUE
C
C CALCULATION OF INTAKE AIR PROPERTIES
EQUINT=EGR*FLEFT*SAFC/((1.-EGP)*(ELEFT+SAFC)+EGR*SAFC)
WRITE(LPT,7020)
WRITE(LPT,7010) STROKE,AINT0,7M,TP,
1 CONL,AFXTO,ZV,TW,
2 ROPE,AINTC,SAFC,TCYLI,
3 VCLFAP,AEXTC,FKCAL,TINV
WRITE(LPT,7011) VCUP,AFUELS,VACAL,TEXV,
5 AFUELF,RHFUEL
WRITE(LPT,7020)
AINVV=AINJV*180./3.1416
AINTT=AINJT*180./3.1416

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WRITE(LPT,7030) WSRATO,PPLUM0.
1      AINVV,ENTUR.
1      AINTT,ALPHA,RLFSP.
3      RINIT,9FTA,ASPARK.
4      RINIT,RHGAS
WRITE(LPT,7031) RCIP,SDFCAY,TSCALE
WRITE(LPT,7020)
WRITE(LPT,7040) RPM,PINT,ASTOV,PRINOV.
1  FUEL,TINT,ASTIN,PRININ.
2  EGR,EQUINT,ASTCL,PRINCL
WRITE(LPT,7041) ASTCB,PRINCL.
1  PAMB,PEXT,ASTCL,PRINCL.
2  TAMR,TEXT,ASTEX,PRINEX.
3  ELEFT
WRITE(LPT,7020)
WRITE(LPT,7050) DINV,ARE(6),PCYL(2).
1  SINV,ARE(7),COHT,FTEMP(2,1).
2  XINV,ARE(3),COHT1,FFQUI(2,1)
WRITE(LPT,7051) ARE(4),COHT2,TEXT.
4  DEXV,ARE(5).
5  SEXV.
6  XEXV
WRITE(LPT,7020)
WRITE(LPT,7060) RSKIRT.
1  FCOE.
2  RINGN
WRITE(LPT,7020)
WRITE(LPT,7100)
WRITE(LPT,7110)
WRITE(LPT,7000) (XINEF(I),I=1,NINEF)
WRITE(LPT,7120)
WRITE(LPT,7000) (YINEF(I),I=1,NINEF)
WRITE(LPT,7140)
WRITE(LPT,7110)
WRITE(LPT,7000) (XEXEF(I),I=1,NEXEF)
WRITE(LPT,7120)
WRITE(LPT,7000) (YEXEF(I),I=1,NEXEF)
RETURN
23  FORMAT(8F10.0)
6020 FORMAT(5E12.4)
6030 FORMAT(6E12.4)
6040 FORMAT(4E12.4)
6050 FORMAT(2E12.4)
6060 FORMAT(I2)
6070 FORMAT(10E12.4)
301  FORMAT(I2)
7000 FORMAT(10X,10F10.3)
7010 FORMAT(32H      ENGINE GEOMETRY      *,
1      32H      TIMING      *,
2      36H      FUEL PROPERTIES      *,
3      30H      ESTIMATE TEMPERATURES      ,/,
4  2X,12HSTROKE      =,F10.3,8HCM      *,
5  17H  INT.VAL.OPEN  =,F9.1,6HNEG  *,
6  19H  7N(NQ. OF H)  =,F10.1,7H      *,
7  18H  PISTON TOP(TP) =,F10.1,1HK,/,
8  2X,12HCON.ROD      =,F10.2,8HCM      *,
9  17H  EXH.VAL.OPEN  =,F9.1,6HNEG  *,
1  19H  7N(NQ. OF C)   =,F10.1,7H      *,
2  18H  CYL.WALL(TW)   =,F10.1,1HK,/,
3  2X,12HRORE      =,F10.3,8HCM      *,

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4 17H INT.VAL.CLOSE =, F9.1.6HDEG *,
5 19H SAFC(STOTCH.A/F)=, F10.1.7H *,
6 18H CYL.WEAD(TCYLW)=, F10.1.1HK,/,
7 2X.12HCLEAR.VOL. =, F10.2.8HCM**3 *,
8 17H EXH.VAL.CLOSE =, F9.1.6HDEG *,
9 19H LOWER HEATING =, F10.0.7H CAL/G*,
5 18H INT.VALVE(TINV)=, F10.1.1HK)
7011 FORMAT(2X,
2 12HCUP VOL. =, F10.2.8HCM**3 *,
3 17H FUEL INJ.START=,F9.1.6HDEG *,
4 19H VAPOIZING HEAT =, F10.0.7H CAL/G*,
5 18H EXH.VALVE(TEXV)=,F10.1.1HK,/,
6 32X,
7 17H FUEL INJ.END =, F9.1.6HDEG *,
8 19H DENSITY =, F9.3.7HG/C**3 ,1H*)
7020 FORMAT(2X,128H-----
1-----
2---
)
7030 FORMAT(42H INITIAL JET DATA *,
1 44H JET MIXING PARAMETER *,
2 43H PLUME MODEL ,/,
3 2X,20HJET DIRECTION** ,19X,1H*,
4 27H SWIRL RATIO AT PDC =,F10.3.74*QPM *,
5 23H INITIAL PLUME RADIIJS =,F10.4.74 CM *,/,
6 2X,20H ANGLE(VERTICAL) =,F10.2.104 DEG *,
7 27H AIR ENTRAIN. PARAMETER , 16X,1H*,
8 23H ENTRAIN. PARAMETER =, F10.3.9X,1H*,/,
9 2X,20H ANGLE(TANGENTIAL)= ,F10.2.104 DEG *,
1 27H ALPHA =, F10.3.6X,1H*,
1 23H LAM. FLAME SPEED =, F10.2.104 CM/SEC *,/,
2 22H JET RADIUS =,F10.5.104 CM *,
3 27H BETA =, F10.3.6X,1H*,
4 23H SPARK PLUG LOCATION =, F10.2.104 DEG *,/,
5 22H JET LOCATION(R) =, F10.3.104 CM *,
6 27H DENSITY OF SURROUND. GAS =,F10.5.7H G/CC *,
7 8X,19H(FROM INJ. NOZZLE) )
7031 FORMAT(
8 22H PISTON CUP RADIUS =, F10.3.104 CM *,
9 27H SWIRL DECAY FACTOR =, F10.3.6X,1H*,
1 23H TAYLOR MICRO SCALE =, F10.4.104 CM )
7040 FORMAT(2X,31H ENGINE CONDITION *,
1 31H INTAKE CONDITIONS *,
2 31H COMPUTING INTERVALS *,
3 31H PRINT CONTROL ,/,
4 2X,15HENGINE SPEED =, F8.0.84 RPM *,
5 15H PRESSURE =, F8.3.84 ATA *,
6 15H VALVE OVERLAP=, F8.2. 84 DEG *,
6 15H VALVE OVERLAP=, F8.2.8X,/,
8 2X,15HFUEL AMOUNT =, F8.5. 84 G/SHOT*,
9 15H TEMPERATURE =, F8.2.84 K *,
9 15H INTAKE =, F8.2.84 DEG *,
1 15H INTAKE =, F8.2.8X,/,
2 2X,15HFGR =, F8.3.7X,1H*,
3 15H EQUI. RATIO =,F8.3.7X,1H*,
4 15H COMPRESSION =, F8.2.84 DEG *,
5 15H COMPRESSION =, F8.2 )
7041 FORMAT(2X,
6 31H AMBIENT CONDITIONS *,
7 31H EXHAUST CONDITIONS(ASSUME) *,
8 15H COMBUCTION =, F8.2.84 DEG *,

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9 15H COMBUSTION      =, F8.2,8X,/.
9 2X,15H PRESSURE     =, F8.2,8H ATA  *,
9 15H PRESSURE        =, F8.2,8H ATA  *,
2 15H EXPANSION        =, F8.2,8H DEG  *,
3 15H EXPANSION        =, F8.2,8X,/.
42X,15H TEMPERATURE   =, F8.2,8H K    *,
5 15H TEMPERATURE     =, F8.2,8H K    *,
6 15H EXHAUST          =, F8.2,8H DEG  *,
7 15H EXHAUST          =, F8.2,8X,/.
4 32X,1H*,
5 15H EQUI. RATIO     =, F8.3,7X,1H*)
7050 FORMAT(2X,31H      INTAKE VALVE      *,
1 31H      HEAT TRANS. AREA      *,
2 31H      HEAT TRANS. COEFF      *,
3 31H      INITIAL CONDITION      /,
4 2X,15H DIAMETER        =, F9.3,7H CM  *,
5 15H INTAKE VALVE = .F9.3,7H CM**2*,
6 31H      (WOSCHNITZ EQ.) * ,
7 15H CYL. PRESS.        =, F9.2,7H ATA  /,
8 2X,15H LIFT            =, F9.3,7H CM  *,
9 15H EXHAUST VALVE = .F9.3,7H CM**2*,
9 15H COHT              =, F9.5,6X,1H*,
1 15H CYL. TEMP.         =, F9.1,7H DEG  /,
2 2X,15H NUMBER          =, F9.1,6X,1H*,
3 15H PISTON TOP         =, F9.3,7H CM**2*,
4 15H COHT1             =, F9.5,6X,1H*,
5 15H CYL. EQUI.        = .F9.3)
7051 FORMAT(2X,31H      EXHAUST VALVE      *,
1 15H PISTON TOP         = .F9.3,7H CM**2*,
2 15H COHT2             =, F9.5,6X,1H*,
3 15H EXHAUST TEMP. =, F9.1,7H DEG  *, /,
4 2X,15H DIAMETER        = .F9.3,7H CM  *,
5 15H CYL. HEAD          =, F9.3,7H CM**2*, /,
6 2X,15H LIFT            =, F9.3,7H CM  *,
7 15H CYL. WALL          =, 7X,9H VARIABLE* /,
8 2X,15H NUMBER          =, F9.1,6X,1H*)
7060 FORMAT(2X,31H      FRICTION LOSS      *, /,
1 2X,15H PISTON SKIRT    = .F9.3,7H CM  *, /,
2 2X,15H JOU. BEAR. COE = .F9.3,6X,1H*, /,
3 2X,15H NO. OF RINGS    =, F9.1,6X,1H*)
7100 FORMAT(1H1,/,2X,
1 'INTAKE VALVE--EFFECTIVE FLOW AREA VS. CRANK ANGLE')
7110 FORMAT(5X,'NORMALIZED CRANK ANGLE')
7120 FORMAT(5X,'NORMALIZED EFFECTIVE FLOW AREA')
7140 FORMAT(//,2X,
1 'EXHAUST VALVE--EFFECTIVE FLOW AREA VS. CRANK ANGLE')
END

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SUBROUTINE RUNGE (ENTINT)

THIS PROGRAM WAS MADE FOR OPERATING RUNGE-KUTTA METHOD

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COMMON/PROP/ IFCHF(100),EFUEL(100),EANG(100),FMWT(100),
1 OFUEL(100),OHLOS(100),DIEMAS(100),DOEMAS(100),
1 FBGAS(100),ECP(100),FENTH(8,100),FMASS(8,100),EEQUI(8,100),
1 EVOL(4,100),FTEMP(8,100),PCYL(8)
COMMON /TIMIS/ AINT0,AFXT0,AINTC,AFXTC,AFUELS,AFUELE
COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,IE
COMMON /STAT1/ RPM,ILAST,NJET,PHIO,FSR
COMMON /GEOM1/ STROKE,BORE,CONL,VCLFAR,VCUP,RCUP,CYLN
COMMON /HETRS/ NOIVID,TMETAL(10),QHTRC(10),ARE(10)
COMMON /HETRI/ PRASE,THASE,VRASE,COHT1,COHT2,COHT,RHR(10)
COMMON /SUM1/ STGINT,STGEXT,STOEXT
COMMON /SUM2/ TTGINT,TTGEXT,TTOEXT,TTQHT(10),TQHT(10),PC
COMMON /FUEL1/ FUEL,FKCAL,ZM,ZN,PST,SAFC,VACAL
9FAL*4 M3A3
COMMON /FUEL/ AF(6),ENW,CX,HY,O7,OLOWER
COMMON/OXDANT/XT/CMPSTN/X(7),MRAR
COMMON /JETS/ PJET(50),HJET(50),AJFT(50),BJFT(50),THER(50),
1 VPJET(50),VZJET(50),WJET(50),VJET(50),AINJ(50),RHJET(50),
2 PITCH(50)
COMMON /PLJME/ PMASS(50),BMASS(50),RPLUM(50),HRMASS(50)
COMMON /JETDAT/ WSWIR0,A_PHA,RFTA,PHGAS
COMMON /SUPGAS/ FSWIR,WSWIR,SDFCAY
COMMON/COMP/ RPLUM0,ENTUR,RLFSP,ASPAK,TSCALE
COMMON/INFL0/ NINEF,XINEF(20),YINEF(20),AREIND,PINT,TINT,GINT,
1 EQINT,AREINT,XINV
COMMON/FAFLO/NEXEF,XEXEF(20),YEXEF(20),AREEXO,PEXT,TEXT,GFXT,
1 IGLEFT,TLFFT,DEXT,OFLOW,ELEFT,AREEXT,XEXV
COMMON /NOYSP/ CONNO(100),PPMNO(100),WNO(100),SUMNO(100),PPMEXT
DIMENSION SUMHT(30)
DEL=ZN/ZM
STGINT=0.
STGEXT=0.
STOEXT=0.
GINT=0.
GFXT=0.
DEXT=0.
RESFR=0.0
NSTEP=1
IFE=IE+1
DO 31 I=1,IFE
SUMHT(I)=0.
21 CONTINUE
DO 24 I=1,NOIVID
22 TQHT(I)=0.
ANGLE=ANGLE1
30 IO(20,20,22,22,22),JCOND
22 CALL VGAS(0.001,0.001,RPM,ANGLE1,DUM,UJM,WSWIR,DUM,FSWIR)
FSWIR=FSWIR-SDFCAY*WSWIR*WSWIR*ASTEP/(6.*RPM)
GO TO 21
20 FSWIR=1.0
FSWIR=WSWIR0
21 CONTINUE
IF(JCOND,EN,4) GO TO 30
30 IO 40

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C  CALCULATION OF JET MODEL IN ORDER TO GET THE ENTRAINMENT AIR
3) DOFMAS(1)=0.
C  CHECK WHETHER NEW FUEL ELEMENT IS INJECTED OR NOT
  NJET=NJET+1
  IF (IE=NJET) 1010,1020,1020
1010 AXX=AFUELE+10.
  IF (ANGLE.GT.AXX) GO TO 40
  IE=IE+1
  FTEMP(2,IE)=FTEMP(2,1)
  CALL UPRUP(PCYL(2),FTEMP(2,IE),FEQUI(2,IE),DEL,PSI,
  1 RESPRK,EENTH(2,IE),CSURP,CSURT,RHO,DRHODT,DRHONP,CHI,
  2 ERGAS(IE),CVRG)
  EENTH(2,IE)=EENTH(2,IE)*1000.
  EMWT(IE)=MRAR
  ECP(IE)=ERGAS(IE)/41.443+CVRG
  EVOL(2,IE)=EMASS(2,IE)*ERGAS(IE)*FTEMP(2,IE)/PCYL(2)
1020 CONTINUE
  DO 32 I=2,IE
    FEQUI0=FEQUI(2,I)
    EMASS0=EMASS(2,I)
    IF (EMASS(2,I).LT.0.040) GO TO 35
    IF (EMASS(2,I).GT.DOFMAS(1)) GO TO 37
C
C  ALL AIR HAS BEEN ENTRAINED BY JET
35 ALPHA=0.
  BETA=0.
37 CONTINUE
  IF (HJET(1).LT.0.2) GO TO 220
  IF (RJET(1).LT.1.0) GO TO 222
  JSTEP=4
  GO TO 230
222 JSTEP=8
  GO TO 230
220 JSTEP=50
230 CALL JET(RJET(1),HJET(1),AJET(1),RJET(1),THER(1),VRJET(1),
  1 VZJET(1),WJET(1),TOM,EMASS(2,1),ASTEP,JSTEP,RPM,ANGLE,PITCH(1),
  1 FSWIP,WSWIP)
  VJET(1)=SQRT(VRJET(1)**2+VZJET(1)**2+(RJET(1)*WJET(1))**2)
  VOL=(3.1416*RJET(1)**2*(1.-THER(1)/(2.*3.1416))+3.1416*AJET(1)**2
  1 *SIN(THER(1)/2.)*VJET(1)*PITCH(1)/(6.*RPM)
  RHJET(1)=EMASS(2,1)/VOL
  FEQUI(2,1)=FEFUEL(1)*(SAFC+EEQUI(2,1))/(EMASS(2,1)-EFUEL(1))
  1 +FEQUI(2,1)
  FEQUI(3,1)=(FEQUI(2,1)-FEQUI0)/ASTEP
  DIEMAS(1)=TOM/ASTEP
  SUMDI(1)=TOM
  DOFMAS(1)=0.
  DOFMAS(1)=DOFMAS(1)+DIEMAS(1)
  EMASS(2,1)=EMASS0
  FEQUI(2,1)=FEQUI0
32 CONTINUE
  SUMDI(1)=-DOFMAS(1)*ASTEP
  DIEMAS(1)=0.
  FEQUI(3,1)=0.
40 CONTINUE
  PCYL(1)=PCYL(2)
  DO 100 I=1,IE
    EMASS(1,I)=EMASS(2,I)
    FEQUI(1,I)=FEQUI(2,I)
    EVOL(1,I)=EVOL(2,I)

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      ETEMP(1,I)=ETEMP(2,I)
      FENTH(1,I)=FENTH(2,I)
100  CONTINUE
      ANGLE=ANGLE+1
      CALL CALCUL(DV CYL,ENTINT)
      CALL DELTA(DV CYL,ENTINT)
      STGINT=STGINT+GINT/6.
      STGEXT=STGEXT+GEXT/6.
      STOEXT=STOEXT+OEXT/6.
      DO 120 I=1,NDIM
120  TQHT(I)=TQHT(I)+QHTRC(I)/6.

C
C   SECOND STEP
C
      NSTEP=NSTEP+1
      PCYL(4)=PCYL(3)*ASTEP
      PCYL(1)=PCYL(2)+PCYL(4)/2.
      DO 200 I=1,IE
      FMASS(4,I)=FMASS(3,I)*ASTEP
      FEQUI(4,I)=FEQUI(3,I)*ASTEP
      EVOL(4,I)=EVOL(3,I)*ASTEP
      ETEMP(4,I)=ETEMP(3,I)*ASTEP
      FENTH(4,I)=FENTH(3,I)*ASTEP
      FMASS(1,I)=FMASS(2,I)+FMASS(4,I)/2.
      FEQUI(1,I)=FEQUI(2,I)+FEQUI(4,I)/2.
      EVOL(1,I)=EVOL(2,I)+EVOL(4,I)/2.
      ETEMP(1,I)=ETEMP(2,I)+ETEMP(4,I)/2.
      FENTH(1,I)=FENTH(2,I)+FENTH(4,I)/2.
      IF(IECHE(I),EO,I) GO TO 210
      CALL HPROP(PCYL(1),ETEMP(1,I),FEQUI(1,I),DEL,PSI,FENTHLP,
1  CSUBP,CSURT,RHO,DPHNT,DRHDP,FMWT(1),ERGAS(I),CVBG,FRG)
      GO TO 212
210 CALL UPROP(PCYL(1),ETEMP(1,I),FEQUI(1,I),DEL,PSI,RESFRK,ENTHLP,
1  CSUBP,CSURT,RHO,DPHNT,DRHDP,CHI,FRGAS(I),CVBG)
      FMWT(I)=WRAP
212  CONTINUE
      FRG(I)=ERGAS(I)/41.443+CVBG
      SUPHT(I)=SIMHT(I)-DHLOS(I)/5.
220  CONTINUE
      ANGLE=ANGLE+1+ASTEP/2.
      CALL CALCUL(DV CYL,ENTINT)
      CALL DELTA(DV CYL,ENTINT)
      STGINT=STGINT+GINT/3.
      STGEXT=STGEXT+GEXT/3.
      STOEXT=STOEXT+OEXT/3.
      DO 225 I=1,NDIM
225  TQHT(I)=TQHT(I)+QHTRC(I)/3.

C
C   THIRD STEP
C
      PCYL(5)=PCYL(3)*ASTEP
      PCYL(1)=PCYL(2)+PCYL(5)/2.
      DO 300 I=1,IE
      FMASS(5,I)=FMASS(3,I)*ASTEP
      FEQUI(5,I)=FEQUI(3,I)*ASTEP
      EVOL(5,I)=EVOL(3,I)*ASTEP
      ETEMP(5,I)=ETEMP(3,I)*ASTEP
      FENTH(5,I)=FENTH(3,I)*ASTEP
      FMASS(1,I)=FMASS(2,I)+FMASS(5,I)/2.
      FEQUI(1,I)=FEQUI(2,I)+FEQUI(5,I)/2.

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      EVOL(1,I)=EVOL(2,I)+EVOL(5,I)/2.
      FTEMP(1,I)=FTEMP(2,I)+FTEMP(5,I)/2.
      FEENTH(1,I)=FEENTH(2,I)+FEENTH(5,I)/2.
      IF(IECHE(I).EQ.1) GO TO 310
      CALL HPROP(PCYL(1),FTEMP(1,I),FEQHI(1,I),DEL,PSI,FNTHLP,
1 CSUBP,CSURT,RHO,DRHONT,DRHODP,EMWT(I),ERGAS(I),CVBG,FRGR)
      GO TO 312
310 CALL HPROP(PCYL(1),FTEMP(1,I),FEQHI(1,I),DEL,PSI,RESFRK,ENTHLP,
1 CSUBP,CSURT,RHO,DRHONT,DRHODP,CHI,ERGAS(I),CVBG)
      EMWT(I)=MRAP
312 CONTINUE
      ECP(1)=ERGAS(I)/41.443+CVBG
      SUMHT(I)=SUMHT(I)-OHLOS(I)/3.
300 CONTINUE
      ANGLE=ANGLE1+ASTEP/2.
      CALL CALCQ(DVCYL,ENTINT)
      CALL DELTA(DVCYL,ENTINT)
      STGINT=STGINT+GINT/3.
      STGEXT=STGEXT+GEXT/3.
      STOFXT=STOFXT+OFXT/3.
      DO 320 I=1,NDIMD
320 TOTHT(I)=TOTHT(I)+OHTRC(I)/3.
C
C   FOURTH STEP
C
      PCYL(6)=PCYL(3)*ASTEP
      PCYL(1)=PCYL(2)+PCYL(6)
      DO 400 I=1,IE
      FMASS(6,I)=FMASS(3,I)*ASTEP
      FEQHI(6,I)=FEQHI(3,I)*ASTEP
      EVOL(6,I)=EVOL(3,I)*ASTEP
      FTEMP(6,I)=FTEMP(3,I)*ASTEP
      FEENTH(6,I)=FEENTH(3,I)*ASTEP
      FMASS(1,I)=FMASS(2,I)+FMASS(6,I)
      FEQHI(1,I)=FEQHI(2,I)+FEQHI(6,I)
      EVOL(1,I)=EVOL(2,I)+EVOL(6,I)
      FTEMP(1,I)=FTEMP(2,I)+FTEMP(6,I)
      FEENTH(1,I)=FEENTH(2,I)+FEENTH(6,I)
      IF(IECHE(I).EQ.1) GO TO 410
      CALL HPROP(PCYL(1),FTEMP(1,I),FEQHI(1,I),DEL,PSI,FNTHLP,
1 CSUBP,CSURT,RHO,DRHONT,DRHODP,EMWT(I),ERGAS(I),CVBG,FRGR)
      GO TO 412
410 CALL HPROP(PCYL(1),FTEMP(1,I),FEQHI(1,I),DEL,PSI,RESFRK,ENTHLP,
1 CSUBP,CSURT,RHO,DRHONT,DRHODP,CHI,ERGAS(I),CVBG)
      EMWT(I)=MRAP
412 CONTINUE
      ECP(1)=ERGAS(I)/41.443+CVBG
      SUMHT(I)=SUMHT(I)-OHLOS(I)/3.
400 CONTINUE
      ANGLE=ANGLE1+ASTEP
      CALL CALCQ(DVCYL,ENTINT)
      CALL DELTA(DVCYL,ENTINT)
      STGINT=STGINT+GINT/6.
      STGEXT=STGEXT+GEXT/6.
      STOFXT=STOFXT+OFXT/6.
      DO 420 I=1,NDIMD
420 TOTHT(I)=TOTHT(I)+OHTRC(I)/6.

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FIFTH STEP

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PCYL(1)=PCYL(3)*ASTEP
PCYL(2)=PCYL(2)+(PCYL(4)+2.*PCYL(5)+2.*PCYL(6)+PCYL(7))/6.
DO 500 I=1,IE
  FMASS(7,I)=FMASS(3,I)*ASTEP
  FEQUI(7,I)=FEQUI(3,I)*ASTEP
  FVOL(7,I)=FVOL(3,I)*ASTEP
  FTEMP(7,I)=FTEMP(3,I)*ASTEP
  FENTH(7,I)=FENTH(3,I)*ASTEP
  EMASS(2,I)=FMASS(2,I)+(FMASS(4,I)+2.*EMASS(5,I)+2.*EMASS(6,I)
1 +EMASS(7,I))/6.
  FEQUI(2,I)=FEQUI(2,I)+(FEQUI(4,I)+2.*FEQUI(5,I)+2.*FEQUI(6,I)
1 +FEQUI(7,I))/6.
  FVOL(2,I)=FVOL(2,I)+(FVOL(4,I)+2.*FVOL(5,I)+2.*FVOL(6,I)
1 +FVOL(7,I))/6.
  FTEMP(2,I)=FTEMP(2,I)+(FTEMP(4,I)+2.*FTEMP(5,I)+2.*FTEMP(6,I)
1 +FTEMP(7,I))/6.
  FENTH(2,I)=FENTH(2,I)+(FENTH(4,I)+2.*FENTH(5,I)+2.*FENTH(6,I)
1 +FENTH(7,I))/6.
  IF(IECHE(I).EQ.1) GO TO 510
  CALL HPROP(PCYL(1),FTEMP(1,I),FEQUI(1,I),DEL,PSI,ENTHLP,
1 CSUBP,CSURT,RHO,DRHODT,DRHODP,EMWT(I),ERGAS(I),CVBG,EBGR)
  GO TO 512
510 CALL UPROP(PCYL(1),FTEMP(1,I),FEQUI(1,I),DEL,PSI,RESFRK,ENTHLP,
1 CSUBP,CSURT,RHO,DRHODT,DRHODP,CHI,ERGAS(I),CVBG)
  EMWT(I)=MBAR
512 CONTINUE
  ECP(I)=ERGAS(I)/41.447+CVBG
  DHLOS(I)=(SUMHT(I)-DHLOS(1))/6.)*ASTEP
500 CONTINUE
C INJECTED FUEL HAS SAME TEMP AND ENTHALPY AS AIR. ( THIS ASSUMPTION IS
C NECESSARY FOR THE ACCURATE CALCULATION. BECAUSE THE MASS JUST AFTER
C INJECTED IS SO SMALL THAT IT WILL CAUSE A LARGE AMOUNT OF ERROR.)
  IF(ANGLE.GT.AFUELE) GO TO 530
  IF(IE.EQ.1) GO TO 530
  FTEMP(2,IE)=FTEMP(2,1)
  FENTH(2,IE)=FENTH(2,1)
530 CONTINUE
  RETURN
  END

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      SUBROUTINE CALCUL(DVCYL,FNTINT)
C
C THIS SUBROUTINE IS TO SET THE DATA FOR SUBROUTINE RUNGE
      COMMON/EPROP/ IECH(100),EFUEL(100),EANG(100),EMWT(100),
1 DHFUEL(100),DHLOS(100),DIEMAS(100),DOEMAS(100),
1 ERGAS(100),ECP(100),FENTH(8,100),EMASS(8,100),EEQUI(8,100),
1 EVOL(8,100),ETEMP(8,100),PCYL(8)
      COMMON /TIMIG/ AINT0,AEXT0,AINTC,AEXTC,AFUELS,AFUELE
      COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,IE
      COMMON /GEOMT/ STROKE,BORE,CONL,VCLEAR,VCUP,RCUP,CYLN
      COMMON /HETRS/ NDIVID,TMETAL(10),QHTRC(10),ARF(10)
      COMMON /HETRI/ PRASE,TBASE,VBASE,COHT1,COHT2,COHT,RHR(10)
      COMMON /SUM2/ TTGINT,TTGEXT,TTQEXT,TTQHTR(10),TOHTR(10),PS
      COMMON /STAT1/ RPM,JLAST,NJET,PHIO,EGR
      COMMON /FUELP/ FUEL,FKCAL,ZM,ZN,PSI,SAFC,VACAL
      COMMON /JETS/ RJET(50),HJET(50),AJET(50),BJET(50),THER(50),
1 VRJET(50),VZJET(50),WJET(50),VJET(50),AINJ(50),RHJET(50),
2 PITCH(50)
      COMMON /PLUME/ PMASS(50),BMASS(50),RPLUM(50),HRMASS(50)
      COMMON /JETDAT/ WSWIR0,ALPHA,BETA,RHGAS
      COMMON/INFLO/ NINEF,XINEF(20),YINEF(20),AREIND,PINT,TINT,GINT,
1 EQUINT,ARFINT,XINV
      COMMON/EXFLO/NFEXF,XEXEF(20),YEXEF(20),AREEXD,PEXT,TEXT,GEXT,
1 IGLEFT,TLEFT,QEXT,QFLOW,ELEFT,AREEXT,XEXV
      COMMON/COMR/ RPLUM0,ENTUR,RLFSP,ASPAK,TSCALE
C
C CYLINDER VOLUME
      CALL VOLCY(ANGLE,VCYL,DVCYL,STROKE,BORE,CONL,VCLEAR,VCUP)
C
C HEAT TRANSFER
      CALL HEATR
C
C NO HEAT RELEASE FOR ELEMENT 1(AIR)
      DHFUEL(1)=0.
      GO TO (100,200,300,400,600),JCOND
C
C WHEN THE INTAKE AND EXHAUST VALVE OPEN
C INTAKE PORT CALCULATION
100 CALL INPOR
      DIEMAS(1)=GINT
      IF(GINT) 700,710,710
C
C INTAKE FLOW IS FROM PORT TO CYLINDER
710 EEQ0=EEQUI(1,1)
      EEQN=(EMASS(1,1)*EFQUI(1,1)*(EQUINT+SAFC)+GINT*EQUINT*
1 (EEQUI(1,1)+SAFC))/(EMASS(1,1)*(EQUINT+SAFC)+GINT*(EFQUI(1,1)
2 +SAFC))
      EEQUI(3,1)=EEQN-EEQ0
      QFLOW=GINT*ENTINT
      GO TO 720
C
C INTAKE FLOW IS FROM CYLINDER TO PORT (BACK FLOW)
700 EFQUI(3,1)=0.
      QFLOW=GINT*ENT(ETEMP(1,1),EEQUI(1,1),PCYL(1))
C
C EXHAUST PORT CALCULATION
720 CALL EXPOR
      DOEMAS(1)=-GEXT
      EMASS(3,1)=GINT+GEXT
      QFLOW=QFLOW+GEXT*FENTH(1,1)

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      GO TO 2000
C
C   WHEN THE INTAKE PROCESS CALCULATION
C   INTAKE PORT CALCULATION
200 CALL INPOR
    DIEMAS(1)=GINT
    IF(GINT) 800,810,810
C
C   INTAKE FLOW IS FROM PORT TO CYLINDER
810 EEQO=EEQUI(1,1)
    EEON=(EMASS(1,1)*EEOUT(1,1)*(EQUINT+SAFC)+GINT*EQUINT*
      1 (EEQUI(1,1)+SAFC))/(FMASS(1,1)*(EQUINT+SAFC)+GINT*(EEQUI(1,1)
      2 +SAFC))
    EEQUI(3,1)=EEON-EEQO
    QFLOW=GINT*FNTINT
    GO TO 820
C
C   INTAKE FLOW IS FROM CYLINDER TO PORT (BACK FLOW)
800 EFQUI(3,1)=0.
    QFLOW=GINT*EENTH(1,1)
820 GEXT=0.
    QEXT=0.
    EMASS(3,1)=GINT
    GO TO 2000
C
C   COMPRESSION AND EXPANSION
300 EFQUI(3,1)=0.
    EMASS(3,1)=0.
    QFLOW=0.
    GINT=0.
    GEXT=0.
    QEXT=0.
    GO TO 2000
C
C   COMBUSTION AND EXPANSION PROCESS
400 CONTINUE
    IF(IE.EQ.1) GO TO 300
    IF(NSTEP.GE.2) GO TO 410
    CALL DCAL
C
C   THE EFFECT OF PUSHING THE FUEL ELEMENT INTO CYLINDER
    IF(ANGLE.GF.AFUELE) GO TO 410
    DDV=EVOL(1,IE)/ASTEP
410 CONTINUE
    QFLOW=-DOEMAS(1)*EENTH(1,1)
    GINT=0.
    GEXT=0.
    QEXT=0.
    IF(ANGLE.GF.AFUELE) GO TO 420
    DVCYL=DVCYL-DDV
420 CONTINUE
    GO TO 2000
C
C   EXHAUST VALVE OPEN
600 EFQUI(3,1)=0.
    CALL EXPOR
    DOEMAS(1)=-GEXT
    EMASS(3,1)=GEXT
    QFLOW=GEXT*FENTH(1,1)
2000 RETURN
    END

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SUBROUTINE FRIC

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C
C CALCULATION OF THE FRICTION LOSSES
C THIS PROGRAM WAS ORIGINALLY MADE BASED ON IN.-LB UNITS.
COMMON /STAT1/ RPM, JLAST, NJET, PHIO, FGR
COMMON /GEOMT/ STROKE, BORE, CONL, VCLEAR, VCUP, RCUP, CYLN
COMMON /INFLO/ NINEF, XINEF(20), YINEF(20), AREIND, PINT, TINT, GINT,
1 FQUINT, ARFINT, XINV
COMMON /AMRTE/ TAMR, PAMR
COMMON /FRIDT/ RSKIRT, FCDE, RINGN, FMED(10)
FAC1=2.54
FAC2=1000./14.2
BOREX=BORE/FAC1
STROX=STROKE/FAC1
RSKIX=RSKIRT/FAC1
CR=(3.1416*BORE*BORE*STROKE/4.+(VCUP+VCLEAR)/(VCUP+VCLEAR))

C
C MISCELLANEOUS AND PUMPS
FMEP(2)=FAC2*0.39*(RPM/1000.)**1.5

C
C CAM GEAR
DINTV=SQRT(AREIND*4./(3.1416*XINV))/FAC1
FMEP(3)=FAC2*(30.-(4.*RPM/1000.))*XINV*DINTV**1.75/(BOREX*BOREX
1 *STROX)

C
C BEARING
FMEP(4)=FAC2*(FCDE*BOREX/STROX)*RPM/1000.

C
C BLOWBY
XX=ABS(PAMR-PINT)
IF (XX.LT.0.) XX=0.
FMEP(5)=FAC2*SQRT(XX)*(1.72*CR**0.4-(0.49+0.015*CR)*(RPM/1000.))**
1 1.185)

C
C VISCOUS PISTON
FMEP(6)=FAC2*(21.93*RSKIX/(BOREX*STROX)*STROX*RPM/5000.)

C
C STATIC RING TENSION
FMEP(7)=FAC2*2.11*STROX*RINGN/(BOREX*BOREX)

C
C RING GAS PRESSURE
FMEP(8)=FAC2*XX*(2.35*STROX/(BOREX*BOREX))*(0.088*CR+0.182*CR**
1 (1.33-(0.121*STROX*RPM/5000.)))

C
C TOTAL FRICTION LOSS
FMEP(1)=0.
DO 100 I=2,8
FMEP(1)=FMEP(1)+FMEP(I)
100 CONTINUE
RETURN
END

```

SUBROUTINE VGAS(RJET,HJET, RPM, ANGLE,VRGAS,VZGAS,WSWIR,VPIS,
1 FSWIR)

```

C
C
C CALCULATION OF THE GAS VELOCITY SURROUNDING THE JET
COMMON /GEOMT/ STROKE,BORE,CONL,VCLEAR,VCUP,RCUP,CYLN
COMMON /JETDAT/ WSWIR0,ALPHA,BETA
C RJET=JET RADIUS FROM CENTER(CM) (GIVEN)
C HJET=JET VERTICAL LOCATION FROM CYLINDER HEAD (GIVEN)
C RPM= ENGINE SPEED (GIVEN)
C ANGLE= CRANK ANGLE (DEG),TDC=360 (GIVEN)
C VRGAS=VELOCITY COMP. OF RADIAL DIRECTION (GIVEN)
C VZGAS=VELOCITY COMP. OF VERTICAL DIRECTION (GIVEN)
C WSWIR=ANGULAR VELOCITY(RAD/SEC) (GIVEN)
C VPIS= PISTON SPEED(CM/SEC) (GIVEN)
C FSWIR=CONSERVATION RATIO OF SWIRL (GIVEN)
C STROKE ,BORE,CONL,VCLEAR,VCUP,RCUP,WSWIR0 ARE GIVEN IN COMMON
C (SEE THE INPUT ROUTINE TO CHECK THE MEANINGS OF THESE VALUES)
C NO SUBROUTINES ARE REQUIRED
  RCYL=BORE/2.
  AK1=VCUP/(3.1416*RCYL*RCYL)
  AK2=VCUP/(3.1416*RCUP*RCUP)
  ANG=ANGLE*3.1416/180.
  ANG0=3.1416
C
C PISTON HIGHT FROM THE PISTON TO THE CYLINDER HEAD
  HIGH=SQRT(1.-(STROKE/2.*SIN(ANG)/CONL)**2 )
  HIGH=VCLEAR/(3.1416*BORE*BORE/4.)+STROKE/2.*(1.-COS(ANG))
  1 *CONL*(1.-HIGH)
C
C PISTON HIGHT AT BDC
  HIGH0=SQRT(1.-(STROKE/2.*SIN(ANG0)/CONL)**2 )
  HIGH0=VCLEAR/(3.1416*BORE*BORE/4.)+STROKE/2.*(1.-COS(ANG0))
  1 *CONL*(1.-HIGH0)
C
C PISTON SPEED
  VPIS=SQRT(CONL*CONL-STROKE*STROKE/4.*SIN(ANG)*SIN(ANG))
  VPIS=STROKE/2*SIN(ANG)+STROKE*STROKE/4.*SIN(ANG)*COS(ANG)/VPIS
  VPIS=VPIS*3.1416/180.*RPM*6.
  XX=HIGH/AK1
  IF(RJET.LT.RCUP) GO TO 100
  IF(HJET.LT.HIGH) GO TO 200
  VZGAS=0.
  VRGAS=0.
  GO TO 400
C
C GAS VELOCITY COMPONENTS ABOVE THE PISTON( FLAT PART)
200 VRGAS=RJET/(2.*AK1)*(RCYL*RCYL/(RJET*RJET)-1.)*VPIS/(XX*(1.+XX))
  VZGAS=HJET/HIGH*VPIS
  GO TO 400
100 IF(HJET.LT.HIGH) GO TO 300
C
C GAS VELOCITY COMPONENTS INSIDE THE CUP
  VRGAS=0.
  VZGAS=(AK1-AK2+HJET)/(AK1+HIGH)*VPIS
  GO TO 400
C

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C  GAS VELOCITY COMPONENTS ABOVE PISTON CJP
300 VRGAS=RJET/(2.*AK1)*(1.-AK2/AK1)/(XX*(XX+AK2/AK1))
    VRGAS=-VRGAS*VPIS
    VZGAS=(1.-RCYL*RCYL/(PCUP*RCUP*(XX+1.)))*HJET/HIGH*VPIS

C
C  GAS VELOCITY (TANGENTIAL COMPONENT)
400 WSWIR=(HIGH+AK1)/(HIGH0+AK1)*WSWIR0*(AK2*RCUP**4.
    1 +HIGH0*RCYL**4.)/(AK2*RCUP**4.+HIGH*RCYL**4.)
    WSWIR=WSWIR*FSWIR
    RETURN
    END
    SUBROUTINE CONT(XX,YY,X1,Y0,X,Y,N)
    DIMENSION Y(2),Y(2)
    IF(N-2) 10,20,30
10  X(1)=XX
    Y(1)=YY
    XX=XX+X1
    N=2
    RETURN
20  X(2)=XX
    Y(2)=YY
    N=3
    GO TO 60
30  IF((Y(2)-Y0)*(YY-Y0)) 40,50,50
40  X(1)=XX
    Y(1)=YY
    GO TO 60
50  X(2)=XX
    Y(2)=YY
60  XX=(Y0-Y(1))*(X(2)-X(1))/(Y(2)-Y(1))+X(1)
    RETURN
    END

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SUBROUTINE JET(RJET,HJET,AJET,RJET,THER,VRJET,V7JET,WJET,TDM,
1 AMJET,ASTEP,JSTEP,RPM,ANGLE,PITCH,FSWIR,WSWIR)

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C
C
C THIS SUBROUTINE IS FOR GETTING JET TRAJECTORY AND AIR ENTRAINMENT
COMMON /GEOMT/ STROKE,BORE,CONL,VCLER,VCUP,RCUP,CYLN
COMMON /JETDAT/ WSWIR,ALPHA,BETA,RHGAS
C RJET=RADIAL JET LOCATION FROM CENTER(CM) (GIVEN AND RETURNED)
C HJET=VERTICAL JET LOCATION FROM CYL. HEAD (GIVEN AND RETURNED)
C AJET=TANGEN. JET LOCATION FROM NOZZLE HEAD (GIVEN AND RETURNED)
C AJET=TANGEN. JET LOCATION FROM INJECTION NOZZ. (GIVEN AND RETURNED)
C RJET=JET RADIUS(CM) (GIVEN AND RETURNED)
C THER=CONTACTING ANGLE(RAD) (GIVEN AND RETURNED)
C VRJET=JET VELOCITY OF RADIAL DIRECTION(CM/SEC) (GIVEN AND RETURNED)
C V7JET=JET VEL. VERTICAL DIRECTION(CM/SEC) (GIVEN AND RETURNED)
C WJET=JET ANGULAR VELOCITY(RAD/SEC) (GIVEN AND RETURNED)
C TDM=ENTRAINED MASS(G/GIVEN TIME) (RETURNED)
C AMJET=JET MASS(G) (GIVEN AND RETURNED)
C ASTEP=CALCULATION INTERVAL OF MAIN PROGRAM(DEG) (GIVEN)
C JSTEP=HOW MANY TIMES DO YOU WANT TO CALCULATE IN ONE CALCULATION
C INTERVAL OF MAIN PROGRAM (GIVEN)
C RPM=ENGINE SPEED(RPM) (GIVEN)
C ANGLE=CRANK ANGLE (DEG),TDC =360 (GIVEN)
C PITCH=PITCH OF JET ELEMENT(GIVEN INPUT ROUTINE) (GIVEN)
C FSWIR=CONSERVATION RATIO OF SWIRL (GIVEN)
C STROKE ,BORE,CONL,VCLER,VCUP,RCUP,WSWIR,ALPHA,BETA,RHGAS ARE
C GIVEN IN COMMON
C (SEE THE INPUT ROUTINE TO CHECK THE MEANINGS OF THESE VALUES)
C SUBROUTINE REQUIRED:
C VGAS
C CONT
  DIMENSION YX(2),YY(2)
  RCUP=2.463R
  PCYL=BORE/2.
  TDM=0.
  AASTEP=ASTEP/FL0AT(JSTEP)
  C1=ASTEP/(6.*RPM)
  C2= AASTEP/(6.*RPM)
  C3=1./(6.*RPM)
  VJET=SQRT(VRJET**2 +V7JET**2 +(RJET*WJET)**2 )
  DO 3000 I=1,JSTEP
    RHJET=AMJET/((3.1416*RJET**2*(1.-THER/(2.*3.1416))+BJET**2
1 *SIN(THER)/2.)*VJET*PITCH/(6*RPM))
    ANGLJ=ANGLE+FL0AT(I)*AASTEP
    ANG=ANGLJ*3.1416/180.
    HIGH=SQRT(1.-(STROKE/2.*SIN(ANG)/CONL)**2 )
    HIGH=VCLER/(3.1416*BORE*BORE/4.)+STROKE/2.*(1.-COS(ANG))
1 +CONL*(1.-HIGH)
C
C GAS VELOCITY SURROUNDING THE JET
  CALL VGAS(RJET,HJET,RPM, ANGLJ,VRGAS,V7GAS,WSWIR,VPTIS,FSWIR)
1111 FORMAT(7E12.4)
C
C CALCULATION OF THE PARALLEL VELOCITY COMPONENT TO THE JET
  VI=SQRT(VRJET**2 +(RJET*WJET)**2 +V7JET**2 )
  VI=(VRJET*VRGAS+RJET**2.*WSWIR*WJET+V7JET*V7GAS)/VI
C
C CALCULATION OF THE NORMAL VELOCITY COMPONENT TO THE JET
  VN=VRGAS**2 +(RJET*WSWIR)**2 +V7GAS**2
  XXX=VN-VI**2

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      IF (XXX.GT.0.) GO TO 50
      VN=0.
      GO TO 60
50  VN=SQRT(VN-VI**2)
60  CONTINUE

C
C  CHANGES OF MASS AND VELOCITY COMPONENTS OF THE JET
C  CHANGE OF MASS (G)
      DM= VJET*SQRT(RHJET/RHGAS)*RHGAS*PITCH/(6.*RPM)
      DM=DM*2.*3.1416*RJET*(ALPHA*ABS(VJET-VI)+BETA*ABS(VN))
      DM=DM*(1.-THER/(2.*3.1416))
      DM=DM*C2
      TDM=TDM+DM
      AMJET=AMJET+DM
C  CHANGE OF VERTICAL VELOCITY
      DVZ=DM/AMJET*(VZGAS-VZJET)
C  CHANGE OF RADIAL VELOCITY
      DVR=AMJET*2*JET*(WJET**2 -RHGAS/RHJET*WSWIR**2 )
      DVR=DVR*C2
      DVR=(DVR-(VRJET-VRGAS)*DM)/AMJET
C  CHANGE OF ANGULAR VELOCITY
      DW=((WSWIR-WJET)*RJET*DM-2.*AMJET*VRJET*WJET*C2)/(AMJET*RJET)
C  CHANGE OF TOTAL JET VELOCITY
      DV=(RJET**2.*WJET*DW+RJET*WJET**2 *VRJET*C2+VRJET*DVR+VZJET*DVZ)
      DV=DV/VJET

C
C  NEW STATE CONDITIONS OF THE JET
      VJET=VJET+DV
      WJET=WJET+DW
      VRJET=VRJET+DVR
      VZJET=VZJET+DVZ
      RJET=RJET+VRJET*C2
      ALJET=VJET*PITCH/(6.*RPM)
      VOLJE=DM/RHGAS+(AMJET-DM)/RHJET
C  JET RADIUS WITHOUT CONTACTING ANY WALL
      BJETO=SQRT(VOLJE/(3.1416*ALJET))
      HJET=HJET+VZJET*C2
      AJFT=AJFT+WJET*C2

C
C  CALCULATION OF THE JET CONFIGURATION
      X1=RJET+BJETO
      X2=HJET+BJETO
      X5=HIGH+VCUP/(3.1416*PCUP*RCUP)
      IF (HJET.GT.HIGH) GO TO 100
      IF (RCYL.GT.X1) GO TO 200
      IF (RCYL.GT.RJET) GO TO 300

C
C  JET IS RESTRICTED BY THE CYLINDER WALL (VRJET=0.)
      VRJET=0.
      RJET=1.414*BJETO
      THER=3.1416
      RJET=RCYL
      GO TO 200

C
C  JET IS CONTACTING WITH THE CYLINDER WALL
300  NN=0
      X3=RJET
      X4=RCYL
      GO TO 1500
200  IF (X2.LT.HIGH) GO TO 400

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      IF(X1.LT.RCUP) GO TO 400
      IF(RJET.LT.RCUP) GO TO 500
C
C JET IS CONTACTING WITH THE PISTON HEAD
      NN=0
      X3=HJET
      X4=HIGH
      GO TO 1500
C
C JET IS NOT CONTACTING
400 RJET=RJET0
      THER=0.
      GO TO 2000
100 IF(RJET.LT.RCUP) GO TO 600
      SL=ABS(HJET-HIGH)
      SP=ABS(RJET-RCUP)
      IF(SL.GT.SP) GO TO 700
C
C JET IS RESTRICTED BY THE PISTON HEAD(VZJET=VPIS)
      VZJET=VPIS
      RJET=1.414*RJET0
      THER=3.1416
      HJET=HIGH
      GO TO 2000
700 IF(HJET.GT.X5) GO TO 800
C
C JET IS RESTRICTED BY THE PISTON CUP(VRJET=0.)
      VRJET=0.
      RJET=1.414*RJET0
      THER=3.1416
      RJFT=RCUP
      GO TO 2000
C
C JET IS RESTRICTED BY THE PISTON CUP EDGE(VRJET=0. AND VZJET=VPIS)
800 VRJET=0.
      VZJET=VPIS
      RJET=RCUP
      HJET=X5
      RJFT=1.414*RJET0
      GO TO 2000
600 IF(RCUP.LT.X1) GO TO 900
      IF(X5.LT.X2) GO TO 1000
C
C JET IS IN THE PISTON CUP WITHOUT ANY RESTRICTION
      RJFT=RJET0
      THER=0
      GO TO 2000
1000 IF(X5.LT.HJET) GO TO 1100
C JET IS CONTACTING WITH THE PISTON BOTTOM
C
      NN=0
      X3=HJET
      X4=X5
      GO TO 1500
C
C JET IS RESTRICTED BY THE PISTON BOTTOM
1100 RJET=1.414*RJET0
      THER=3.1416
      HJET=X5
      VZJET=VPIS

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      GO TO 2000
900  IF(RCUP.LT.RJET) GO TO 1200
C
C  JET IS CONTACTING WITH THE PISTON CUP WALL
500  N1=0
      X3=RJET
      X4=RCUP
      GO TO 1500
C
C  JET IS RESTRICTED BY THE PISTON CUP WAL_
1200 BJET=1.414*BJETO
      THER=3.1416
      RJET=RCUP
      VRJET=0.
      GO TO 2000
C
C  SOLVE THE CONTACTING ANGLE
1500 ITEL=1
1550 IF(RJET.GT.(X4-X3)) GO TO 1600
      RJET=X4-X3
1600 ANG1=2.*ATAN(SQRT(RJET*RJET-(X4-X3)*(X4-X3))/(X4-X3))
      THER=ANG1
      AREA1=3.1416*RJET*RJET*(1.-ANG1/(2.*3.1416))+(X4-X3)*SIN(ANG1
1  /2.)*RJET
      AREA2=3.1416*BJETO*BJETO
      ERRO=(AREA1-AREA2)/AREA2
      IF(ABS(ERRO).LT.0.005) GO TO 2000
      Y0=0.
      XNEXT=0.1
      CALL CONT(RJET,ERRO,XNEXT,Y0,XX,YY,N1)
1990  FORMAT(2E12.4)
      ITEL=ITEL+1
      IF(ITES.GT.30) GO TO 1990
      GO TO 1550
1990  WRITE(6,1999)
1999  FORMAT('STOP DUE TO THE OVER ITERATION')
2000  CONTINUE
3000  CONTINUE
      RETURN
      END

```

SUBROUTINE OPFPA

C

C

C THIS SUBROUTINE IS FOR OPERATION OF EACH PROCESS

COMMON/EPROP/ TECHF(100),EFUEL(100),EANGL(100),FMWT(100),

1 DHFUEL(100),DHLOS(100),DIEMAS(100),DOEMAS(100),

1 ERGAS(100),ECP(100),FENTH(8,100),FMASS(8,100),EEQUI(8,100),

1 EVOL(8,100),FTEMP(8,100),PCYL(8)

COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,IF

COMMON /FUFLP/ FUEL,FYCAL,ZM,ZN,PST,SAFC,VACAL

COMMON /TIMIG/ AINT0,AFXI0,AINTC,AEXTC,AFUELS,AFUELE

COMMON /OSOPF/ LPT,INP,LINECO,LINEST,ITEL,LITEL

COMMON/CONTL/ ASTIN,ASTCL,ASTCR,ASTEX,ASTOV,PRININ,PRINCL,PRINEX,

1 PRINOV

COMMON /STAT1/ RPM,JLAST,NJET,PHIO,EGR

COMMON /HETR1/ PRASF,TBASE,VBASE,COHT1,COHT2,COHT,RHR(10)

COMMON /GEOMT/ STROKE,RORE,CONL,VCLFAR,VCUP,RCUP,CYLN

COMMON /SUM2/ TTGINT,TTGEXT,TTQEXT,TTQHTR(10),TQHTR(10),PS

COMMON/INF10/ NINEF,XINEF(20),YINEF(20),AREIND,PINT,TINT,GINT,

1 EQUINT,AREINT,XINV

COMMON /AMPTE/ TAMR,PAMR

COMMON /NOXSP/ CONNO(100),PPMNO(100),WNO(100),SUMOM(100),PPMEXT

ANGLE=ANGLE+ASTEP

IF (ANGLE-AEXTC) 100,120,120

100 IF (JCOND-1) 110,9000,9000

110 IF (JLAST.EQ.1) GO TO 112

C

C SET THE LAST COMPUTING STEP

ASTEP=AINT0-(ANGLE-ASTEP)

ANGLE=AINT0

JLAST=1

GO TO 9000

C

C INTAKE AND EXHAUST VALVE OPEN

112 JCOND=1

JLAST=0

ASTEP=ASTOV

LINEST=FIX(PRINOV)

LINECO=0

WRITE(LPT,7000)

WRITE(LPT,7010)

WRITE(LPT,7020)

WRITE(LPT,7030)

GO TO 9000

120 IF (ANGLE-AINTC) 130,140,140

130 IF (JCOND-2) 150,9000,9000

150 IF (JLAST.EQ.1) GO TO 152

ASTEP=AEXTC-(ANGLE-ASTEP)

ANGLE=AEXTC

JLAST=1

GO TO 9000

C

C INTAKE VALVE OPENS

152 JCOND=2

JLAST=0

ASTEP=ASTIN

LINEST=FIX(PRININ)

LINECO=0

WRITE(LPT,7200)

WRITE(LPT,7010)

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WRITE(LPT,7220)
WRITE(LPT,7230)
GO TO 9000
140 IF(ANGLE-AFUELS) 160,170,170
160 IF(JCOND-3) 180,9000,9000
180 IF(JLAST.EQ.1) GO TO 182
  ASTEP=AINTC-(ANGLE-ASTEP)
  ANGLE=AINTC
  JLAST=1
  GO TO 9000
C
C COMPRESSION PROCESS
182 JCOND=3
  JLAST=0
  ASTEP=ASTCL
  LINEST=IFIX(PRINCL)
  LINECO=0
C
C CALCULATE THE OVERALL EQUIVALENCE RATIO
C
  PHIO=0.5
  DO 172 I=1.4
    FRES=(EMASS(2,1)-TTGINT)*PHIO/(SAFC+1.)
    FEGR=TTGINT*PHIO*EGR/(SAFC+1.)
    PHIO=(FUEL+FRES+FEGR)/(EMASS(2,1)-FRES+FEGR)*SAFC
  172 CONTINUE
C
C CALCULATE THE VOLUMETRIC EFFICIENCY
  DEL=ZN/ZM
  CALL UPROP(PAMB,TAMB,0.,DEL,PST,0.,DJM,DUM,DUM,DUM,DUM,DUM,
1 DUM,RGAS,DUM)
  DISP=3.1416/4.*BORE*BORE*STROKE
  THMASS=PAMB*DISP/(RGAS*TAMB)
  EFFVOL=TTGINT/THMASS
C
C CORRECT THE EQUIVALENCE RATIO OF CHARGED AIR
  EEQUI(2,1)=(FRES+FEGR)/(EMASS(2,1)-FRES-FEGR)*SAFC
  TRASE=ETEMP(2,1)
  PRASE=PCYL(2)
  VRASE=EVOL(2,1)
C
C NOX CONCENTRATION FOR CHARGED AIR
  CONNO(1)=(EMASS(2,1)-TTGINT)/EMWT(1)*PPMEXT/1000000.
1 +TTGINT*FEGR/EMWT(1)*PPMEXT/1000000.
  PPMNO(1)=1000000.*CONNO(1)*EMWT(1)/EMASS(2,1)
  WNO(1)=30.*CONNO(1)
  WRITE(LPT,6100) PHIO
  WRITE(LPT,6120) EFFVOL
  WRITE(LPT,6140) EEQUI(2,1)
  WRITE(LPT,6160) PPMNO(1),WNO(1)
  WRITE(LPT,7400)
  WRITE(LPT,7010)
  WRITE(LPT,7420)
  WRITE(LPT,7430)
  GO TO 9000
170 IF(ANGLE-AFXT0) 190,200,200
190 IF(JCOND-4) 210,192,192
192 IF(ANGLE-AFUELE-20.) 9000,9000,194
194 ASTEP=ASTCL
  GO TO 9000

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210 IF(JLAST.EQ.1) GO TO 212
    ASTEP=AFUELS-(ANGLE-ASTEP)
    ANGLE=AFUELS
    JLAST=1
    GO TO 9000
C
C FUEL STARTS TO BE INJECTED
C COMBUSTION AND EXPANSION
212 JLAST=0
    JCOND=4
    ASTEP=ASTCR
    LINEST=IFIX(PRINCL)
    LINECO=0
    WRITE(LPT,7600)
    WRITE(LPT,7010)
    WRITE(LPT,7620)
    WRITE(LPT,7630)
    GO TO 9000
220 IF(ANGLE-AINT0-720.) 220,230,230
220 IF(JCOND-5) 240,9000,9000
240 IF(JLAST.EQ.1) GO TO 242
    ASTEP=AEXT0-(ANGLE-ASTEP)
    ANGLE=AEXT0
    JLAST=1
    GO TO 9000
C
C EXHAUST VALVE OPENS
242 JCOND=5
    JLAST=0
    ASTEP=ASTEX
    LINEST=IFIX(PRINFX)
    LINECO=0
    IF(IE.EQ.1) GO TO 244
C
C CALCULATE THE TOTAL MASS AND ENTHALPY
    TENTH=0.
    TMASS=0.
    DO 7320 I=1,IF
        TENTH=TENTH+EFENTH(2,I)*EMASS(2,I)
        TMASS=TMASS+EMASS(2,I)
7320 CONTINUE
C
C CALCULATE THE AVERAGE ENTHALPY
    AVENT=TENTH/TMASS
C
C CALCULATE THE AVERAGE TEMPERATURE
C FIRST FIND OUT THE ELEMENT WHICH ENTHALPY IS CLOSE TO THE
C AVERAGE ENTHALPY
    DENTM=1000.
    II=1
    DO 7330 I=1,IF
        DENT=ABS(AVENT-EFENTH(2,I))
        IF(DENTM.LT.DENT) GO TO 7330
        DENTM=DENT
        II=I
7330 CONTINUE
C
C DEFINE THE NEW PROPERTIES
    ETEMP(2,1)=ETEMP(2,II)+(AVENT-EFENTH(2,II))/FCP(II)
    EFQUI(2,1)=P-II0

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      FENTH(2,1)=AVENT
      EMASS(2,1)=TMASS
      CALL HPROD(PCYL(2),FTEMP(2,1),FEQUI(2,1),DEL,PSI,ENTHLP,CSURP,
1 CSUBT,RHO,DRHODT,DRHODP,EMWT(1),ERGAS(1),CVBG,EBGR)
      ECP(1)=ERGAS(1)/41.443+CVBG
      EVOL(2,1)=VCYLN
      IE=1

C
C NOX AMOUNT WILL BE DEFINED.
C FXHAUST NOX ON MASS BASE
      ANOXEX=TWNQ*ITGINT/TMASS*RPM/120.
      WRITE(LPT,7340)
      WRITE(LPT,7342) PCYL(2),ETEMP(2,1),FEQUI(2,1),FENTH(2,1),
1 EMASS(2,1)
      WRITE(LPT,7450) TPPM,ANOXEX
7340 FORMAT(/,10X,***EXPANSION PROCESS IS CALCULATED AS ONE ELEMENT**
1*)
7342 FORMAT(15X,18HPRESSURE = ,F10.2,'ATA',/,
1 15X,18HAV. TEMPERATURE = ,F10.1,'< DEG',/,
2 15X,18HAV. EQUI. RATIO = ,F10.3,/,
3 15X,18HAV. ENTHALPY = ,F10.2,'CAL/G',
4 15X,18HTOTAL MASS = ,F10.4,'G')
244 CONTINUE
      WRITE(LPT,7800)
      WRITE(LPT,7010)
      WRITE(LPT,7820)
      WRITE(LPT,7230)
      GO TO 9000
230 JCOND=5
9000 ANGLE=ANGLE-ASTEP
      RETURN
6100 FORMAT(/,10X,OVERALL EQUIVALENCE RATIO = ,F12.3)
6120 FORMAT(10X,VOLUMETRIC EFFICIENCY = ,F12.3)
6140 FORMAT(10X,CORRECT CHARGED AIR PHI = ,F12.3)
6160 FORMAT(10X,INDUCED AIR AND REG. GAS NOX,/,
1 15X,PPM = ,F12.1,5X,MASS = ,E12.3,'G')
7000 FORMAT(1H1,5X,INTAKE AND EXHAUST VALVE OPEN,/)
7010 FORMAT(1H,OUTPUT DATA)
7020 FORMAT(2X,4HTHEO,3X,4H P,3X,4H T,3X,4H V,3X,4HWORK,
1 3X,7HCYL.MAS,3X,15H HEAT TRANSFER,6X,4HAEFI,3X,4H GWI,5X,
2 4HAEFF,3X,4H GWE)
7030 FORMAT(2X,4HDEG,3X,4HATA,3X,4H K,2X,5HCM**3,3X,4H PS,
1 3X,7H KG,3X,15H CAL/A CAL,5X,5HCM**2,3X,4H G/S,4X,
2 5HCM**2,3X,4H G/S,/)
7200 FORMAT(1H1,5X,INTAKE VALVE OPEN,/)
7220 FORMAT(2X,4HTHEO,3X,4H P,3X,4H T,3X,4H V,3X,4HWORK,
1 3X,7HCYL.MAS,3X,15H HEAT TRANSFER,5X,4HAEFI,3X,4H GWI)
7230 FORMAT(2X,4HDEG,3X,4HATA,3X,4H K,2X,5HCM**3,3X,4H PS,
1 3X,7H G,3X,15H CAL/A CAL,5X,5HCM**2,3X,4H G/S,/)
7400 FORMAT(1H1,5X,COMPRESSION,/)
7420 FORMAT(2X,4HTHEO,3X,4H P,3X,4H T,3X,4H V,3X,4HWORK,
1 3X,7HCYL.MAS,3X,15H HEAT TRANSFER,7X,4HFSWR,3X,4H S,RT)
7430 FORMAT(2X,4HDEG,3X,4HATA,3X,4H K,2X,5HCM**3,3X,4H PS,
1 3X,7H G,3X,15H CAL/A CAL,11X,3X,4H*PPM)
7450 FORMAT(/,10X,***EXHAUST NOX***,/,
1 15X,15HNOX CONCEN. = ,F10.1,'PPM',/,
2 15X,15HTOTAL MASS = ,E12.3,'G')
7600 FORMAT(1H1,5X,COMBUSTION AND EXPANSION,/)
7620 FORMAT(2X,4HTHEO,3X,PRESS,9X,PS,7X,FS,1P,7X,S,RT,7X,
1 PPM,9X,WNO,/,1X.

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1          3HNUJM,1X,2H**3X,4HT.AV,3X,4HRTM,3X,4HR.OT.
1 3X,4HMASS,3X,4HPMAS,3X,4HBMAS, 3X,4H V ,3X,4HFQUI,3X,4H CP,
2 3X,4HENTH,3X,4H PPM,3X,4H WNO,1X,1H- JET LOCATIONS ,1X,
1 4HRJET,1X,5HC.AVG ,2X,4H.T. )
7630 FORMAT( 6X,4X,4H K ,3X,4H K ,3X,4X ,3X,4H MG ,3X,4H MG .
1 3X,4H MG ,2X,5HCM**3, 7X,2X,5HCAL/G,2X,5HCAL/G,2X,4H PPM,
2 1X,7HG*10**6,1X,5HR(CM) , 1X,5HZ(CM),1X,5H DEG ,2X,4H CM ,2X,
3 4H DEG,2X,4H CAL)
7800 FORMAT(1H1.5X, 'EXHAUST VALVE OPEN',/)
7820 FORMAT(2X ,4HTHED,3X,4H P ,3X,4H T ,3X,4H V ,3X,4HWORK.
1 3X,7HCYL.MAS,3X,15H HEAT TRANSFER,5X,4HAEFE,3X,4H GWF)
END

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SUBROUTINE EXHOR

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C
C EXHAUST PORT CALCULATION
C THIS PROGRAM WAS ORIGINALLY MADE USING METER-KG UNIT
C
C COMMON/EPROP/ IECHF(100),EFJEL(100),EANGL(100),EMWT(100),
1 DHFUEL(100),DHLOS(100),DIEMAS(100),DOEMAS(100),
1 ERGAS(100),ECP(100),EFNTH(9,100),FMAS(8,100),FEQUI(8,100),
1 EVOL(8,100),ETEMP(8,100),PCYL(8)
COMMON/EXFLO/NEXEF,XEXEF(20),YEXEF(20),AREEXD,PEXT,TEXT,GFXT,
1 IGLFT,TLEFT,QEXT,QFLOW,ELEFT,AREEXT,XEXV
COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,IE
COMMON /TIMIG/ AINT0,AFXT0,AINTC,AFXTC,AFUELS,AFUELE
COMMON /FUELP/ FUEL,FKCAL,ZM,ZN,PSI,SAFC,VACAL
COMMON /STAT1/ RPM,JLAST,NJET,PHIO,ESR
IF(PEXT-PCYL(1)) 50,50,60
C EXHAUST FLOW IS FROM CYLINDER TO EX. PORT
C P VALUE DOESN'T CHANGE MUCH.
50 CEXT=-1.
PHIGH=ERGAS(1)*9.8
PHIGH=PCYL(1)*10000.
PREX=PEXT/PCYL(1)
EHIGH=FEQUT(1,1)
IF(IGLFT) 51,51,52
C IGLFT=1 THERE IS RESIDUAL GAS
C IGLFT=0 THERE IS NOT RESIDUAL GAS
52 THIGH=ETEMP(1,1)
AKCYL=1.34
AKHIGH=AKCYL
GO TO 100
51 THIGH=TLEFT
PHIGH=ERGAS(1)*9.8
AKLEF=1.34
AKHIGH=AKLEF
GO TO 100
C EXHAUST FLOW IS FROM EX. PORT TO CYLINDER
60 PHIGH=ERGAS(1)*9.8
CEXT=1.
EHIGH=FEQUT(1,1)
PHIGH=PFXT*10000.
PREX=PCYL(1)/PFXT
THIGH=ETEMP(1,1)
AKEXT=1.34
AKHIGH=AKEXT
C
C CALCULATE THE EFFECTIVE EXHAUST FLOW AREA
100 IF (ANGLE-360.) 150,150,160
150 ANAE=(ANGLE-(AFXT0-720.))/(AFXTC-(AFXT0-720.))
GO TO 200
160 ANAE=(ANGLE-AFXT0)/(AFXTC-AFXT0+720.)
200 CALL TWODIM(NEXEF,XEXEF,YEXEF,ANAE,AREFAC)
AREEXT=AREFXD*AREFAC
AREEXT=AREEXT/10000.
PRCRIT=(2./((AKHIGH+1.)))*((AKHIGH/(AKHIGH-1.))
C
C CHECK WHETHER FLOW IS CHOKED OR NOT
IF(PRCRIT-PREX) 300,300,310
C
C CHOKED

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310 PREX=PRCRIT
C
C NEXT EQUATION IS BASED ON METER -KG UNIT
300 GEXT=      SQRT(ABS(2.*AKHIGH*9.8/RHIGH/THIGH
1 / (AKHIGH-1.)*(PREX** (2./AKHIGH)-PREX** ((AKHIGH+1.)
2 /AKHIGH))))
GEXT=PHIGH*AREFXT/6./RPM*GEXT
GEXT=CEXT*GFXT
GFXT=GEXT*1000.
AREFXT=AREFXT*10000.
IF (CEXT) 410,410,400
410 TMANI=THIGH*PREX** ((AKHIGH-1.)/AKHIGH)
OEXT=GEXT*ENT(TMANI,FHIGH,SAFC)
GO TO 1000
400 OEXT=GEXT*ENT(TEXT,FHIGH,SAFC)
1000 RETURN
END

```

```

C      SUBROUTINE VOLCY(ANGLE,VCYL,DVCYL,STROKE,BORE,CONL,VCLFAR,VCUP)
        PAI=3.141593
        ANGRAD=ANGLE*PAI/180.
        HSTROK=STROKE/2.
C      DELTA VOLUME CALCULATION
        DVCYL=PAI*BORE**2/4.*(HSTROK*SIN(ANGRAD)+HSTROK**2*SIN(ANGRAD)
1      *COS(ANGRAD)/SQRT(CONL**2-HSTROK**2*SIN(ANGRAD)**2))*PAI/180.
C      VOLUME CALCULATION
        DISTB=CONL*(1.-SQRT(1.-(HSTROK/CONL)**2*SIN(ANGRAD)**2))
1      +HSTROK*(1.-COS(ANGRAD))
        VCYL=VCLFAR+VCUP+PAI*BORE*BORE/4.*DISTB
        RETURN
        END
C

```

```

      SUBROUTINE TWOIM(N,X,Y,XIN,YOUT)
      DIMENSION X(1),Y(1)
      XDUMMY=XIN
      IF(XDUMMY-X(1)) 510,810,910
510  XDUMMY=X(1)
810  CONTINUE
      IF(XDUMMY-X(N)) 820,820,520
520  XDUMMY=X(N)
820  CONTINUE
      J=0
      3 J=J+1
      5 IF(XDUMMY-X(J)) 1,2,3
      2 YOUT=Y(J)
      GO TO 4
      1 YOUT=Y(J)-(X(J)-XDUMMY)/(X(J)-X(J-1))*(Y(J)-Y(J-1))
      4 RETURN
      END

```

SUBROUTINE HEATR

```

C
C HEAT TRANSFER CALCULATION
COMMON/ERROR/ IFCHF(100),EFJEL(100),FANGI(100),FMWT(100),
1 DHFUEL(100),DHLOS(100),DIEMAS(100),DIEMAS(100),
1 FRGAS(100),FCP(100),FENTH(8,100),FMASS(8,100),FEQUI(8,100),
1 EVOL(8,100),ETEMP(8,100),PCYL(8)
COMMON/STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,IF
COMMON/STAT1/ RPM,ILAST,NJET,PHIO,FCR
COMMON/GEOMT/ STROKE,RORE,CONL,VCLFAR,VCUP,RCUP,CYLN
COMMON/HETPS/ NDIVID,TMETAL(10),QHTPC(10),ARF(10)
COMMON/JETS/ RJET(50),HJET(50),AJET(50),RJET(50),THER(50),
1 VPJET(50),VZJET(50),WJET(50),VJET(50),AINJ(50),RHJET(50),
2 PITCH(50)
COMMON/SUPGAS/ FSWIR,WSWIR,SDECAF
COMMON/HETR1/ PRASE,TRASE,VRASE,COHT1,COHT2,COHT,RHR(10)
DIMENSION HTCON2(10),HTI(10)
ANGRAD=ANGLE*3.1416/180.
CALL VOLCY(ANGLE,CYLV,DIM,STROKE,RORE,CONL,VCLFAR,VCUP)
C
C GET THE H.T. AREA OF CYLINDER WALL
C
ARF(2) = (CYLV-VCUP)*4./RORE
DO 200 I=1,NDIVID
QHTPC(I)=0.
200 CONTINUE
DO 202 I=1,IF
DHLOS(I)=0.
202 CONTINUE
HTCON1=COHT*7014.*RORE**(-0.2)*PCYL(1)**0.8/(2.16*10.**8*DDM)
GO TO (210,210,220,220,210),JCOND
C
C ISENTROPIC TEMPERATURE
C
220 PISEN=PRASE*(VRASE/CYLV)**1.32
HTCON2=COHT1*(STROKE*DDM/30.)*100.*COHT2*CYLV*TRASE/(PRASE
1 *VRASE)*(PCYL(1)-PISEN)
GO TO 230
C
C FOR PROCESS --INTAKE,EXHAUST AND VALVE OVERLAP
C
210 PISEN=PCYL(1)
HTCON2=COHT1*(STROKE*DDM/30.)
230 CONTINUE
DO 300 I=2,NDIVID
C
C 0.4 IS AN ADJUSTING FACTOR
HTCON2(I)=(HTCON2+WSWIR**2*H(I)*0.4)**0.8
300 CONTINUE
IFILL=0
IF(I2.F0.1) GO TO 1000
TARFA=0.
DO 2400 J=1,IF
I=IF+1-J
IF(I.F0.1) GO TO 2120
C
C THE AREA OF JET CONTACTING WITH WALL
APFATH=RJET(I)*SIN(THER(I)/2.)*2.*VJET(I)*PITCH(I)/(6.*RPM)
TARFA=TARFA+APFATH
C
C CHECK WHETHER THE PISTON CUP IS FULL WITH JET ELEMENTS OR NOT
C

```

```

      IF (TAREA.GT.ARF(4) ) GO TO 2090
      RTAREA=ARE(2)+ARE(3)+ARE(5)+ARE(6)+ARE(7)
C
C  PISTON CUP IS NOT FILLED WITH JET ELEMENTS
      DHLOS(I)=HTCON1*ETEMP(1,I)**(-0.53)*HTCO2(4)*ARFATH*
      1 (ETEMP(1,I)-TMETAL(4))
      QHTPC(4)=QHTPC(4)+DHLOS(I)
      QHTPC(1)=QHTPC(1)+DHLOS(I)
      GO TO 2900
C
C  PISTON CUP IS FILLED WITH JET ELEMENTS
      2090 IFILL=1
      2100 AA=ARFATH*HTCON1*ETEMP(1,I)**(-0.53)
      RTAREA=ARE(2)+ARE(3)+ARE(5)+ARE(6)+ARE(7)
      2110 DO 2110 JJ=2,NNDIVIN
      IF (IFILL.EQ.0) GO TO 2112
      IF (JJ.EQ.4) GO TO 2110
      2112 HTI(JJ)=AA*ARE(JJ) /RTAREA*HTCO2(JJ)*(ETEMP(1,I)-TMETAL(JJ))
      QHTPC(JJ)=QHTPC(JJ)+HTI(JJ)
      DHLOS(I)=DHLOS(I)+HTI(JJ)
      QHTPC(1)=QHTPC(1)+HTI(JJ)
      2110 CONTINUE
      GO TO 2900
C
C  FOR ELEMENT 1
      2120 XX=ARE(4)
      IF (IFILL.EQ.0) GO TO 2114
      AA=(ARE(2)+ARE(3)+ARE(4)+ARE(5)+ARE(6)+ARE(7)-TAREA)*HTCON1*
      1 ETEMP(1,I)**(-0.53)
      RTAREA=ARE(2)+ARE(3)+ARE(5)+ARE(6)+ARE(7)
      GO TO 2116
      2114 RTAREA=ARE(2)+ARE(3)+ARE(5)+ARE(6)+ARE(7)+ARE(4)-TAREA
      XX=ARE(4)
      ARE(4)=ARE(4)-TAREA
      AA=RTAREA*HTCON1*ETEMP(1,I)**(-0.53)
      GO TO 2116
      2900 CONTINUE
      ARE(4)=XX
      GO TO 9000
      1900 HTCO11=HTCON1*ETEMP(1,I)**(-0.53)
      DO 1900 I=2,NNDIVIN
      QHTPC(I)=HTCO11*HTCO2(I)*(ETEMP(1,I)-TMETAL(I))*ARE(I)
      QHTPC(1)=QHTPC(1)+QHTPC(I)
      1900 CONTINUE
      DHLOS(1)=QHTPC(1)
      9000 RETURN
      END

```



```

SUBROUTINE DELTA(DVCYL,FNTINT)
COMMON/EPROP/ IECHF(100),EFUFL(100),EANGI(100),FMWT(100),
1 DHFUEL(100),DHLOS(100),DIEMAS(100),DOEMAS(100),
1 FPGAS(100),FCP(100),FENTH(8,100),FMASS(8,100),FEQUI(8,100),
1 EVOL(8,100),ETEMP(8,100),PCYL(8)
COMMON /STATE/ ANGLE1,ANGLE,JCONO,ASTEP,NSTEP,IE
COMMON/FXFLD/HFXEF,XEXEF(20),YFEXF(20),AREEXD,PEXT,TEXT,GEXT,
1 IGLEFT,TLFFT,OFEXT,OFLOW,FLEFT,ARFEXT,XEXV
DIMENSION DO(100),HENTH(100)
AJ=42.68
DO 50 I=1,IE
DO(I)=DHFUEL(I)-DHLOS(I)
HENTH(I)=EFENTH(I,I)
50 CONTINUE
FNTCYL=HENTH(1)
AA=DO(1)*QFLOW - (DIEMAS(1)-
1 DOEMAS(1))*HENTH(1)
AA=AA*EVOL(1,1)/(EMASS(1,1)*FCP(1)*ETEMP(1,1))+(DIEMAS(1)
1 -DOEMAS(1))/FMASS(1,1)*EVOL(1,1)
RR=EVOL(1,1)*EVOL(1,1)/(EMASS(1,1)*FCP(1)*ETEMP(1,1)*A.I)
1-FVOL(1,1)/PCYL(1)
IF(IE.LT.2) GO TO 200
DO 100 I=2,IE
AA=AA+EVOL(1,I)/(EMASS(1,I)*FCP(I)*ETEMP(1,I))*(DO(I)
1 +DIEMAS(I)*HENTH(1) -DOEMAS(I)*HENTH(I) - (DIEMAS(I)
2 -DOEMAS(I))*HENTH(I)) + (DIEMAS(I)-DOEMAS(I))/EMASS(1,I)
3 *EVOL(1,I)
RR=RR+EVOL(1,I)*EVOL(1,I) / (EMASS(1,I)*FCP(I)
1 *ETEMP(1,I)*A.I)-EVOL(1,I)/PCYL(1)
100 CONTINUE
200 PCYL(3)=(DVCYL-AA)/RR
EVOL(3,1)=EVOL(1,1)/(FMASS(1,1)*FCP(1)*ETEMP(1,1)
1 *(DO(1)+QFLOW - (DIEMAS(1)
2 -DOEMAS(1))*HENTH(1) )+(DIEMAS(1)-DOEMAS(1))/FMASS(1,1)
3 *EVOL(1,1)+(EVOL(1,1)*EVOL(1,1)/(FMASS(1,1)*FCP(1)*ETEMP(1,1)
4 *A.I)-EVOL(1,1)/PCYL(1))*PCYL(3)
ETEMP(3,1)=ETEMP(1,1)*(PCYL(3)/PCYL(1)+EVOL(3,1)/EVOL(1,1)
1 - (DIEMAS(1)-DOEMAS(1))/EMASS(1,1))
FMASS(3,1)=DIEMAS(1)-DOEMAS(1)
FENTH(3,1)=FCP(1)*ETEMP(3,1)
IF(IE.LT.2) GO TO 400
DO 300 I=2,IE
EVOL(3,I)=EVOL(1,I)/(FMASS(1,I)*FCP(I)*ETEMP(1,I))
1*(DO(I)+DIEMAS(I)*HENTH(1) -DOEMAS(I)*HENTH(I) - (DIEMAS(I)-
2 DOEMAS(I))*HENTH(I)) + (DIEMAS(I)-DOEMAS(I))/FMASS(1,I)
3 *EVOL(1,I)+(EVOL(1,I)*EVOL(1,I)/(FMASS(1,I)*FCP(I)*ETEMP(1,I)*A.I)
4 -EVOL(1,I)/PCYL(1))*PCYL(3)
ETEMP(3,I)=ETEMP(1,I)*(PCYL(3)/PCYL(1)+EVOL(3,I)/EVOL(1,I)-
1 (DIEMAS(I)-DOEMAS(I))/FMASS(1,I))
FMASS(3,I)=DIEMAS(I)-DOEMAS(I)
FENTH(3,I)=FCP(I)*ETEMP(3,I)
300 CONTINUE
400 RETURN
END

```

FUNCTION ENT(T,E,XXX)

C
C TO CALCULATE THE ENTHALPY OF GAS AT LOW PRESSURE .(T<1800 K)
C THIS SUBROUTINE IS USED FOR CALCULATING THE ENTHALPY OF INITIAL GAS
C INSIDE THE CYLINDER. INTAKE AIR AND EXHAUST GAS.
C IT IS RECOMMENDED THAT M.MARTIN'S PROGRAMS BE USED FOR HIGH PRESSURE
C OR HIGH TEMPERATURE GASES.
C

SAFC=14.4
IF(E.LT.0.01) GO TO 100
AF=SAFC/E
GO TO 200
100 AF=0.
200 CONTINUE
IF(T-800.) 10,10,20
10 ENT =-0.405671 +0.243353*T -0.164608E-4*T**2 +0.157984E-7
1 *T**3+0.253172E-10*T**4 -0.179767E-13*T**5
IF(AF) 99,99,40
40 ENT =ENT +(14.9607 -0.126357*T +0.769710E-3*T**2-0.517585E-6
1 *T**3 +0.595961E-10*T**4 +0.833377E-13*T**5)/(AF+1.)
RETURN
20 ENT =11.3176 +0.190755*T +0.637625E-4*T**2 -0.182173E-7*T**3
1 +0.223445E-11*T**4
IF(AF) 99,99,30
30 ENT =ENT +(-42.2372 +0.199892*T +0.871219E-4*T**2 +0.600828E-7
1 *T**3 -0.299545E-10*T**4 +0.391857E-14*T**5)/(AF+1.)
99 RETURN
END

```

C***** VERSION 1.0 *** 5/29/74 *****
C
C      SUBROUTINE HPROD
C
C      PURPOSE:
C      TO CALCULATE THE SPECIFIC ENTHALPY OF THE PRODUCTS OF HYDRO
C      CARBON-AIR COMBUSTION AS A FUNCTION OF TEMPERATURE AND PRES
C      SURE, USING AN APPROXIMATE CORRECTION FOR DISSOCIATION.
C      THE PARTIAL DERIVATIVES OF H WITH RESPECT TO THESE VARIABLES
C      ARE ALSO CALCULATED, ALONG WITH THE GAS DENSITY AND ITS PAR
C      TIAL DERIVATIVES
C
C      USAGE:
C      CALL HPROD(P,T,PHI,DEL,PSI,ENTHLP,CSURP,CSURT,RHO,DRHODT,
C              DRHODP)
C
C      DESCRIPTION OF PARAMETERS:
C      GIVEN:
C      P      - ABSOLUTE PRESSURE OF PRODUCTS (ATM)
C      T      - TEMPERATURE OF PRODUCTS (DEG K)
C      PHI     - EQUIVALENC RATIO (FUEL/AIR RATIO DIVIDED BY THE
C              CHEMICALLY CORRECT FUEL/AIR RATIO)
C      DEL     - MOLAR C:H RATIO OF THE PRODUCTS
C      PSI     - MOLAR N:O RATIO OF THE PRODUCTS
C      RETURNS:
C      ENTHLP- SPECIFIC ENTHALPY OF THE PRODUCTS (KCAL/G)
C      CSURP  - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO T
C              AT CONSTANT P (CAL/G-DEG K)
C      CSURT  - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO P
C              AT CONSTANT T (CC/G)
C      RHO    - DENSITY OF THE PRODUCTS (G/CC)
C      DRHODT- PARTIAL DERIVATIVE OF RHO WITH RESPECT TO T AT
C              CONSTANT P (G/CC-DEG K)
C      DRHODP- PARTIAL DERIVATIVE OF RHO WITH RESPECT TO P AT
C              CONSTANT T (G/CC-ATM)
C
C      REMARKS:
C      1) ENTHALPY DATUM STATE IS AT T = 0 ABSOLUTE WITH
C          O2,N2,H2 GASEOUS AND C SOLID GRAPHITE
C      2) IN CASE OF PROBLEMS CONTACT MIKE MARTIN AT 253-2411
C          (ROOM 3-339 D)
C
C      SUBROUTINES AND FUNCTION SUBPROGRAMS REQUIRED:
C      DERIVS,CLDPRD
C
C      METHOD:
C      SEE MARTIN & HEYWOOD 'APPROXIMATE RELATIONS FOR THE THERMO-
C      DYNAMIC PROPERTIES OF HYDROCARBON-AIR COMBUSTION PRODUCTS'
C*****
C
C      SUBROUTINE HPROD(P,T,PHI,DEL,PSI,ENTHLP,CSURP,CSURT,RHO,DRHODT,
C      1  DRHODP,AMWT,RAVG,CAVAVG,ENERGY)
C      LOGICAL RICH,LFAN,NOTHOT,NOTWRM,NOTC_D
C
C      INITIALIZE PARAMETERS USED IN THE CALCULATION
C
C      DATA AHFCO2,AHFH2O,AHFCO/-93.965,-57.103,-27.200/
C      DATA ROVR2/.99745E-3/
C      DATA TCOLD,THOT /1000.,1100./

```

```

C
RICH = PHI .GE. 1.0
LEAN = .NOT. RICH
NOTHOT = T .LT. THOT
NOTCLD = T .GT. TCOLD
NOTWRM = .NOT. (NOTCLD .AND. NOTHOT)
EPS=(4.*DEL)/(1. + 4.*DEL)

C
C   USE SIMPLE ROUTINE FOR LOW TEMPERATURE MIXES
C
IF (NOTCLD) GO TO 5
CALL CLOPRN(P,T,PHI,DEL,PSI,ENTHLP,CSURP,CSURT,RHO,DRHODT,
1  DRHODP,IER,AMWT)
GO TO 30

C
C   CALCULATE EQUILIBRIUM CONSTANTS FOR DISSOCIATION.
C   (NOTE THAT UNITS ARE INVERSE PRESSURE TO THE 1/2 POWER)
C
5 AK1 = .39E-4 * EXP(-.3*FPS + 34000./T)
  AK2 = .14E-3 * EXP(1.3*FPS + 29000./T)

C
C   CALCULATE A, X, Y, AND U AS IN NOTES
C
  A = ((2.- FPS + PSI)/(4.*P*AK1*AK1))**.33333333
  T1 = 2.- EPS + PSI
  T2 = 1. + 2.*T1
  T3 = EPS*A
  X = A*(3.*T1 + T2*T3)/(3.*(1. + 2.*T3)*T1 + 2.*T2*T3*T3)

C
  Z = (1.- PHI)/X
  IF (RICH) Y = X/(1.- .64*Z + .30*Z**2)
  IF (LEAN) Y = X*(1. + Z + .36*Z**2)/(1. + .36*Z) - (1. - PHI)
  U = (2. - FPS + PSI)*(1.- 2.*FPS*X)/(4.*AK1*AK2*P*X)

C
C   CALCULATE THE ENTHALPY OF FORMATION FOR THIS APPROXIMATE
C   COMPOSITION
C
  ENTFOR = 1000.*ROVR2*((117. + 30.*FPS)*Y + 135.*EPS*U)
  XH2O = 2.*(1.- FPS)*PHI
  T1 = 7.*PSI + 5.*Y + 3.*J
  T2 = PSI - 3.*Y - 11

C
  IF (LEAN) GO TO 10

C
  RCVT = 2. + 2.*(7. - 4.*EPS)*PHI + T1
  RCVV = 4. + (2.- 3.*FPS)*PHI + T2
  XC02 = 2.- (2.- FPS)*PHI
  XC0 = 2.*(PHI - 1.)
  ENTFOR = ENTFOR - 1000.*ROVR2*13.*(PHI - 1.)/FP.
  GO TO 20

C
10 RCVT = 7. + (9. - 8.*FPS)*PHI + T1
  RCVV = 1. + (5.- 3.*FPS)*PHI + T2
  XC0 = 0.
  XC02 = FPS*PHI

C
20 ENTFOR = ENTFOR + (XC02*AHFC02 + XH2O*AHFH2O + XC0*AHFC0)

C
C   ADD IN TRANSLATIONAL, VIBRATIONAL, AND ROTATIONAL TERMS TO GFT

```

```

C   TOTAL ENTHALPY
C
C   TV = (3000.- 2000.*EPS + 300.*PSI)/(1.- .5*EPS + .09*PSI)
C   TV = TV/( EXP(TV/T) - 1.)
C   AMCP = (8.*EPS + 4.)*PHI + 32. + 28.*PSI
C
C   ENTHLP = (POVR2*(RCVT*T + RCVV*TV*2.) + ENTFOR)/AMCP
C
C   CALCULATE AVERAGE MOLECULAR WEIGHT, AND GET DENSITY BY
C   USING THE PERFECT GAS LAW
C
C   IF (LEAN) AMWT = AMCP/(1. + (1.- EPS)*PHI + PSI + Y + U)
C   IF (RICH) AMWT = AMCP/((2.- EPS)*PHI + PSI + Y + U)
C   RHO = .012187*AMWT*P/T
C
C   GET PARTIAL DERIVATIVES BY WAY OF A SUBROUTINE CALL
C
C   CALL DERIVS(P,T,PHI,EPS,PSI,A,X,Y,U,AMWT,CSURP,CSURT,DRHODT,
1   DRHODP)
C
C   IF CALCULATING FOR AN INTERMEDIATE TEMPERATURE, USE A WEIGHTED
C   AVERAGE OF THE RESULTS FROM THIS ROUTINE AND THOSE FROM THE
C   SIMPLE ROUTINE
C
C   IF (NOTWRM) GO TO 30
C
C   CALL CLOPRN(P,T,PHI,DFL,PSI,TH,TCP,TCT,TRHO,TDRT,TDRP,IER,AMWT)
C   W1 = (T - TCOLD)/(THOT - TCOLD)
C   W2 = 1.0 - W1
C
C   ENTHLP = W1*ENTHLP + W2*TH
C   CSURP = W1*CSURP + W2*TCP
C   CSURT = W1*CSURT + W2*TCT
C   RHO = W1*RHO + W2*TRHO
C   DRHODT = W1*DRHODT + W2*TDRT
C   DRHODP = W1*DRHODP + W2*TDRP
C
C   30 RAVG=82.057/AMWT
C   CVAVG=CSURP-1.98/AMWT
C   ENERGY=1000.*ENTHLP-1.98*T/AMWT
C
C   RETURN
C   END

```

C***** VERSION 1.1 ***

C
C SUBROUTINE CLOPRD

C PURPOSE:

C TO CALCULATE THE SPECIFIC ENTHALPY OF THE PRODUCTS OF HC-A19
C COMBUSTION AT TEMPERATURES AND PRESSURES WHERE DISSOCIATION
C OF THE PRODUCT GASES MAY BE IGNORED. THE DENSITY OF THE
C PRODUCT GAS IS ALSO CALCULATED, AS ARE THE PARTIAL
C DERIVATIVES OF BOTH OF THESE QUANTITIES WITH RESPECT TO
C PRESSURE AND TEMPERATURE.

C USAGE:

C CALL CLOPRD(P,T,PHI,DEL,PSI,ENTHLP,CSUBP,CSUBT,RHO,DRHODT,
C DRHODP,IER)

C DESCRIPTION OF PARAMETERS:

C GIVEN:

C P - ABSOLUTE PRESSURE OF PRODUCTS (ATM)
C T - TEMPERATURE OF PRODUCTS (DEG K)
C PHI - EQUIVALENCE RATIO (FUEL/AIR RATIO DIVIDED BY THE
C CHEMICALLY CORRECT FUEL/AIR RATIO)
C DEL - MOLAR C:H RATIO OF THE PRODUCTS
C PSI - MOLAR N:O RATIO OF THE PRODUCTS

C RETURNS:

C ENTHLP- SPECIFIC ENTHALPY OF THE GAS (KCAL/G)
C CSUBP - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO T
C AT CONSTANT P (CAL/G-DEG K)
C CSUBT - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO P
C AT CONSTANT T (CC/G)
C RHO - DENSITY OF THE MIXTURE (G/CC)
C DRHODT- PARTIAL DERIVATIVE OF RHO WITH RESPECT TO T AT
C CONSTANT P (G/CC-DEG K)
C DRHODP- PARTIAL DERIVATIVE OF RHO WITH RESPECT TO P AT
C CONSTANT T (G/CC-ATM)
C IER - FLAG, SET TO 1 FOR T<100 DEG K
C 2 FOR T> 6000 DEG K
C 0 OTHERWISE

C REMARKS:

C 1) ENTHALPY DATUM STATE IS AT T = 0 ABSOLUTE WITH
C O₂,N₂,H₂ GASEOUS AND C SOLID GRAPHITE
C 2) IN CASE OF PROBLEMS CONTACT MIKE MARTIN AT 253-2411
C (ROOM 3-339 D)

C SUBROUTINES AND FUNCTION SUBPROGRAMS NEEDED: NONE

C METHOD:

C DESCRIBED IN APPENDIX IV OF WRITEUP

C*****

C SUBROUTINE CLOPRD(P,T,PHI,DEL,PSI,ENTHLP,CSUBP,CSUBT,RHO,
C 1 DRHODT,DRHODP,IER,MBAR)

C

C LOGICAL RICH,LEAN
C DIMENSION A(6,6,2),X(6)
C DIMENSION A1(36),A2(36)

```

EQUIVALENC (A1(1),A(1,1,1)),(A2(1),A(1,1,2))
REAL*4 MRAR,K

```

C
C
C
C

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INITIALIZE PARAMETERS, AND CHECK TO SEE IN WHAT TEMPERATURE
RANGE WE ARE SO THAT THE CORRECT FITTED COEFFICIENTS WILL BE
USED. FLAG TEMPERATURES TOO BIG OR TOO SMALL

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DATA A1/11.94033,2.088581,-0.47029,.037363,-.589447,-97.1418,
1 4.139094,4.60783,-.9356009,.06669498,.0335801,-56.62588,
2 7.099556,1.275957,-.2877457,.022355,-.1598696,-27.73464,
3 5.555680,1.787191,-.2881342,.01951547,.1611828,.76498,
4 7.865847,.6883719,-.031944,-.00268708,-.2013873,-.893455,
5 6.807771,1.453404,-.328985,.02561035,-.1199462,-.331835/
DATA A2/4.737305,16.65283,-11.23249,2.828001,.00676702,-93.75793,
7 7.809672,-.2023519,.3418708,-1.179013,.00143629,-57.08004,
8 6.97393,-.8238319,2.942042,-1.176239,.0004132409,-27.19597,
9 6.991878,.1617044,-.2182071,.2968197,-.01625234,-.118189,
6 6.295715,2.388387,-.0314788,-.3267433,.00435925,.103637,
- 7.092199,-1.295825,3.20688,-1.202212,-.0003457938,-.013967/

```

C

```

RICH = PHI .GT. 1.0
LEAN = .NOT. RICH
EPS = 4.*DFL/(1. + 4.*DFL)
IFR = 0
IF (T .LT. 100.) IFR = 1
IF (T .GT. 6000.) IFR = 2
IR = 1
IF (T .LT. 500.) IR = 2

```

C
C
C

```

GET THE COMPOSITION IN MOLES/MOLE OXYGEN

```

```

IF (RICH) GO TO 10
Y(1) = EPS*PHI
X(2) = 2.*(1.- EPS)*PHI
X(3) = 0.
X(4) = 0.
X(5) = 1.- PHI
GO TO 20
10 Z = 1000./T
K = EXP(2.743 + 7*(-1.761 + Z*(-1.611 + 7*.2803)))
ALPHA = 1. - K
BETA = (2.*(1.- EPS*PHI) + K*(2.*(PHI - 1.) + EPS*PHI))
GAMMA = 2.*K*EPS*PHI*(PHI - 1.)
C = ( - BETA + SQRT(BETA*BETA + 4.*ALPHA*GAMMA))/(2.*ALPHA)
X(1) = EPS*PHI - C
X(2) = 2.*(1. - EPS*PHI) + C
X(3) = C
X(4) = 2.*(PHI - 1.) - C
X(5) = 0.
20 X(6) = PSI

```

C
C
C
C

```

CONVERT COMPOSITION TO MOLE FRACTIONS AND CALCULATE AVERAGE
MOLECULAR WEIGHT

```

```

IF (LEAN) TMOLES = 1. + PSI + PHI*(1.-EPS)
IF (RICH) TMOLES = PSI + PHI*(2.-EPS)
DO 30 J = 1,6
30 X(J) = X(J)/TMOLES
MRAR = ((A.*EPS + 4.)*PHI + 32. + 2A.*PSI)/TMOLES

```

C

C CALCULATE H, CP, AND CT AS IN WRITEUP. USING FITTED
C COEFFICIENTS FROM JANAF TABLES
C

```

ENTHLP = 0.
CSURP = 0.
CSURT = 0.
ST = T/1000.
DO 40 J = 1,6
  TH = ((( A(4,J,IR)/4.*ST + A(3,J,IR)/3. ) *ST
1      + A(2,J,IR)/2. ) *ST + A(1,J,IR) ) *ST
  TCP = (( A(4,J,IR)*ST + A(3,J,IR) ) *ST
1      + A(2,J,IR) ) *ST + A(1,J,IR)
  TH = TH - A(5,J,IR)/ST + A(6,J,IR)
  TCP = TCP + A(5,J,IR)/ST**2
  ENTHLP = ENTHLP + TH*X(J)
40  CSURP = CSURP + TCP*X(J)
  ENTHLP = ENTHLP/MBAR
  CSURP = CSURP/MBAR

```

C
C NOW CALCULATE RHO AND ITS PARTIAL DERIVATIVES
C USING PERFECT GAS LAW
C

```

RHO = .012187*MBAR*P/T
DRHODT = -RHO/T
DRHODP = RHO/P

```

C
C ALL DONE
C RETURN
C END


```

SUBROUTINE DERIVS(P,T,PHI,EPS,PSI,A,X,Y,U,AMWT,CSURP,CSURT,
1  DRHONT,DRHONP)
LOGICAL RICH,LEAN
DATA ROVR2/.99345/
DATA SCALF/41.29287/

C
RICH = PHI .GE. 1.0
LEAN = .NOT. RICH

C
C3 = (117. + 30.*EPS)*1000.
C4 = 1.35E5*EPS
C5 = 2.0 - FPS + PSI
C6 = 5.0 - 2.*FPS + 2.*PSI

C
DUOTPX = 6.3E4*U/T**2
DUOTX = -U/P
DUOXPT = -U/(X*(1. - 2.*EPS*X))

C
DADTP = (3.4E4*2./3.)*A/T**2
DADPT = -A/(3.*P)

C
AP = EPS*A
T5 = 3.*C5
DXDA = T5*(T5 + 2.*C6*AP)/(T5*(1. + 2.*AP) + 2.*C6*AP**2)**2

C
Z = (1. - PHI)/X
IF (LEAN) DYDX = (1. + .72*Z)/(1. + .36*Z)**2
IF (RICH) DYDX = (1. - 1.28*Z + .90*Z**2)/(1. - .64*Z + .3*Z**2)**2

C
DYDTP = DYDX*DXDA*DADTP
DYDPT = DYDX*DXDA*DADPT
DUOTP = DUOXPT*DXDA*DADTP + DUOTPX
DUOPT = DUOXPT*DXDA*DADPT + DUOTX

C
DHFDPT = C3*DYDPT + C4*DUOPT
DC2DPT = -2.*(3.*DYDPT + DUOPT)
DC1DPT = 5.*DYDPT + 3.*DUOPT
DHFDTP = C3 * DYDTP + C4*DUOTP
DC2DTP = -2.*(3.*DYDTP + DUOTP)
DC1DTP = 5.*DYDTP + 3.*DUOTP

C
TV0 = (3000. - 2000.*FPS + 300.*PSI)/(1. - .5*EPS + .09*PSI)
FARG = EXP(TV0/T)
TV = TV0/(FARG - 1.)
DTVOTP = TV0*FARG/(T*(FARG - 1.))**2 *TV0

C
AMCP = (8.*EPS + 4.)*PHI + 32. + 28.*PSI
C1 = 7.*PSI + 5.*Y + 3.*J
C2 = 2.*(PSI - 3.*Y - U)
IF (LEAN) C1 = C1 + 7. + (9. - 8.*EPS)*PHI
IF (RICH) C1 = C1 + 2. + 2.*(7. - 4.*EPS)*PHI
IF (LEAN) C2 = C2 + 2.*(1. + (5. - 3.*FPS)*PHI)
IF (RICH) C2 = C2 + 2.*(4. + (2. - 3.*EPS)*PHI)

C
CSURP = ROVR2/AMCP*(C1 + T*DC1DTP + C2*DTVOTP + TV*DC2DTP
1  + DHFDTP)
CSURT = ROVR2/AMCP*(T*DC1DPT + TV*DC2DPT + DHFDPT)*SCALF

C
IF (LEAN) G = 1. + (1.-FPS)*PHI + PSI + Y + U
IF (RICH) G = (2.- FPS)*PHI + PSI + Y + U

```

```

      G = -AMCP/G**2
      DMOTP = G*(DYDTP + DUOTP)
      DMOPD = G*(DYOPD + DUOPD)
C
      DRHODT = .012187*P/T*(DMOTP - AMWT/T)
      DRHODP = .012187/T*(AMWT + P*DMOPD)
C
      RETURN
      END

```

SUBROUTINE INPOR

```

C
C INTAKE PORT CALCULATION
C THIS PROGRAM WAS ORIGINALLY MADE USING METER-KG UNIT
COMMON/EPROP/ TECHF(100),EFUEL(100),EANGL(100),EMWT(100),
1 DHFUEL(100),DHLOS(100),DIEMAS(100),DOEMAS(100),
1 ERGAS(100),ECP(100),FENTH(8,100),FMASS(8,100),FEQUI(8,100),
1 EVOL(8,100),FTEMP(8,100),PCYL(8)
COMMON/INFLO/ NINEF,XINEF(20),YINEF(20),AREIND,PINT,TINT,GINT,
1 EQUINT,AREINT,XINV
COMMON /STATE/ ANGLE1,ANGLE,JCOND,ASTEP,NSTEP,IE
COMMON /TIMIG/ AINTO,AEXTO,AINTC,AEXTC,AFUELS,AFUELE
COMMON /STAT1/ RPM,JLAST,NJET,PHIO,EGR

C
IF(PINT-PCYL(1)) 50,50,60

C
C INTAKE FLOW IS FROM CYLINDER TO PORT (BACK FLOW)
50 CINT=-1.
   RHIGH=ERGAS(1)*9.8
   PHIGH=PCYL(1)*10000.
   PRIN=PINT/PCYL(1)
   THIGH=FTEMP(1,1)
   AKHIGH=1.35
   GO TO 100

C
C INTAKE FLOW IS FROM PORT TO CYLINDER
C P VALUE DOESN'T CHANGE MUCH.
60 RINT=ERGAS(1)*9.8
   CINT=1.
   RHIGH=RINT
   PHIGH=PCYL(1)*10000.
   PRIN=PCYL(1)/PINT
   THIGH=TINT
   AKHIGH=1.35

C
C CALCULATE THE EFFECTIVE INTAKE FLOW AREA
100 ANAI=(ANGLE-AINTO)/(AINTC-AINTO)
   CALL TWODIM(NINEF,XINEF,YINEF,ANAI,AREFAC)
   AREINT=AREIND*AREFAC
   AREINT=AREINT/10000.

C
C NEXT EQUATION IS BASED ON METER-KG UNIT
GINT=
1 /((AKHIGH-1.)*(PRIN*(2./AKHIGH)-PRIN*((AKHIGH+1.)
2 /AKHIGH))))
GINT=PHIGH*AREINT/6./RPM*GINT
GINT=GINT*CINT
GINT=GINT*1000.
AREINT=AREINT*10000.
RETURN
END

```

SUBROUTINE UPROP

PURPOSE:

TO CALCULATE THE ENTHALPY AND DENSITY OF A HOMOGENEOUS MIXTURE
OF AIR, RESIDUAL GAS, AND FUEL AS A FUNCTION OF
EQUIVALENCE RATIO, TEMPERATURE, AND PRESSURE

USAGE:

CALL UPROP(P,T,PHI,DEL,PSI,RESFRK,ENTHLP,CSURP,CSURT,RHO,
DRHODT,DRHODP,CHI)

DESCRIPTION OF PARAMETERS:

GIVEN:

P - ABSOLUTE PRESSURE OF PRODUCTS (ATM)
T - TEMPERATURE OF PRODUCTS (DEG K)
RESFRK - RESIDUAL GAS FRACTION
PHI - EQUIVALENCE RATIO (FUEL/AIR RATIO DIVIDED BY THE
CHEMICALLY CORRECT FUEL/AIR RATIO)

GIVEN IN COMMON AREA /FUEL/:

AF(I) - 6 DIMENSIONAL VECTOR OF ENTHALPY COEFFICIENTS SUCH
THAT THE ENTHALPY OF FUEL VAPOR AS A FUNCTION
OF TEMPERATURE (T DEG K) IS GIVEN BY:

$$H(T) = AF(1)*ST + (AF(2)*ST**2)/2 + (AF(3)*ST**3)/3 \\ + (AF(4)*ST**4)/4 - AF(5)/ST + AF(6)$$

WHERE ST = T/1000 AND H(T) = <KCAL/MOLE>

FOR MOST APPLICATIONS THE ENTHALPY FUNCTION H(T) SHOULD
BE VALID OVER AT LEAST THE FOLLOWING TEMPERATURE RANGE:

$$300 < T < 1000$$

ENTHALPY DATUM STATE IS AT T = 0 ABSOLUTE WITH O₂, N₂,
AND H₂ GASEOUS AND C SOLID GRAPHITE.

ENW - AVERAGE NUMBER OF NITROGEN ATOMS PER FUEL MOLECULE
CX - AVERAGE NUMBER OF CARBON ATOMS PER FUEL MOLECULE
HY - AVERAGE NUMBER OF HYDROGEN ATOMS PER FUEL MOLECULE
OZ - AVERAGE NUMBER OF OXYGEN ATOMS PER FUEL MOLECULE
QLOWER - LOWER HEATING VALUE (KCAL/G)
XI - MOLAR N:O RATIO OF THE OXIDANT (FOR AIR XI = 3.76)

RETURNS:

DEL - MOLAR C:H RATIO OF THE PRODUCTS
PSI - MOLAR N:O RATIO OF THE PRODUCTS
CHI - EQUIVALENCE RATIO OF THE PRODUCTS FOR AN EQUIVALENT
HYDROCARBON-OXIDANT COMBUSTION
ENTHLP - SPECIFIC ENTHALPY OF THE PRODUCTS (KCAL/G)
CSURP - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO T
AT CONSTANT P (CAL/G-DEG K)
CSURT - PARTIAL DERIVATIVE OF ENTHLP WITH RESPECT TO P
AT CONSTANT T (CC/G)
RHO - DENSITY OF THE PRODUCTS (G/CC)
DRHODT - PARTIAL DERIVATIVE OF RHO WITH RESPECT TO T AT
CONSTANT P (G/CC-DEG K)
DRHODP - PARTIAL DERIVATIVE OF RHO WITH RESPECT TO P AT
CONSTANT T (G/CC-ATM)

RETURNS IN COMMON AREA CMPSTN:

X(1) - CARBON DIOXIDE MOLE FRACTION
X(2) - WATER VAPOR MOLE FRACTION
X(3) - CARBON MONOXIDE MOLE FRACTION
X(4) - HYDROGEN MOLE FRACTION
X(5) - OXYGEN MOLE FRACTION
X(6) - NITROGEN MOLE FRACTION
X(7) - FUEL MOLE FRACTION

UPRP 30
UPRP 40
UPRP 50
UPRP 60
UPRP 70
UPRP 80
UPRP 90
UPRP 100
UPRP 110
UPRP 120
UPRP 130
UPRP 140
UPRP 150
UPRP 160
UPRP 170
UPRP 180
UPRP 190
UPRP 200
UPRP 210
UPRP 220
UPRP 230
UPRP 240
UPRP 250
UPRP 260
UPRP 270
UPRP 280
UPRP 290
UPRP 300
UPRP 310
UPRP 320
UPRP 330
UPRP 340
UPRP 350
UPRP 360
UPRP 370
UPRP 380
UPRP 390
UPRP 400
UPRP 410
UPRP 420
UPRP 430
UPRP 440
UPRP 450
UPRP 460
UPRP 470
UPRP 480
UPRP 490
UPRP 500
UPRP 510
UPRP 520
UPRP 530
UPRP 540
UPRP 550
UPRP 560
UPRP 570
UPRP 580
UPRP 590
UPRP 600
UPRP 610
UPRP 620
UPRP 630

```

C      MBAR - MOLECULAR WEIGHT OF UNBURNED MIXTURE
C
C      REMARKS:
C      1) ENTHALPY DATUM STATE IS AT T = 0 ABSOLUTE WITH
C      02,N2,H2 GASFOUS AND C SOLID GRAPHITE
C      2) THIS IS A MODIFIED VERSION OF MIKE MARTIN'S SUBROUTINE
C      UPROP. IN CASE OF PROBLEMS CONTACT COLIN FERGUSON AT
C      253-5348 (ROOM 31-158)
C
C      SUBROUTINES AND FUNCTION SUBPROGRAMS NEEDED: NONE
C
C      METHOD:
C      DESCRIBED IN APPENDIX A OF HIRSH ET AL. SAE PAPER # 760161
C
C*****
C      SUBROUTINE UPROP(P,T,PHI,DEL,PSI,RESFRK,ENTHLP,CSURP,CSURT,RHO,
C      DRHODT,DRHODP,CHI,PAVG,CAVVG)
C      COMMON /FUEL/ AF(6),ENW,CX,HY,OZ,QLOWER
C      LOGICAL RICH,LEAN
C      DIMENSION A(6,7,2)
C      DIMENSION A1(42),A2(42),TABLE(7)
C      EQUIVALENCE (A(1),A(1,1,1)),(A2(1),A(1,1,2))
C      REAL*4 MBAR,K
C      COMMON /OXDANT/ XI /CMPSTN/ X(7),MBAR
C
C      INITIALIZE PARAMETERS, AND CHECK TO SEE IN WHAT TEMPERATURE
C      RANGE WE ARE SO THAT THE CORRECT FITTED COEFFICIENTS WILL BE
C      USED. FLAG TEMPERATURES TOO BIG OR TOO SMALL
C
C      DATA A1/11.94033,2.088581,-0.47029,.007363,-.589447,-97.1418,
1 6.139094,4.60783,-.9356009,6.669498E-02,.0335801,-56.62588,
2 7.099556,1.275957,-.2877457,.022355,-.1598696,-27.73464,
3 5.555680,1.787191,-.2891342,1.951547E-02,.1611829,.76498,
4 7.865847,.6883719,-.031944,-2.68708E-03,-.2013873,-.893455,
5 6.807771,1.453404,-.328985,2.561035E-02,-.1189462,-.331935,
6 6*0.0/
C      DATA A2/4.737305,16.65283,-11.23249,2.828001,6.76702E-03,-93.75793
7 7.809672,-.2023519,3.418708,-1.179013,1.43629E-03,-57.08004,
8 6.97393,-.8239319,2.942042,-1.176239,4.132409E-04,-27.19597,
9 6.991878,.1617044,-.2132071,.2968197,-1.525234E-02,-.118189,
1 6.295715,2.388387,-.0314788,-.3267433,4.35925E-03,.103637,
2 7.092199,-1.295825,3.20688,-1.202212,-3.457938E-04,-.013967,
3 6*0.0/
C      DATA TABLE /-1.,1.,1.,-1.,0.,0.,0./
C
C      ENTER INTO ARRAYS A1 AND A2 THE FUEL PARAMETERS
C
C      DO 5 I=1,6
C      A1(I + 36)=AF(I)
C      A2(I + 36)=AF(I)
C      RICH = PHI .GT. 1.0
C      LEAN = .NOT. RICH
C      W = ENW/CX
C      Z = OZ/CX
C      DEL = CX/HY
C      EPS = 4.*DEL/(1. + 4.*DEL - 2.*DEL*7)
C      IFR = 0
C      IF (T .LT. 100.) IFR = 1
C      IF (T .GT. 6000.) IFR = 2
C      IR = 1
C      IF (T .LT. 500.) IR = 2

```

GET THE COMPOSITION IN MOLES/MOLE OXYGEN OF OXIDANT

```

C      PCTRES = RESFRK
C      PCTNEW = 1.0 - RESFRK
C      IF (RICH) GO TO 10
X(1) = EPS*PHI*PCTRES
X(2) = (2.*(1. - EPS) + EPS*7)*PHI*PCTRES
X(3) = 0.
X(4) = 0.
X(5) = (1. - PHI)*PCTRES + PCTNEW
DCDT = 0.
GO TO 20
10 7T = 1000./T
K = EXP(2.743 + 7T*(-1.751 + 7T*(-1.511 + 7T*.2803)))
DKDT = -K*7T*(-1.751 + 7T*(-3.222 + 7T*.9409))/T
ALPHA = 1.0 - K
BETA = 2.*(1. - EPS*PHI) + K*(2.*(PHI - 1.) + EPS*PHI)
BETA = BETA + EPS*PHI*7
GAMMA = 2.*K*EPS*PHI*(PHI - 1.)
C = (-BETA + SQRT(BETA*BETA + 4.*ALPHA*GAMMA))/(2.*ALPHA)
DCDT = -DKDT*(C*C + (2.*(PHI - 1.) + EPS*PHI)*C - GAMMA/K)
DCDT = DCDT/(2.*ALPHA*C + BETA)
X(1) = (EPS*PHI - C)*PCTRES
X(2) = (2.0*(1. - EPS*PHI) + EPS*PHI*7 + C)*PCTRES
X(3) = C*PCTRES
X(4) = (2.0*(PHI - 1.) - C)*PCTRES
X(5) = PCTNEW
20 X(6) = XI + EPS*PHI*W/2.*PCTRES
X(7) = PCTNEW + EPS*PHI/CX

C      CONVERT COMPOSITION TO MOLE FRACTIONS AND CALCULATE AVERAGE
C      MOLECULAR WEIGHT
C
IF (LEAN) TMOLES = XI + (1. + EPS*PHI/CX)*PCTNEW
+ (1. + (1. - EPS)*PHI + EPS*PHI*(7 + W/2.))*PCTRES
IF (RICH) TMOLES = XI + (1. + EPS*PHI/CX)*PCTNEW
+ ((2. - EPS)*PHI + EPS*PHI*(7 + W/2.))*PCTRES
DO 30 J = 1,7
30 X(J) = X(J)/TMOLES
MBAR = EPS*PHI*(12. + 1./DEL + 16.*7 + 14.*W) + 32. + 28.*XI
MBAR = MBAR/TMOLES

C      CALCULATE H, CP, AND CT AS IN WRITEUP, USING FITTED
C      COEFFICIENTS FROM JANAF TABLES
C
FNTHLP = 0.
CSURP = 0.
CSURT = 0.
ST = T/1000.
DO 40 J = 1,7
TH = (((A(4,J,IR)/4.*ST + A(3,J,IR)/3.)*ST
1 + A(2,J,IR)/2.)*ST + A(1,J,IR))*ST
TCP = ((A(4,J,IR)*ST + A(3,J,IR))*ST
1 + A(2,J,IR))*ST + A(1,J,IR)
TH = TH - A(5,J,IR)/ST + A(6,J,IR)
TCP = TCP + A(5,J,IR)/ST**2
FNTHLP = FNTHLP + TH*X(J)
40 CSURP = CSURP + TCP*X(J) + 1000.*TH*DCDT*PCTRES*TABLE(J)
FNTHLP = FNTHLP/MBAR

```

UPRP1250
 UPRP1250
 UPRP1270
 UPRP1280
 UPRP1290
 UPRP1300
 UPRP1310
 UPRP1320
 UPRP1330
 UPRP1340
 UPRP1350
 UPRP1360
 UPRP1370
 UPRP1380
 UPRP1390
 UPRP1400
 UPRP1410
 UPRP1420
 UPRP1430
 UPRP1440
 UPRP1450
 UPRP1460
 UPRP1470
 UPRP1480
 UPRP1490
 UPRP1500
 UPRP1510
 UPRP1520
 UPRP1530
 UPRP1540
 UPRP1550
 UPRP1550
 UPRP1570
 UPRP1580
 UPRP1590
 UPRP1600
 UPRP1610
 UPRP1620
 UPRP1630
 UPRP1640
 UPRP1650
 UPRP1660
 UPRP1670
 UPRP1680
 UPRP1690
 UPRP1700
 UPRP1710
 UPRP1720
 UPRP1730
 UPRP1740
 UPRP1750
 UPRP1760
 UPRP1770
 UPRP1780
 UPRP1790
 UPRP1800
 UPRP1810
 UPRP1820
 UPRP1830
 UPRP1840

C	CSURP = CSURP/MRBP	UPRP1850
C		UPRP1860
C	NOW CALCULATE RHO AND ITS PARTIAL DERIVATIVES	UPRP1870
C	USING PERFECT GAS LAW	UPRP1880
C		UPRP1890
	RHO = .012187*MBAR*P/T	UPRP1900
	DRHODT = -RHO/T	UPRP1910
	DRHODP = RHO/P	UPRP1920
C		UPRP1930
C	CALCULATE PSI AND CHI FOR MIXED GASES	UPRP1940
C		UPRP1950
	PSI = (XI + EPS*PHI*W/2.)/(1. + EPS*Z*PHI/2.)	UPRP1960
	CHI = PHI*(1. + EPS*Z/2.)/(1. + EPS*Z*PHI/2.)	UPRP1970
C		
C		
	RAVG=82.057/MRBP	
	CVAVG=CSURP-1.98/MRBP	
C		UPRP1980
C	ALL DONE	UPRP1990
	RETURN	UPRP2000
	END	UPRP2010

SUBROUTINE EQIR(TTTT,PPPP,P-HIC,IFLAG,Z)

C

C VARIABLES LIST

C

REAL*8 DPPATM,DPTMP,DEQIB,XMOFR

DIMENSION DEQIB(4),XMOFR(14),YMOFR(14),Z(5)

C CALCULATE RATIOS OF H/C,N/C,O/C,AND C/C WHERE C=1.

TEMP=TTTT

PATM=PPPP

SLR=15.1

ERIURN=1./P-HIC

IF(TEMP.LT.1800.) GO TO 101

IFLAG=0

WHY=(12.*SLR-137.4)/(-SLR+.25*137.4)

XWHY=1.+.25*WHY

DEQIB(1)=WHY

DEQIB(2)=1.

DEQIB(4)=2.*XWHY*ERIURN

DEQIB(3)=3.764*DEQIB(4)

C

C CALCULATE N AND NO EQIB. AND EQIB. MOLEFRACTIONS

DPPATM=PATM

DPTMP=TEMP

CALL PTCHEM(DPTMP,DPPATM,DEQIB,XMOFR,ISENT)

DO 100 I=1,14

YMOFR(I)=XMOFR(I)

100 CONTINUE

GO TO 103

101 IFLAG=1

DO 102 J=1,14

102 YMOFR(J)=0.

103 Z(1)=YMOFR(2)

Z(2)=YMOFR(5)

Z(3)=YMOFR(8)

Z(4)=YMOFR(9)

Z(5)=YMOFR(14)

RETURN

END

SUBROUTINE DNODT(TTTT,PPPP,TOTMOL,ZMOFR,IFLAG,XNO,F)

```

C
C VARIABLE LIST
C
C
C      F          FINAL EVALUATION OF R.H.SIDE RATE EQUATION
C      W,X,Y,Z    DUMMY VARIABLES
C      VOL        VOLUME OF ELEMENT
C      XNO        AMOUNT OF NITRIC OXIDE
C      RC1F       RATE CONSTANT FOR FIRST REACTION, FORWARD
C      RC1R       RATE CONSTANT FOR FIRST REACTION, REVERSE
C      RC2F       RATE CONSTANT FOR SECOND REACTION, FORWARD
C      RC2R       RATE CONSTANT FOR SECOND REACTION, REVERSE
C      TEMP       TEMPERATURE OF ELEMENT
C      RTEMP      RECIPROCAL OF TEMP
C
      DIMENSION ZMOFR(5)
      TEMP=TTTT
      PATM=PPPP
      VOL=82.06*TEMP*TOTMOL/PATM
      IF(TEMP.LT.1800.) GO TO 2000
      IF(IFLAG.GT.0) GO TO 2000
      IF(TOTMOL.LE.0.0) GO TO 2000
C 4. COMPUTE RATE CONSTANTS (FUNCTIONS OF TEMPERATURE ONLY)
      RTEMP=1.9857*TEMP
      RC1F=7.6E+13*EXP(-75460./RTEMP)
      RC1R=1.6E+13
      RC2F=6.4E+09*EXP(-6255./RTEMP)*TEMP
      RC2R=1.5E+09*EXP(-38720./RTEMP)*TEMP
      RCOH=4.1E+13
C
      TMOLNO=ZMOFR(4)*TOTMOL
      TMOLN=ZMOFR(3)*TOTMOL
      XMOLCO=ZMOFR(1)
C 5. CALCULATE DNODT=F(VOL,TEMP,PATM,EBURN,ZMOFR,XNO)
      ZR=RC1R*ZMOFR(4)
      WR=RC2F*ZMOFR(5)+RCOH*ZMOFR(2)
      CAPL=ZR/WR
      ALPHA=XNO/TMOLNO
C
      TERM1=2.*RC1R*TMOLN*TMOLNO/VOL*(1.-ALPHA*ALPHA)
      TERM2=1.+ALPHA*CAPL
      F=TERM1/TERM2
C
      GO TO 3000
2000 F=0.
3000 CONTINUE
      RETURN
      END

```

```

C      SUBROUTINE PTCHFM ( TMP, PRS, D, XMOFR, ISENT )
C
C      THE ORIGINAL MIT EQUILIBRIUM PTCHFM SUBROUTINE HAS BEEN REDUCED
C      AND IS DESIGNED TO PROCESS 4 ELEMENTS & 14 SPECIES
C
C      ARRAY D CONTAINS RATIOS OF ELEMENTS H, C, N, O RESPECTIVELY:
C
C      E.G., DATA D / 1.43, 1.0, 13.0, 3.46 /
C
C      ARRAY XMOFR CONTAINS MOLE FRACTIONS OF EACH SPECIES:
C      SYMBOLS OF EACH SPECIES 1 TO 14 (HEX'IE') ARE AS FOLLOWS:
C
C      0      'HCO ' , 'CO ' , 'CO2 ' , 'H ' , 'OH ' , 'H2 ' ,
C      1      'H2O ' , 'N ' , 'NO ' , 'NO2 ' , 'N2 ' , 'N2O ' ,
C      2      'O ' , 'O2 ' /
C
C      INPUT:      ( DOUBLE PREC. )
C
C      TMP      = TEMPERATURE ( DEGREES K )
C      PRS      = PRESSURE ( ATMOSPHERES )
C      D        = ARRAY(4) ( RATIO, 4 ELEMENTS )
C
C      OUTPUT:     ( DOUBLE PREC. )
C
C      XMOFR = ARRAY(14) ( MOLE FRACTIONS, 14 SPECIES )
C      ISENT = ERROR CODE:
C      0 = NO ERROR
C      1 = TEMP TOO HIGH
C      2 = TEMP TOO LOW
C      3 = ( UNUSED )
C      4 = TOO MANY ITERATIONS, RESULTS DOUBTFUL, LOOK UP NU
C      5 = TOO MANY ITERATIONS
C      6 = THERE ARE NO GASES PRESENT
C      7 = CHECK IF THERE ARE ENOUGH SPECIES
C      8 = TOO MANY TRIES FOR T
C
C      AUTHOR:  DAN DANTZER      LATEST REVISION 12/14/72
C      ADAPTED FOR USE WITH HPCHEM BY TOM MIKUS: CURRENT TO 5/23/74
C
C      IMPLICIT REAL*8(A-H,O-Z)
C
C      EQUIVALENCE ( ITOTSP, M      )
C      EQUIVALENCE ( ITOTSP, M1     )
C      EQUIVALENCE ( NELEM , N      )
C      EQUIVALENCE ( G(1,1), CMV(1) )
C
C      DIMENSION J(1), XMOFR(1)
C      DIMENSION A(4,14), ZL(14,8)
C      DIMENSION ZL1(56), ZL2(56)
C      DIMENSION C2(2)
C      DIMENSION RTP(5)
C
C      FOLLOWING ARRAYS ARE 'NELEM' IN SIZE
C
C      DIMENSION JD(4), XMJ(4), XNJ(4), F(4), F(4,4)

```

```

00001370
00001380
00001390
00001400
00001410
00001420
00001430
00001440
00001450
00001460
00001470
00001480
00001490
00001500
00001510
00001520
00001530
00001540
00001550
00001560
00001570
00001580
00001590
00001600
00001610
00001620
00001630
00001640
00001650
00001660
00001670
00001680
00001690
00001700
00001710
00001720
00001730
00001740
00001750
00001760
00001770
00001780
00001790
00001800
00001810
00001820
00001830
00001840
00001850
00001860
00001870
00001880
00001890
00001900
00001910
00001920
00001930
00001940
00001950
00001960

```

```

C      FOLLOWING ARRAYS ARE 'NELEM' +2 = 'INXNSL'
C
C      DIMENSION R(6), G(6,6)
C
C      FOLLOWING ARRAYS ARE 'ITOTSP'
C
C      DIMENSION CMV(14), CP(14), CPT(14), X(14), XMAX(14)
C      DIMENSION HORT(14), SR(14), C(14)
C      DIMENSION XHORT(14)
C
C      COMMON / HORT / HORTSM,SMOHDOT,XMU,RTD,SUMNI
C
C      NSAME = INITIALIZATION FLAG
C      NFLEM = NO OF ELEMENTS INVOLVED
C      ITOTSP = TOTAL NR OF SPECIES INVOLVED
C
C      DATA NSAME / 0 /
C      DATA NELEM / 4 /
C      DATA INXNSL / 6 /
C      DATA ITOTSP / 14 /
C
C      DATA DD,XMU,E,F / 28*0.000 /
C      DATA R, G / 42 * 0.000 /
C      DATA A, CP, CPT, X, XMAX / 112 * 0.000 /
C      CMN IS NOT INITIALIZED WHEN IT LIES WITHIN ARRAY G
C
C      ARRAY ZL(K,J) CONTAINS THE HI-TEMP DATA FOR EACH OF 14 SPECIES
C
C      K = SPECIES NO ( 1 - 14 )
C      J = DATA ( 1 - 8 EACH SPECIES )
C
C      DATA WAS TAKEN FROM ORIGINAL DATA SET ( CARDS), ARRANGED IN
C      ROW,COL (14,8), BUT DATA STATEMENT INTERNALLY STORES
C      BY COL,ROW: THEREFORE, DATA MUST BE REVERSED FOR PROG EXEC.
C      ORIGINAL DATA ARRANGMENT MAINTAINED FOR CONVENIENCE IN MAKING
C      CHANGES TO SPECIES DATA.
C
C      NR OF CONTINUATION CARDS LIMITED TO 19
C      CONTINUATION COL #6 CONTAINS THE HEXIDECIMAL SPECIES NO
C
C      DATA ZL1 /
1  9.3434439D 00, 2.9512196D 00,-6.7088366D-01, 5.0901942D-02,
1 -4.1140777D-01,-6.9903498D 00, 6.2395554D 01, 2.3009987D 00,
2  7.0995646D 00, 1.2759552D 00,-2.8774744D-01, 2.2356123D-02,
2 -1.5986955D-01,-2.9023636D 01, 5.4823700D 01, 1.2890015D 00,
3  1.1940331D 01, 2.0885811D 00,-4.7029203D-01, 3.7363116D-02,
3 -5.8944768D-01,-9.9468796D 01, 6.2207169D 01, 2.3269949D 00,
4  4.9679995D 00,-5.9678716D-13, 1.9345219D-13,-1.8732195D-14,
4 -7.4194936D-14, 5.0619217D 01, 3.3404419D 01, 1.0119925D 00,
5  5.6197815D 00, 1.9668446D 00,-3.8645178D-01, 2.7364515D-02,
5  1.3418680D-01, 8.0923529D 00, 5.0777405D 01, 2.0489998D 00,
6  5.5556803D 00, 1.7971914D 00,-2.8813416D-01, 1.9515470D-02,
6  1.6118270D-01,-1.2590199D 00, 3.8126053D 01, 2.0239983D 00,
7  6.1390944D 00, 4.6078291D 00,-9.3560094D-01, 6.6694975D-02,
7  3.3580098D-02,-5.9687856D 01, 5.1456772D 01, 3.0619965D 00 /
C      DATA ZL2 /
8  5.1632023D 00,-1.8977487D-01, 3.6921006D-02, 3.6241105D-03,
8 -3.2718156D-02, 1.1134157D 02, 4.2733066D 01, 1.0359793D 00,
9  7.5180626D 00, 1.0245209D 00,-2.3053735D-01, 1.7926671D-02,
9 -1.9369543D-01, 1.8756821D 01, 5.8378296D 01, 2.0729971D 00,

```

```

A 1.21232820 01, 1.25649930 00, -3.01122960-01, 2.36587490-02, 00002570
A -6.22562890-01, 2.38395980 00, 6.88109590 01, 3.11099820 00, 00002590
R 6.80776990 00, 1.45340350 00, -3.28985750-01, 2.56103460-02, 00002590
R -1.18946190-01, -2.40383530 00, 5.31551610 01, 2.07199860 00, 00002600
C 1.23659610 01, 1.72617820 00, -4.05288460-01, 3.14184350-02, 00002610
C -5.81208770-01, 1.41054700 01, 6.43314670 01, 3.10999970 00, 00002620
D 5.10063090 00, -1.51772200-01, 4.89531380-02, -2.88143520-03, 00002630
D 8.92994180-03, 5.80809480 01, 4.47525480 01, 1.03799440 00, 00002640
E 7.86584570 00, 6.88371900-01, -3.19441000-02, -2.68708170-03, 00002650
F -2.01387290-01, -2.96845440 00, 5.74246370 01, 2.07499890 00 / 00002660

```

C
C
C

```

IF(NSAME)2000,2000,2004
2000 NSAME=1

```

```

AP=1.9872600

```

```

ITMAX = 500

```

```

ITW = 400

```

```

DIF = 15.000

```

```

DIF1 = DIF

```

```

T = 1.000

```

```

TLUR = 6000.

```

```

XN=N

```

```

TOL1 = .0100

```

```

TOL3 = .0000100

```

```

TOL5 = 1.00-5

```

```

TOL6 = .100

```

```

TOL7 = 10.000

```

C
C
C
C
C
C

```

ARRAY A(I,K) CONTAINS NR OF ATOMS PER ELEMENT ( IN SPECIES )

```

```

I = ELEMENTS H, C, N, O RESPECTIVELY

```

```

K = SPECIES NR

```

```

A(1,1) = 1.

```

```

A(1,4) = 1.

```

```

A(1,5) = 1.

```

```

A(1,6) = 2.

```

```

A(1,7) = 2.

```

```

A(2,1) = 1.

```

```

A(2,2) = 1.

```

```

A(2,3) = 1.

```

```

A(3,8) = 1.

```

```

A(3,9) = 1.

```

```

A(3,10) = 1.

```

```

A(3,11) = 2.

```

```

A(3,12) = 2.

```

```

A(4,1) = 1.

```

```

A(4,2) = 1.

```

```

A(4,3) = 2.

```

```

A(4,5) = 1.

```

```

A(4,7) = 1.

```

```

A(4,9) = 1.

```

```

A(4,10) = 2.

```

```

A(4,12) = 1.

```

```

A(4,13) = 1.

```

```

A(4,14) = 2.

```

C
C
C

```

LOAD DATA INTO SPECIES ARRAY 7L

```

```

00002570
00002590
00002590
00002600
00002610
00002620
00002630
00002640
00002650
00002660
00002670
00002680
00002690
00002700
00002710
00002720
00002730
00002740
00002750
00002760
00002770
00002780
00002790
00002800
00002810
00002820
00002830
00002840
00002850
00002860
00002870
00002880
00002890
00002900
00002910
00002920
00002930
00002940
00002950
00002960
00002970
00002980
00002990
00003000
00003010
00003020
00003030
00003040
00003050
00003060
00003070
00003080
00003090
00003100
00003110
00003120
00003130
00003140
00003150
00003160

```

```

      II = 0
      DO 1050 K = 1,7
      I = K + 7
      DO 1050 J = 1, 8
      II = II + 1
      ZL(K,J) = 7L1(II)
1050  7L(I,J) = 7L2(II)
      DO 3010 I = 1,N
      XMU(I) = 0.0
3010  CONTINUE
C
C
C      END OF ONE-TIME INITIALIZATION
C
2004  IF ( TMP - 200.0 ) 2112, 2112, 2355
2355  CONTINUE
      IF ( TMP - TLUR ) 2012, 2012, 2009
2009  ISENT=1
      GO TO 5000
2112  ISENT=2
      GO TO 5000
2012  CONTINUE
      TK = TMP / 1.00+3
      XLP = DLOG ( PRS )
C
C      START OF ORIGINAL 'HS' SUBROUTINE
C
      DO 5004 K10=1, M
      IF ( 7L(K10,1) ) 5003, 5002, 5003
5002  HORT(K10) = 0.1111111100
      SR (K10) = -1.006
      GO TO 5004
5003  HORT(K10) = ((( ( ZL(K10,4) * TK / 4.00 + ZL(K10,3) / 3.000 ) *
1      TK + ZL(K10,2) / 2.00 ) * TK + 7L(K10,1) ) * TK -
2      ZL(K10,5) / TK + 7L(K10,6) ) / ( 42 * TK )
      SR(K10) = ( ZL(K10,1) * DLOG(TK) + TK * ( 7L(K10,2) +
1      7L(K10,3) * 0.500 * TK + 7L(K10,4) * TK **2 / 3.00 ) -
2      ZL(K10,5) * 0.500 / TK ** 2 + 7L(K10,7) ) / 42
5004  C(K10) = HORT(K10) - SR(K10) + XLP
C
C      END OF ORIGINAL 'HS' SUBROUTINE
C
      ISENT=0
      ITER=0
      ITTPDG=0
      TOL4 = 0.170
      YMAX = 0.
      DO 412 J=1,M1
      XMAX(J) = 1.0010
      DO 412 I=1,N
      IF (A(I,J)) 412,412,413
413  IF (D(I)/A(I,J) -XMAX(J)) 414,412,412
414  XMAX(J)= D(I)/A(I,J)
412  CONTINUE
      X0=0.000
      DO 90 I=1,N
90  X0=X0+D(I)
      AVD = X0 / XN
      Y0=0.000
      DO 93 J=1,M

```

```

00003170
00003180
00003190
00003200
00003210
00003220
00003230
00003240
00003250
00003260
00003270
00003280
00003290
00003300
00003310
00003320
00003330
00003340
00003350
00003360
00003370
00003380
00003390
00003400
00003410
00003420
00003430
00003440
00003450
00003460
00003470
00003480
00003490
00003500
00003510
00003520
00003530
00003540
00003550
00003560
00003570
00003580
00003590
00003600
00003610
00003620
00003630
00003640
00003650
00003660
00003670
00003680
00003690
00003700
00003710
00003720
00003730
00003740
00003750
00003760

```

```

93      Y0=Y0+ XMAX(J)                                00003770
      X0= DMIN1(X0,Y0)                                00003780
      X0=X0*1.0500                                    00003790
      DO 825 J=1,M1                                    00003800
825      XMAX(J)=XMAX(J)*1.0500                        00003810
C                                              00003820
C      CAUTION*** ASSUMPTION: THAT EACH ELEMENT MOLE RATIO DIVIDED BY 00003830
C      THE SUM OF THE RATIOS WILL BE GREATER THAN 0.01: 00003840
C      IF = OR < 0.01. THEN MUST USE FOLLOWING ROUTINE: 00003850
C      I.E., REMOVE THE 'C' COMMENT FROM COL 1 FROM HERE TO LABEL 530 & 00003860
C      FROM LABEL 503 TO 475 00003870
C      NOTE: ARRAY K2 IS DIMENSIONED (2) 00003880
C                                              00003890
C      SUM IS NOT DEFINED IN ORIGINAL PROGRAM 00003900
      SUM = 0.0 00003910
      DO 525 I = 1,N 00003920
525      SUM = SUM + D(I) 00003930
C                                              00003940
C      L1=0 00003950
      NG05=1 00003960
      RATIO = .0100 00003970
      DO 526 I=1,N 00003980
      IF (D(I)/SUM - RATIO) 527,527,526 00003990
527      L1=L1+1 00004000
      K2(L1) =I 00004010
526      CONTINUE 00004020
      NL= L1 00004030
      IF (NL) 528,528,529 00004040
528      NG05 =1 00004050
      GO TO 530 00004060
529      NG05=2 00004070
530      CONTINUE 00004080
C                                              00004090
C                                              00004100
C      ITER4=0 00004110
      NG06=1 00004120
      RH2=1.000 00004130
C                                              00004140
C      END OF ENTRY INITIALIZATION & CHECKING OF TEMPERATURE 00004150
C                                              00004160
C      BEGINNING OF MAIN PROGRAM LOOP 00004170
C                                              00004180
C      NG0=1 00004190
      ITER2=0 00004200
      IF (ITER - 1) 473,473,474 00004210
474      RH2=DSORT(H2) 00004220
      RH2=DMIN1(RH2,1.000) 00004230
473      NG01=1 00004240
      DO 101 J=1,M1 00004250
      SUM= C(J) 00004260
      DO 1002 I=1,N 00004270
1002      SUM=SUM+ XMU(I)*A(I,J) 00004280
101      CP(J)= SUM 00004290
      DO 1012 J=1,M1 00004300
1012      CPT(J)= CP(J) 00004310
      DO 1001 I=1,N 00004320
1001      D(I)= D(I) 00004330
      L1= 0 00004340
      SUMEX=0.000 00004350
      DO 102 J=1,M 00004360

```

	J1=J	00004370
	IF (CPT(J)+ 30.000) 420,420, 421	00004380
421	XJ=DEXP(-CPT(J))	00004390
	SUMFX=SUMFX+XJ	00004400
102	X(J)=XJ	00004410
	IF (SUMFX-1.000-TOL1*R+2) 103,103,107	00004420
103	IF (SUMFX-1.000+TOL1*R+2) 112,104,104	00004430
104	L1=1	00004440
	DO 106 I=1,N	00004450
	SUM=0.0	00004460
	DO 105 J=1,M	00004470
105	SUM=SUM+ A(I,J)*X(J)	00004480
106	F(I,1) = SUM	00004490
	YMAX = X0	00004500
	GO TO 123	00004510
420	CPT1 = CPT(J1)	00004520
	DO 423 J=1,M	00004530
	J1= J	00004540
	CPT2 = CPT(J)-CPT1	00004550
	IF (CPT2 +30.000) 420,420,422	00004560
422	X(J) =DEXP(-CPT2)	00004570
423	CONTINUE	00004580
107	SUM=0.000	00004590
	DO 416 J=1,M	00004600
416	SUM= SUM+ X(J)	00004610
	SUM= X0/SUM	00004620
	DO 108 J= 1,M	00004630
108	X(J)=X(J)*SUM	00004640
	DO 109 I=1,N	00004650
	SUM= 00(I)	00004660
	DO 110 J=1,M	00004670
110	SUM = SUM -A(I,J)*X(J)	00004680
109	00(I)= SUM	00004690
	GO TO 123	00004700
112	DO 113 J=1,M	00004710
113	X(J)= 0.000	00004720
123	L=L1	00004730
C		00004740
C	L = 0 OR 1 ONLY	00004750
C		00004760
	IF (L) 131,131, 200	00004770
131	DO 132 I=1,N	00004780
132	XNU(I)=-00(I)	00004790
	GO TO 23	00004800
430	DO 431 J=1,M1	00004810
	CMN(J)= 0.000	00004820
	DO 431 I=1,N	00004830
431	CMN(J)=CMN(J)+XNU(I)*A(I,J)	00004840
	COMP=TOL5*TOL5/H2	00004850
	XNU0=0.000	00004860
	DO 432 I=1,N	00004870
432	XNU0= XNU0+ XNU(I)*0(I)	00004880
446	H= -XNU0	00004890
	ITTRDG=ITTRDG+1	00004900
	IF (ITTRDG-5000) 2358,2358,2356	00004910
2356	ISENT = 8	00004920
	GO TO 5000	00004930
2358	CONTINUE	00004940
	DO 433 J=1,M1	00004950
433	CPT(J)= CP(J)+ I*CMN(J)	00004960

```

      EXMIN= 1.0010
      DO 510 I=1,M
        IF (CPT(J) - EXMIN) 511,510,510
511 CONTINUE
        EXMIN= CPT(J)
510 CONTINUE
        SUMEX =0.000
        DO 513 J=1,M
          IF(CPT(J)-EXMIN-DIF1) 517,517,516
516 X(J)= 0.000
          GO TO 513
517 X(J) =DEXP(EXMIN -CPT(J))
          SUMEX =SUMEX +X(J)
513 CONTINUE
          IF (EXMIN) 521,521 , 519
519 IF(SUMEX*DEXP(-EXMIN)-1.000) 443,521,521
521 PRON = X0 /SUMEX
          DO 522 J=1,M
522 H= H+ PRON* X(J)*CMN(J)
443 CONTINUE
          IF (H) 458,458,457
457 T0=T
          H0= H
          GO TO (448,459) , 'GO
448 T= T+T
          IF (T - 1.0015 ) 446, 446, 908
908 ISFNT = 7
          GO TO 5000
458 T1=T
          NG0=2
459 IF(DABS(H/H2)-TOL3) 453,453,460
460 IF ((T1-T0)**2-COMP) 453,453,452
452 T=0.500*(T0+T1)
          GO TO 446
453 DO 454 I=1,N
454 XMU(I) = XMU(I) + T* XNU(I)
          GO TO 99
C
C L = 1 AT THIS POINT
C
200 SDUM = 0.000
      SUM = 0.000
      DO 2 I = 1, N
        SDUM = SDUM + F(I,1) * F(I,1)
        SUM = SUM + F(I,1) * D0(I)
        E(1) = SUM / SDUM
        G(1,1) = 0.000
        Y1 = 0.000
        Z1 = 0.000
71 SUM = E(1) + G(1,1) * Z1
        IF ( SUM )10, 10, 11
10 Z1 = 0.000
        GO TO 8
11 IF ( SUM - YMAX ) 471, 471, 472
472 Z1 = YMAX
        GO TO 8
471 Z1 = SUM
9 IF ( DABS( Z1 - Y1 ) - TOL3 ) 15, 15, 13
13 Y1 = Z1
        GO TO 71

```

```

00004970
00004980
00004990
00005000
00005010
00005020
00005030
00005040
00005050
00005060
00005070
00005080
00005090
00005100
00005110
00005120
00005130
00005140
00005150
00005160
00005170
00005180
00005190
00005200
00005210
00005220
00005230
00005240
00005250
00005260
00005270
00005280
00005290
00005300
00005310
00005320
00005330
00005340
00005350
00005360
00005370
00005380
00005390
00005400
00005410
00005420
00005430
00005440
00005450
00005460
00005470
00005480
00005490
00005500
00005510
00005520
00005530
00005540
00005550
00005560

```


15	DO 16 I = 1, N	00005570
16	XNU(I) = -XN(I) + F(I,1) * Z1	00005580
	DO 19 J = 1, M	00005590
19	X(J) = X(J) * 71	00005600
C		00005610
C	L = 0 OR 1 BELOW THIS POINT	00005620
C		00005630
23	DO 24 I=1,N	00005640
	IF(DARS(XNU(I)) - TOL4 * AVD) 24,24,25	00005650
24	CONTINUE	00005660
	NG01=2	00005670
	GO TO 330	00005680
25	GO TO (550,551), NG06	00005690
551	ITER4=ITER4+1	00005700
	IF (L) 550,550,814	00005710
814	IF (ITER4-20) 550,552,552	00005720
552	ITER4=0	00005730
	NG01=2	00005740
	GO TO 330	00005750
550	H0=0.000	00005760
	DO 26 I=1,N	00005770
26	H0=H0+XNU(I)**2	00005780
	H2= H0	00005790
	T0=0.000	00005800
	T=1.000	00005810
	GO TO 330	00005820
C		00005830
C	SEE COMMENTS ABOVE (LABEL 527)	00005840
C		00005850
503	CONTINUE	00005860
C		00005870
	GO TO (475,476),NG05	00005880
475	K = ITER - (ITER / N) * N	00005890
	IF (K) 531,532,531	00005900
532	K=N	00005910
531	DO 540 L1=1,NL	00005920
	IF(K2(L1)-K) 540,541,540	00005930
540	CONTINUE	00005940
	GO TO 475	00005950
541	IF(DARS(XNU(K))-TOL5*XN(K)) 475,475,542	00005960
542	IF(DARS(XNU(K))-1.0-15) 475,475,8000	00005970
8000	SUM=XNU(K)	00005980
	DO 543 I=1,N	00005990
543	XNU(I)=0.000	00006000
	XNU(K)=SUM	00006010
	H0=SUM*SUM	00006020
	DIF1=100.000	00006030
	H2=H0	00006040
	T0=0.000	00006050
	T=1.000	00006060
	GO TO 430	00006070
475	DIF1=DIF	00006080
C		00006090
	GO TO 430	00006100
330	ITER= ITER+1	00006110
	IF (ITER - ITW) 333,670,670	00006120
670	ISFNT = 4	00006130
	GO TO 5079	00006140
C		00006150
333	GO TO (503,500), NG01	00006160

C		00006170
500	NTOT=N+1	00006180
	DO 820 I=1,N	00006190
820	DD(I)=XMU(I)	00006200
	DO 821 J=1,M	00006210
821	CPT(J)=X(J)	00006220
	IF (L) 727,727,502	00006230
502	XBAR=Z1	00006240
	ITER2 = 1	00006250
750	IF (XBAR) 727, 727, 701	00006260
701	G(N+1,N+1)= 0.000	00006270
	DO 704 K=1,M	00006280
	SUM=- C(K)	00006290
	DO 705 I=1,N	00006300
705	SUM=SUM-XMU(I)*A(I,K)	00006310
	IF (SUM -30.000)425,727, 727	00006320
425	X(K) = XBAR*DEXP(SUM)	00006330
704	CONTINUE	00006340
	DO 706 I=1,N	00006350
	SUM=0.000	00006360
	DO 707 K=1,M	00006370
707	SUM=SUM +A(I,K)*X(K)	00006380
	SUM=SUM/XBAR	00006390
	G(I,N+1) =SUM	00006400
	G(N+1,I) =SUM	00006410
	R(I) = D(I)-SUM*XBAR	00006420
	DO 706 J=1,N	00006430
	SUM= 0.000	00006440
	DO 709 K=1,M	00006450
709	SUM=SUM - A(I,K)*A(J,K)*X(K)	00006460
706	G(I,J)=SUM	00006470
	SUM=-XBAR	00006480
	DO 710 K=1,M	00006490
710	SUM=SUM+X(K)	00006500
	R(N+1) =SUM/XBAR	00006510
	DO 728 I=1,N	00006520
	IF(DABS(R(I)) - TOL6*AVD) 728,728,727	00006530
728	CONTINUE	00006540
	GO TO 730	00006550
727	DO 903 I=1,N	00006560
	IF(DABS(XN(I))-TOL5*D(I)) 903,903,801	00006570
903	CONTINUE	00006580
	DO 822 I=1,N	00006590
822	XMU(I)=DD(I)	00006600
	DO 823 J=1,M	00006610
823	X(J)=CPT(J)	00006620
	GO TO 5079	00006630
801	TOL4=0.100*TOL4	00006640
	NG06=2	00006650
	H2=1.000	00006660
	GO TO 99	00006670
730	IPP=NXNSOL(INXNSL,NTOT,G,R)	00006680
	IF(IPP-2)8001,727,8001	00006690
8001	ITER2=ITER2+1	00006700
	DO 465 I=1,N	00006710
	IF(DABS(R(I)) -TOL7) 465,465,727	00006720
465	CONTINUE	00006730
	DO 731 I=1,NTOT	00006740
	IF(DABS(R(I)) - TOL5) 731, 731, 739	00006750
731	CONTINUE	00006760

```

GO TO 737
733 DO 734 I=1,N
734 XMU(I)=XMU(I)+R(I)
      XBAR=XBAR+R(N+1)
GO TO 750
739 CONTINUE
      IF (IT=RT-ITMAX) 733,740,740
740 ISENT=5
      GO TO 5000
C
C      TEST IF X(J) NEGATIVE
C
737 DO 470 J=1,M
      IF (X(J)) 801,470,470
470 CONTINUE
C
C      END OF MAIN PROGRAM LOOP
C
5079 SUMNI=0.000
      DO 5010 I=1,M
      SUMNI=SUMNI+X(I)
5010 CONTINUE
      IF (SUMNI) 751,752,751
752 ISENT=6
      GO TO 5000
751 CONTINUE
      DO 5011 I=1,M
5011 XMOFR(I)=X(I)/SUMNI
C
C      NOTE: ROUTINE TO CHECK FOR A SINGULAR DERIVATIVE MATRIX
C      IN RTP & RDP ARRAYS HAS BEEN REMOVED.
C
C      ADDITIONAL CALCULATIONS REQUIRED BY HPCHEM:
C
      NP11=N+1
      DO 6000 I=1,N
      DO 6000 J=1,N
      G(I,J)=0.000
      DO 6000 K=1,M
      G(I,J)=G(I,J)-A(I,K)*A(J,K)*X(K)
6000 CONTINUE
      DO 6001 I=1,N
      G(I,NP11)=0.000
      G(NP11,I)=0.000
      DO 6002 K=1,M
      G(I,NP11)=G(I,NP11)+A(I,K)*X(K)
      G(NP11,I)=G(NP11,I)+A(I,K)*X(K)
6002 CONTINUE
      G(I,NP11)=G(I,NP11)/XBAR
      G(NP11,I)=G(NP11,I)/XBAR
6001 CONTINUE
      G(NP11,NP11)=0.0
      XBAR=SUMNI
      YHPRIM=0.0
      HORTSM=0.0
      DO 6010 I=1,N
      RTP(I)=0.0
6010 CONTINUE
      DO 6030 K=1,M
      YHPRIM=XHPRIM+X(K)*((ZL(K,4)*TK+ZL(K,3))*TK+ZL(K,2))

```

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00006770
00006780
00006790
00006800
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00006820
00006830
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00006990
00007000
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00007080
00007090
00007100
00007110
00007120
00007130
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00007150
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00007180
00007190
00007200
00007210
00007220
00007230
00007240
00007250
00007260
00007270
00007275
00007280
00007290
00007300
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00007330
00007340
00007350

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```

1      * TK + ZL(K,1) + ZL(K,5)/(TK*TK) ) 00007360
      XHORT(K) = X(K) * HORT(K) 00007370
      HORTSM = HORTSM + XHORT(K) 00007380
      DO 6020 I = 1,N 00007390
      RTP(I) = RTP(I) - A(I,K) * XHORT(K) 00007400
6020  CONTINUE 00007410
6030  CONTINUE 00007420
      RTP(NP11) = HORTSM / YBAR 00007430
      NPL = N + L 00007440
      DO 6040 I = 1,NPL 00007450
      RTP(I) = RTP(I) / TMP 00007460
6040  CONTINUE 00007470
      IPP = NXNSOL(INXNSL,NPL,3,RTP) 00007510
      CSURP = 0.0 00007540
      DO 6060 K = 1,M 00007550
      RTPA = 0.0 00007560
      DO 6050 I = 1,N 00007570
      RTPA = RTPA + RTP(I) * A(I,K) 00007580
6050  CONTINUE 00007590
      CSURP = CSURP + (HORT(K)/TMP - RTPA)*XHORT(K) 00007600
6060  CONTINUE 00007610
      SMDHDT = XHPRIM + AR*TMP*(CSURP + RTP(NP11)*HORTSM/SUMNI) 00007620
C 00007630
      RETURN 00007640
C 00007650
C 00007660
C 00007670
C 00007680
5000 DO 5100 I = 1, ITOTSP 00007690
5100 XMOFR(I) = 0. 00007700
      RETURN 00007710
      END

```

FUNCTION	NYNSOL(IM,IN,A,B)	
CNXNSOL		00007720
IMPLICIT REAL*8(A-H,O-Z)		00007730
DIMENSION A(2),B(2)		00007740
INTEGER XROW		00007750
XROW(K000FX,K001FX)=K001FX*M-M*K000FX		00007760
M=IM		00007770
N=IN		00007780
N1=N-1		00007790
DO 44 J=1,N1		00007800
K=J		00007810
J1=J+1		00007820
JJ=XROW(J,J)		00007830
WS1=DABS(A(JJ))		00007840
C LOOP TO FIND LARGEST		00007850
DO 11 L=J1,N		00007860
LJ=XROW(L,J)		00007870
WWS1=DABS(A(LJ))		00007880
IF (WS1-WWS1) 12,11,11		00007890
12 WS1=WWS1		00007900
K=L		00007910
11 CONTINUE		00007920
IF (J-K) 13,31,31		00007930
C \$ IF DIAG NOT LARGEST INTERCHANGE ROWS		00007940
13 DO 26 L=1,N		00007950
JL=XROW(J,L)		00007960
KL=XROW(K,L)		00007970
WS1=A(JL)		00007980
A(JL)=A(KL)		00007990
26 A(KL)=WS1		00008000
WS1=B(J)		00008010
B(J)=B(K)		00008020
B(K)=WS1		00008030
31 DO 33 L=J1,N		00008040
JL=XROW(J,L)		00008050
IF (A(JJ)) 33,54,33		00008060
33 A(JL)=A(JL)/A(JJ)		00008070
B(J)=B(J)/A(JJ)		00008080
DO 43 L=1,N		00008090
IF (L-J) 37,43,37		00008100
37 LJ=XROW(L,J)		00008110
38 DO 41 L2=J1,N		00008120
LL2=XROW(L,L2)		00008130
JL2=XROW(J,L2)		00008140
41 A(LL2)=A(LL2)-A(LJ)*A(JL2)		00008150
B(L)=B(L)-A(LJ)*B(J)		00008160
43 CONTINUE		00008170
44 CONTINUE		00008180
C LAST COLUMN HAS NOT BEEN DONE YET		00008190
NN=XROW(N,N)		00008200
IF (A(NN)) 46,54,46		00008210
46 B(N)=B(N)/A(NN)		00008220
DO 50 L=1,N1		00008230
LN=XROW(L,N)		00008240
50 B(L)=B(L)-A(LN)*B(N)		00008250
NYNSOL=1		00008260
RETURN		00008270
54 NYNSOL=2		00008280
RETURN		00008290
END		00008300
		00008310

```

-----C20049.DAT  BIN #28 JUL. 28 1977-----
9.842  9.842  16.8275  12.7  57.29  2.46  1.
-20.   480.   200.   14.   335.  355.
16.5   9.0    14.45  10020.  64.4
0.0196 2000.   0.      500.   650.
650.   500.   700.
2.28   0.0032  1.6
34.    15.     2.      0.02227
3.65   0.08   0.35   0.80   0.012  0.0000065
0.1    0.22   200.   50.
4.57   1.625  2.95   1.625  1.      1.
7.     1.     3.
18
9
0.      0.058  0.096  0.135  0.173  0.211  0.25  0.288
0.308  0.692  0.712  0.75   0.789  0.827  0.865  0.904
0.942  1.0    0.096  0.304  0.544  0.755  0.911  0.991
0.     0.029  0.096  0.911  0.755  0.544  0.304  0.096
1.0    1.0    0.991
0.029  0.0    0.1    0.15   0.2    0.25   0.3    0.35
0.0    0.05   0.1    0.15   0.2    0.25   0.3    0.35
0.4    0.08   0.135  0.19   0.25   0.3    0.35   0.41
0.0
0.47
18
10
0.      0.058  0.096  0.135  0.173  0.211  0.25  0.288
0.308  0.692  0.712  0.75   0.789  0.827  0.865  0.904
0.942  1.0    0.096  0.304  0.544  0.755  0.911  0.991
0.     0.029  0.096  0.911  0.755  0.544  0.304  0.096
1.0    1.0    0.991
0.029  0.0    0.1    0.15   0.2    0.25   0.3    0.35
0.0    0.05   0.1    0.15   0.2    0.25   0.3    0.35
0.4    0.46   0.25   0.35   0.44   0.52   0.57   0.61
0.0    0.15
0.67   0.65
8
310.   1.
0.960  1.035  310.
2.     2.     2.     2.     2.
1.     1.     1.     1.
1.27   640.   0.5    540.
0.420.
-10.   710.
1

```


INTAKE VALVE--EFFECTIVE FLOW AREA VS. CRANK ANGLE

NORMALIZED CRANK ANGLE									
0.0	0.058	0.096	0.135	0.173	0.211	0.250	0.288	0.308	0.692
0.712	0.750	0.789	0.827	0.865	0.904	0.942	1.000		
NORMALIZED EFFECTIVE FLW AREA									
0.0	0.000	0.005	0.044	0.132	0.240	0.345	0.409	0.417	0.417
0.409	0.345	0.240	0.132	0.044	0.005	0.000	0.0		

EXHAUST VALVE--EFFECTIVE FLOW AREA VS. CRANK ANGLE

POST VALVE EFFECTIVE FLOW AREA 75% CRANK ANGLE	NORMALIZED CRANK ANGLE	0.0	0.058	0.135	0.173	0.211	0.250	0.288	0.308	0.692
	0.712	0.750	0.789	0.827	0.865	0.904	0.942	1.000		
NORMALIZED EFFECTIVE FLOW AREA	0.0	0.001	0.015	0.116	0.310	0.480	0.592	0.644	0.650	0.650
	0.644	0.592	0.480	0.310	0.116	0.015	0.001	0.0		

INTAKE AND EXHAUST VALVE OPEN

CUTPUT DATA		P		T		V		WCRK		CYL.MAS		HEAT TRANSFER		AEFI		GWI		AEFE		GWE	
THED	ATA	ATA	K	K	CM**3	PS	KG	CAL/A	CAL	CM**2	G/S	CM**2	G/S	CM**2	G/S	CM**2	G/S				
-8.0	1.31	792.	75.	-0.00	0.043	-0.862E-02	-0.345E-01	0.01	-0.16	0.17	-2.99										
-6.0	1.33	792.	73.	-0.00	0.043	-0.887E-02	-0.700E-01	0.03	-0.28	0.13	-2.47										
-4.0	1.35	793.	71.	-0.00	0.043	-0.901E-02	-0.106E+00	0.05	-0.73	0.09	-1.85										
-2.0	1.35	791.	70.	-0.00	0.042	-0.901E-02	-0.142E+00	0.08	-1.22	0.05	-1.17										
0.0	1.34	788.	70.	-0.01	0.042	-0.886E-02	-0.177E+00	0.11	-1.69	0.02	-0.49										
2.0	1.31	773.	70.	-0.00	0.041	-0.854E-02	-0.212E+00	0.21	-2.35	0.02	-0.30										
4.0	1.25	773.	71.	-0.00	0.040	-0.793E-02	-0.243E+00	0.42	-5.27	0.01	-0.24										
6.0	1.16	758.	73.	-0.00	0.039	-0.698E-02	-0.271E+00	0.63	-7.71	0.01	-0.16										
8.0	1.06	741.	75.	-0.00	0.038	-0.583E-02	-0.295E+00	0.84	-8.55	0.01	-0.09										
10.0	0.98	725.	77.	-0.00	0.037	-0.471E-02	-0.313E+00	1.09	-6.60	0.01	0.02										
12.0	0.95	721.	81.	-0.00	0.037	-0.397E-02	-0.329E+00	1.59	3.43	0.00	0.04										
14.0	0.95	724.	84.	-0.00	0.039	-0.407E-02	-0.346E+00	2.08	10.18	0.0	0.01										

INTAKE VALVE OPEN

OUTPUT DATA			T		V		WCRK		CYL-MAS		HEAT TRANSFER		AEFT		GWI	
THEC	P	ATA	K	CM**3	PS	G	CM**3	PS	G	CAL/A	CAL	CM#2	G/S			
16.0	0.95	726.	89.	-0.30	-0.30	0.041	-0.426E-02	-0.363E+00	2.57	11.68	13.06					
18.0	0.95	727.	94.	-0.30	-0.30	0.043	-0.445E-02	-0.381E+00	3.06	13.06	22.59					
20.0	0.93	692.	99.	-0.31	-0.31	0.047	-0.376E-02	-0.394E+00	3.66	22.59	33.03					
22.0	0.92	653.	105.	-0.31	-0.31	0.052	-0.190E-02	-0.403E+00	4.27	33.03	39.28					
24.0	0.92	616.	111.	-0.31	-0.31	0.059	0.416E-04	-0.403E+00	4.88	39.28	43.92					
26.0	0.92	583.	118.	-0.31	-0.31	0.066	0.195E-02	-0.395E+00	5.48	43.92	47.65					
28.0	0.93	555.	126.	-0.31	-0.31	0.074	0.378E-02	-0.390E+00	6.06	47.65	50.50					
30.0	0.93	530.	134.	-0.31	-0.31	0.083	0.551E-02	-0.358E+00	6.63	50.50	54.04					
32.0	0.93	509.	142.	-0.31	-0.31	0.092	0.716E-02	-0.329E+00	7.20	54.04	57.05					
34.0	0.93	491.	151.	-0.31	-0.31	0.101	0.871E-02	-0.295E+00	7.76	57.05	59.45					
36.0	0.93	475.	161.	-0.32	-0.32	0.111	0.102E-01	-0.254E+00	8.23	59.45	61.29					
38.0	0.93	462.	170.	-0.32	-0.32	0.121	0.115E-01	-0.208E+00	8.59	61.29	63.59					
40.0	0.93	450.	180.	-0.32	-0.32	0.132	0.128E-01	-0.154E+00	8.94	63.59	65.94					
42.0	0.93	440.	191.	-0.32	-0.32	0.143	0.141E-01	-0.100E+00	9.30	65.94	68.11					
44.0	0.93	431.	202.	-0.32	-0.32	0.154	0.153E-01	-0.390E-01	9.57	68.11	69.36					
46.0	0.93	423.	213.	-0.32	-0.32	0.166	0.164E-01	0.265E-01	9.65	69.36	70.87					
48.0	0.93	415.	224.	-0.32	-0.32	0.178	0.175E-01	0.946E-01	9.72	70.87	72.26					
50.0	0.93	407.	236.	-0.33	-0.33	0.190	0.186E-01	0.171E+00	9.72	72.26	73.71					
52.0	0.93	403.	248.	-0.33	-0.33	0.202	0.196E-01	0.311E+00	9.72	73.71	74.95					
54.0	0.93	399.	261.	-0.33	-0.33	0.214	0.206E-01	0.418E+00	9.72	74.95	76.21					
56.0	0.93	393.	273.	-0.33	-0.33	0.227	0.215E-01	0.418E+00	9.72	76.21	77.35					
58.0	0.93	389.	285.	-0.34	-0.34	0.240	0.225E-01	0.508E+00	9.72	77.35	78.39					
60.0	0.93	385.	299.	-0.34	-0.34	0.253	0.234E-01	0.601E+00	9.72	78.39	79.30					
62.0	0.93	382.	312.	-0.34	-0.34	0.266	0.243E-01	0.690E+00	9.72	79.30	80.10					
64.0	0.92	379.	325.	-0.34	-0.34	0.280	0.252E-01	0.794E+00	9.72	80.10	81.36					
66.0	0.92	376.	339.	-0.35	-0.35	0.293	0.261E-01	0.904E+00	9.72	81.36	82.16					
68.0	0.92	374.	352.	-0.35	-0.35	0.307	0.270E-01	0.101E+01	9.72	82.16	82.40					
70.0	0.92	371.	366.	-0.35	-0.35	0.320	0.278E-01	0.112E+01	9.72	82.40	82.53					
72.0	0.92	368.	379.	-0.35	-0.35	0.334	0.287E-01	0.124E+01	9.72	82.53	82.66					
74.0	0.92	367.	393.	-0.35	-0.35	0.348	0.295E-01	0.136E+01	9.72	82.66	82.77					
76.0	0.92	365.	406.	-0.35	-0.35	0.361	0.303E-01	0.148E+01	9.72	82.77	82.82					
78.0	0.92	364.	420.	-0.36	-0.36	0.375	0.311E-01	0.160E+01	9.72	82.82	82.85					
80.0	0.92	362.	434.	-0.36	-0.36	0.389	0.319E-01	0.173E+01	9.72	82.85	82.86					
82.0	0.92	361.	447.	-0.36	-0.36	0.403	0.327E-01	0.186E+01	9.72	82.86	82.87					
84.0	0.92	360.	461.	-0.36	-0.36	0.416	0.335E-01	0.199E+01	9.72	82.87	82.88					
86.0	0.92	359.	474.	-0.37	-0.37	0.430	0.343E-01	0.213E+01	9.72	82.88	82.89					
88.0	0.92	358.	487.	-0.37	-0.37	0.443	0.350E-01	0.227E+01	9.72	82.89	82.90					
90.0	0.93	357.	500.	-0.37	-0.37	0.457	0.357E-01	0.242E+01	9.72	82.90	82.91					
92.0	0.93	356.	513.	-0.37	-0.37	0.470	0.365E-01	0.255E+01	9.72	82.91	82.92					
94.0	0.93	355.	526.	-0.38	-0.38	0.483	0.372E-01	0.268E+01	9.72	82.92	82.93					
96.0	0.93	355.	539.	-0.38	-0.38	0.496	0.379E-01	0.286E+01	9.72	82.93	82.94					
98.0	0.93	354.	551.	-0.38	-0.38	0.509	0.385E-01	0.302E+01	9.72	82.94	82.95					
100.0	0.93	353.	564.	-0.38	-0.38	0.522	0.392E-01	0.317E+01	9.72	82.95	82.96					
102.0	0.93	352.	576.	-0.38	-0.38	0.534	0.399E-01	0.333E+01	9.72	82.96	82.97					
104.0	0.93	352.	588.	-0.38	-0.38	0.547	0.405E-01	0.349E+01	9.72	82.97	82.98					
106.0	0.93	352.	599.	-0.39	-0.39	0.559	0.411E-01	0.366E+01	9.72	82.98	82.99					
108.0	0.93	352.	611.	-0.39	-0.39	0.571	0.417E-01	0.382E+01	9.72	82.99	83.00					
110.0	0.94	352.	622.	-0.39	-0.39	0.582	0.424E-01	0.399E+01	9.72	83.00	83.01					
112.0	0.94	351.	633.	-0.39	-0.39	0.593	0.429E-01	0.417E+01	9.72	83.01	83.02					
114.0	0.94	351.	643.	-0.39	-0.39	0.604	0.434E-01	0.434E+01	9.72	83.02	83.03					
116.0	0.94	351.	653.	-0.39	-0.39	0.615	0.439E-01	0.451E+01	9.72	83.03	83.04					
118.0	0.94	351.	664.	-0.40	-0.40	0.626	0.444E-01	0.469E+01	9.72	83.04	83.05					
120.0	0.94	351.	673.	-0.40	-0.40	0.636	0.449E-01	0.487E+01	9.72	83.05	83.06					
122.0	0.94	351.	683.	-0.40	-0.40	0.646	0.454E-01	0.505E+01	9.72	83.06	83.07					
124.0	0.94	351.	692.	-0.40	-0.40	0.655	0.459E-01	0.524E+01	9.72	83.07	83.08					
126.0	0.95	351.	701.	-0.40	-0.40	0.664	0.463E-01	0.542E+01	9.72	83.08	83.09					
128.0	0.95	351.	709.	-0.40	-0.40	0.673	0.467E-01	0.561E+01	9.72	83.09	83.10					

130.0	0.95	351.	715.	-0.10	0.471E-01	0.580E+01	9.72	50.91
132.0	0.95	351.	725.	-0.10	0.475E-01	0.595E+01	9.72	48.76
134.0	0.95	351.	735.	-0.10	0.478E-01	0.614E+01	9.65	46.43
136.0	0.95	352.	740.	-0.10	0.481E-01	0.637E+01	9.57	43.99
138.0	0.95	352.	747.	-0.11	0.484E-01	0.657E+01	9.30	41.40
140.0	0.95	352.	754.	-0.11	0.487E-01	0.676E+01	8.94	38.40
142.0	0.95	352.	760.	-0.11	0.490E-01	0.696E+01	8.59	35.78
144.0	0.95	352.	766.	-0.11	0.492E-01	0.715E+01	8.23	33.40
146.0	0.95	352.	772.	-0.11	0.494E-01	0.735E+01	7.76	31.09
148.0	0.95	352.	777.	-0.11	0.495E-01	0.755E+01	7.20	28.37
150.0	0.95	353.	782.	-0.11	0.498E-01	0.775E+01	6.63	25.68
152.0	0.95	353.	787.	-0.11	0.499E-01	0.795E+01	6.06	23.54
154.0	0.95	354.	791.	-0.11	0.500E-01	0.815E+01	5.48	21.28
156.0	0.95	354.	795.	-0.11	0.501E-01	0.835E+01	4.88	18.99
158.0	0.95	354.	797.	-0.11	0.502E-01	0.855E+01	4.27	16.72
160.0	0.95	355.	803.	-0.11	0.503E-01	0.875E+01	3.65	14.48
162.0	0.95	355.	806.	-0.11	0.503E-01	0.895E+01	3.06	12.26
164.0	0.95	356.	809.	-0.11	0.503E-01	0.915E+01	2.57	10.26
166.0	0.95	356.	811.	-0.11	0.503E-01	0.935E+01	2.08	8.42
168.0	0.95	357.	813.	-0.11	0.503E-01	0.955E+01	1.59	6.56
170.0	0.95	357.	815.	-0.11	0.503E-01	0.975E+01	1.09	4.72
172.0	0.95	358.	816.	-0.11	0.501E-01	0.995E+01	0.84	3.27
174.0	0.95	358.	817.	-0.11	0.501E-01	0.995E+01	0.63	2.40
176.0	0.95	359.	818.	-0.11	0.503E-01	0.104E+02	0.42	1.56
178.0	0.95	359.	819.	-0.11	0.499E-01	0.106E+02	0.21	0.80
180.0	0.95	360.	819.	-0.11	0.498E-01	0.108E+02	0.11	0.23
182.0	0.95	361.	819.	-0.11	0.497E-01	0.110E+02	0.08	-0.08
184.0	0.95	362.	819.	-0.11	0.495E-01	0.112E+02	0.05	-0.16
186.0	0.97	363.	817.	-0.11	0.494E-01	0.113E+02	0.03	-0.14
188.0	0.97	363.	816.	-0.11	0.493E-01	0.115E+02	0.01	-0.07
190.0	0.97	363.	815.	-0.11	0.491E-01	0.117E+02	0.01	-0.05
192.0	0.93	364.	813.	-0.11	0.490E-01	0.119E+02	0.01	-0.05
194.0	0.93	365.	811.	-0.11	0.488E-01	0.121E+02	0.01	-0.04
196.0	0.99	367.	808.	-0.11	0.487E-01	0.123E+02	0.00	-0.03
198.0	0.99	369.	806.	-0.11	0.485E-01	0.125E+02	0.00	-0.02
200.0	1.00	370.	803.	-0.11	0.483E-01	0.127E+02	0.0	-0.01

OVERALL EQUIVALENCE RATIO = 0.590
 VOLUMETRIC EFFICIENCY = 0.855
 CORRECT CHARGED AIR PHI = 0.031
 INDUCED AIR AND REG. GAS NOX ppm = 52.4 PASS = 0.418E-046

COMPRESSION

CUTPUT DATA										S-RT
THED	ATA	T	V	WCRK	CYL-MAS	HEAT	TRANSFER	FSWR	*RPM	
REC		K	CMW3	PS	G	CAL/A	CAL			
202.0	1.01	371.	799.	-0.11	C.768	0.482E-01	0.129E+02	0.999	3.65	
204.0	1.02	373.	795.	-0.11	C.768	0.480E-01	0.131E+02	0.999	3.65	
206.0	1.03	374.	791.	-0.11	C.768	0.478E-01	0.133E+02	0.998	3.65	
208.0	1.04	375.	787.	-0.11	C.768	0.476E-01	0.135E+02	0.997	3.65	
210.0	1.05	377.	782.	-0.11	C.768	0.473E-01	0.137E+02	0.997	3.65	
212.0	1.06	379.	777.	-0.11	C.768	0.471E-01	0.139E+02	0.996	3.65	
214.0	1.07	380.	772.	-0.12	C.768	0.469E-01	0.140E+02	0.996	3.65	
216.0	1.09	382.	766.	-0.12	C.768	0.466E-01	0.142E+02	0.995	3.65	
218.0	1.10	384.	760.	-0.12	C.768	0.464E-01	0.144E+02	0.994	3.65	
220.0	1.12	386.	754.	-0.12	C.768	0.461E-01	0.146E+02	0.994	3.64	
222.0	1.13	388.	747.	-0.12	C.768	0.459E-01	0.148E+02	0.993	3.64	
224.0	1.15	390.	740.	-0.12	C.768	0.456E-01	0.150E+02	0.992	3.64	
226.0	1.17	392.	733.	-0.13	C.768	0.453E-01	0.151E+02	0.992	3.64	
228.0	1.18	394.	725.	-0.13	C.764	0.450E-01	0.153E+02	0.991	3.64	
230.0	1.19	396.	718.	-0.13	C.768	0.447E-01	0.155E+02	0.991	3.64	
232.0	1.23	399.	709.	-0.14	C.768	0.444E-01	0.157E+02	0.990	3.64	
234.0	1.25	401.	701.	-0.14	C.768	0.440E-01	0.159E+02	0.989	3.64	
236.0	1.27	404.	692.	-0.15	C.768	0.437E-01	0.160E+02	0.988	3.64	
238.0	1.30	406.	683.	-0.15	C.768	0.433E-01	0.162E+02	0.988	3.65	
240.0	1.31	409.	673.	-0.16	C.768	0.430E-01	0.164E+02	0.987	3.65	
242.0	1.35	412.	664.	-0.17	C.768	0.426E-01	0.166E+02	0.987	3.65	
244.0	1.38	415.	653.	-0.17	C.769	0.422E-01	0.167E+02	0.986	3.65	
246.0	1.42	418.	643.	-0.14	C.768	0.419E-01	0.169E+02	0.985	3.65	
248.0	1.45	421.	633.	-0.19	C.769	0.413E-01	0.171E+02	0.985	3.65	
250.0	1.49	424.	622.	-0.20	C.768	0.409E-01	0.172E+02	0.984	3.66	
252.0	1.53	428.	611.	-0.22	C.768	0.404E-01	0.174E+02	0.984	3.66	
254.0	1.57	431.	599.	-0.24	C.768	0.399E-01	0.175E+02	0.983	3.66	
256.0	1.62	435.	588.	-0.24	C.768	0.394E-01	0.177E+02	0.982	3.66	
258.0	1.66	439.	576.	-0.26	C.764	0.389E-01	0.179E+02	0.982	3.67	
260.0	1.71	443.	564.	-0.28	C.768	0.383E-01	0.180E+02	0.981	3.67	
262.0	1.77	447.	551.	-0.30	C.768	0.377E-01	0.181E+02	0.980	3.67	
264.0	1.83	451.	539.	-0.32	C.768	0.370E-01	0.183E+02	0.980	3.68	
266.0	1.89	456.	526.	-0.35	C.768	0.364E-01	0.184E+02	0.979	3.68	
268.0	1.95	461.	513.	-0.37	C.768	0.357E-01	0.186E+02	0.978	3.69	
270.0	2.03	466.	500.	-0.40	C.768	0.350E-01	0.187E+02	0.978	3.69	
272.0	2.11	471.	487.	-0.43	C.768	0.342E-01	0.189E+02	0.977	3.70	
274.0	2.19	476.	474.	-0.47	C.769	0.334E-01	0.190E+02	0.976	3.71	
276.0	2.28	481.	461.	-0.50	C.768	0.325E-01	0.191E+02	0.975	3.71	
278.0	2.34	487.	447.	-0.54	C.768	0.316E-01	0.193E+02	0.975	3.72	
280.0	2.42	493.	434.	-0.59	C.768	0.307E-01	0.194E+02	0.975	3.73	
282.0	2.50	497.	420.	-0.63	C.768	0.297E-01	0.195E+02	0.974	3.74	
284.0	2.57	506.	406.	-0.68	C.768	0.286E-01	0.196E+02	0.973	3.75	
286.0	2.65	512.	393.	-0.74	C.768	0.274E-01	0.197E+02	0.973	3.76	
288.0	2.80	527.	379.	-0.80	C.764	0.261E-01	0.198E+02	0.972	3.78	
290.0	3.14	534.	366.	-0.85	C.768	0.249E-01	0.199E+02	0.971	3.79	
292.0	3.31	534.	352.	-0.92	C.768	0.234E-01	0.200E+02	0.970	3.81	
294.0	3.40	542.	339.	-1.00	C.768	0.218E-01	0.201E+02	0.969	3.84	
296.0	3.50	551.	325.	-1.07	C.768	0.202E-01	0.202E+02	0.969	3.86	
298.0	3.59	553.	312.	-1.14	C.768	0.194E-01	0.203E+02	0.968	3.88	
300.0	4.15	562.	299.	-1.24	C.768	0.165E-01	0.203E+02	0.967	3.91	
302.0	4.40	571.	285.	-1.34	C.768	0.144E-01	0.204E+02	0.966	3.94	
304.0	4.69	587.	271.	-1.44	C.768	0.122E-01	0.204E+02	0.965	3.97	
306.0	5.00	597.	261.	-1.55	C.768	0.073E-02	0.205E+02	0.965	4.00	
308.0	5.34	607.	248.	-1.66	C.769	0.706E-02	0.205E+02	0.965	4.03	
310.0	5.71	618.	235.	-1.78	C.769	0.414E-02	0.205E+02	0.964	4.07	
312.0	6.12	629.	224.	-1.91	C.768	0.045E-03	0.205E+02	0.963	4.12	
314.0	6.57	641.	213.	-2.05	C.768	-0.257E-02	0.205E+02	0.962	4.17	
316.0	7.06	653.	202.	-2.19	C.768	-0.644E-02	0.205E+02	0.961	4.17	

318.0	7.60	665.	191.	-2.34	C.768	-0.107E-01	0.204E+02	0.961	4.23
325.0	8.23	678.	180.	-2.51	C.768	-0.154E-01	0.204E+02	0.960	4.29
322.0	8.86	691.	170.	-2.57	C.768	-0.207E-01	0.203E+02	0.959	4.36
324.0	9.58	705.	161.	-2.85	C.768	-0.264E-01	0.202E+02	0.958	4.44
326.0	10.37	719.	151.	-3.04	C.768	-0.329E-01	0.201E+02	0.957	4.52
328.0	11.24	733.	142.	-3.23	C.768	-0.400E-01	0.199E+02	0.956	4.62
330.0	12.19	748.	134.	-3.43	C.768	-0.479E-01	0.197E+02	0.955	4.74

COMBUSTION AND EXPANSION

OUTPUT DATA																
THEO	PRESS	RTCH	PS	FSWIR	PPAS	S.R.T	PPM	WNO	ENTH	PPM	WNO	JET LOCATIONS	RJET	C-ANG	H.T.	
NUM		K		MG	MG	MG	CM#3	CAL/G	CAL/G		G*10**6	R(CM)	Z(CM)	DEG	CAL	
333.7 PRESS.= 14.27 PS= -3.8 FSWIR= 0.953 S.R.T= 5.146 SUM.H.REJ=0.192E+02																
TOTAL			C.0													
1	1	777.		758.6			C.59	0.267	193.8	52.	42.					-0.62E-01
2	1	777.		13.2		0.0	2.03	0.432	193.8	52.	41.					-0.23E+00
										48.	0.52	2.0	1.15	32.	0.463	0. 0.0
337.5 PRESS.= 16.61 PS= -4.2 FSWIR= 0.950 S.R.T= 5.506 SUM.H.REJ=0.186E+02																
TOTAL			-0.022													
1	1	805.		742.1			C.59	0.268	201.4	52.	42.					-0.83E-01
2	2	737.		20.1		1.8	1.5	0.349	178.5	52.	40.					-0.31E+00
3	1	805.		13.4		0.0	1.81	0.433	201.4	31.	0.89	2.2	1.77	55.	0.783	137.-0.13E-02
										48.	0.53	2.0	1.16	33.	0.463	0. 0.0
341.2 PRESS.= 19.31 PS= -4.7 FSWIR= 0.948 S.R.T= 5.953 SUM.H.REJ=0.178E+02																
TOTAL			C.001													
1	1	834.		717.9			C.59	0.269	209.1	51.	42.					-0.11E+00
2	2	903.		27.0		6.3	3.56	0.337	235.7	52.	39.					-0.40E+00
3	2	770.		20.7		1.8	1.5	0.349	187.7	37.	1.27	2.4	2.22	74.	1.131	170.-0.34E-02
4	1	834.		13.7		0.0	1.64	0.433	209.1	31.	0.92	2.2	1.77	57.	0.790	138.-0.20E-02
										48.	0.55	2.0	1.15	34.	0.467	0. 0.0
345.0 PRESS.= 22.66 PS= -5.1 FSWIR= 0.945 S.R.T= 6.491 SUM.H.REJ=0.167E+02																
TOTAL			C.017													
1	1	903.		685.3			C.59	0.271	217.3	50.	42.					-0.14E+00
2	2	1245.		34.2		14.7	5.29	0.347	353.7	52.	37.					-0.52E+00
3	2	950.		27.9		6.6	3.26	0.337	249.9	41.	1.66	2.4	2.57	92.	1.367	177.-0.99E-02
4	2	807.		21.5		1.9	2.11	0.348	196.6	37.	1.32	2.4	2.22	76.	1.122	168.-0.49E-02
5	1	965.		14.2		0.0	1.49	0.431	217.3	32.	0.97	2.2	1.75	58.	0.798	138.-0.30E-02
										48.	0.57	2.0	1.14	34.	0.476	0. 0.0
349.7 PRESS.= 27.32 PS= -5.4 FSWIR= 0.941 S.R.T= 7.008 SUM.H.REJ=0.153E+02																
TOTAL			C.067													
1	1	901.		643.4			C.59	0.272	227.3	50.	42.					-0.20E+00
2	2	1452.		41.8		29.8	8.03	0.351	570.0	52.	35.					-0.68E+00
3	2	1321.		35.4		16.0	4.77	0.348	378.3	44.	2.06	2.3	2.85	111.	1.420	170.-0.23E-01
4	2	1004.		28.9		7.0	2.94	0.338	267.3	38.	1.37	2.4	2.56	96.	1.314	172.-0.13E-01
5	2	851.		22.4		2.0	1.91	0.348	212.1	33.	1.01	2.3	2.19	79.	1.105	166.-0.71E-02
6	1	901.		14.9		0.0	1.33	0.429	227.3	39.	0.51	2.2	1.72	60.	0.807	138.-0.44E-02
										48.	0.57	2.0	1.12	35.	0.487	24.-0.11E-02
352.5 PRESS.= 34.40 PS= -5.8 FSWIR= 0.936 S.R.T= 7.694 SUM.H.REJ=0.132E+02																
TOTAL			C.112													
1	1	945.		591.2			C.59	0.274	240.0	50.	42.					-0.28E+00
2	3	2325.		50.3		41.8	9.58	0.356	732.8	52.	32.					-0.93E+00
3	3	2138.		43.4		35.4	7.53	0.354	665.5	48.	2.60	2.1	3.06	134.	1.341	148.-0.39E-01
4	3	1745.		36.7		28.9	5.14	0.357	528.0	44.	2.15	2.2	2.83	117.	1.320	159.-0.32E-01
5	2	1247.		30.0		18.3	2.98	0.356	352.8	42.	1.79	2.3	2.52	100.	1.250	165.-0.23E-01
6	2	823.		21.3		7.8	1.51	0.343	197.5	38.	1.43	2.3	2.14	83.	1.083	162.-0.13E-01
7	1	948.		15.5		0.0	1.14	0.427	240.0	34.	1.06	2.2	1.67	62.	0.813	138.-0.57E-02
										49.	0.64	2.0	1.08	36.	0.500	42.-0.26E-02
356.2 PRESS.= 41.54 PS= -6.0 FSWIR= 0.931 S.R.T= 8.140 SUM.H.REJ=0.102E+02																
TOTAL			C.314													
1	1	933.		529.5			C.59	0.276	249.8	75.	63.					-0.39E+00
2	3	2532.		59.9		50.3	10.11	0.365	760.6	52.	29.					-0.12E+01
3	3	2403.		43.4		43.4	8.38	0.365	600.6	385.	23.71	1.8	3.24	164.	1.263	120.-0.52E-01
4	3	2213.		44.8		36.7	6.61	0.354	696.5	56.	3.09	2.0	3.05	144.	1.240	133.-0.49E-01
5	3	1978.		37.3		30.0	4.93	0.359	615.4	45.	2.22	2.1	2.79	125.	1.230	147.-0.43E-01
6	3	1470.		31.0		23.3	2.97	0.361	429.8	42.	1.85	2.2	2.46	106.	1.189	158.-0.34E-01
7	2	838.		24.1		8.3	1.39	0.345	221.3	39.	1.48	2.3	2.07	87.	1.062	159.-0.20E-01
8	1	951.		16.1		0.0	1.01	0.425	249.8	34.	1.11	2.2	1.60	65.	0.820	139.-0.92E-02
										49.	0.68	2.0	1.04	37.	0.513	55.-0.46E-02

365.0	PRESS.= 47.53	PS= -6.1	FSWIR= 0.925	S.RT= 8.275	SUM.H.REJ=0.656E+01	284.	241.	-0.49E+00
TOTAL		C.454				52.	25.	-0.15E+01
1	1	1005.	643.1	58.9	67.99	2293.	150.40	111.-0.65E-01
2	3	2630.	65.3	58.9	10.18	2293.	150.40	111.-0.65E-01
3	3	2584.	57.5	51.9	9.03	765.	47.67	121.-0.59E-01
4	3	2457.	52.7	44.8	7.53	73.	4.09	139.-0.52E-01
5	3	2272.	45.5	37.8	5.96	45.	2.29	154.-0.44E-01
6	3	2046.	38.5	31.0	4.49	43.	1.88	159.-0.36E-01
7	3	1553.	31.7	24.1	2.77	39.	1.52	142.-0.13E-01
8	2	956.	24.7	8.6	1.32	35.	1.14	66.-0.68E-02
9	1	1005.	16.5	0.0	0.93	49.	0.70	
361.7	PRESS.= 51.16	PS= -6.0	FSWIR= 0.919	S.RT= 8.035	SUM.H.REJ=0.231E+01	616.	524.	-0.57E+00
TOTAL		C.584				52.	22.	-0.17E+01
1	1	1010.	413.4	65.3	71.02	3297.	244.12	139.-0.93E-01
2	3	2560.	71.1	59.5	9.99	2712.	183.00	125.-0.82E-01
3	3	2638.	64.6	52.7	8.28	1029.	63.22	117.-0.70E-01
4	3	2624.	58.6	45.5	6.92	84.	4.65	122.-0.63E-01
5	3	2486.	52.2	38.5	5.53	45.	2.25	139.-0.60E-01
6	3	2319.	45.2	31.7	4.22	42.	1.88	157.-0.51E-01
7	3	2097.	38.6	24.5	2.67	40.	1.54	163.-0.31E-01
8	3	1608.	32.1	7.0	1.28	35.	1.16	148.-0.16E-01
9	2	992.	25.0	8.6	0.93			
357.5	PRESS.= 52.31	PS= -5.7	FSWIR= 0.913	S.RT= 7.505	SUM.H.REJ=-.227E+01	882.	744.	-0.61E+00
TOTAL		C.713				52.	19.	-0.17E+01
1	1	1301.	357.7	71.1	19.22	3254.	271.29	167.-0.11E+00
2	3	2419.	80.2	64.6	9.61	2409.	162.37	148.-0.96E-01
3	3	2504.	72.8	53.6	8.80	752.	45.05	136.-0.82E-01
4	3	2627.	64.6	52.2	7.73	83.	4.51	136.-0.71E-01
5	3	2619.	57.0	45.2	6.49	45.	2.20	151.-0.56E-01
6	3	2534.	50.6	38.6	5.25	42.	1.87	167.-0.56E-01
7	3	2345.	44.3	32.1	4.09	40.	1.54	171.-0.34E-01
8	3	2123.	38.4	25.0	2.62	35.	1.16	
9	3	1600.	32.2	8.6	1.02			
371.2	PRESS.= 51.57	PS= -5.1	FSWIR= 0.908	S.RT= 6.852	SUM.H.REJ=-.680E+01	1037.	870.	-0.60E+00
TOTAL		C.807				52.	17.	-0.16E+01
1	1	978.	303.0	80.2	16.36	3045.	277.46	178.-0.10E+00
2	3	2278.	97.8	72.8	10.32	2917.	248.31	179.-0.11E+00
3	3	2345.	81.9	64.6	9.71	2541.	195.07	176.-0.11E+00
4	3	2453.	73.9	57.0	8.92	1569.	105.02	167.-0.10E+00
5	3	2557.	64.2	50.6	7.51	350.	20.47	156.-0.87E-01
6	3	2577.	55.5	44.3	6.31	65.	3.47	156.-0.76E-01
7	3	2481.	49.0	38.4	5.23	44.	2.14	168.-0.69E-01
8	3	2335.	41.5	32.2	4.14	42.	1.86	179.-0.57E-01
9	3	2116.	34.2	8.6	1.59			
373.0	PRESS.= 48.01	PS= -4.3	FSWIR= 0.904	S.RT= 6.213	SUM.H.REJ=-.109E+02	1140.	953.	-0.55E+00
TOTAL		C.872				52.	14.	-0.14E+01
1	1	944.	263.0	87.8	14.66	2960.	279.61	180.-0.92E-01
2	3	2199.	97.8	81.9	11.19	2825.	251.59	177.-0.91E-01
3	3	2246.	85.0	73.9	10.63	2483.	204.59	179.-0.90E-01
4	3	2332.	79.1	64.2	9.96	1780.	132.95	180.-0.91E-01
5	3	2446.	71.5	55.5	8.91	859.	50.14	180.-0.93E-01
6	3	2522.	62.7	49.0	7.53	142.	8.09	173.-0.84E-01
7	3	2511.	53.9	43.5	6.44	53.	2.75	174.-0.75E-01
8	3	2434.	47.0	38.2	5.44	44.	2.10	180.-0.66E-01
9	3	2306.	42.0	8.6	1.40			
378.7	PRESS.= 43.57	PS= -3.4	FSWIR= 0.901	S.RT= 5.457	SUM.H.REJ=-.145E+02	1224.	1019.	-0.47E+00
TOTAL		C.910				52.	13.	-0.12E+01
1	1	905.	236.2	90.7	13.93	2906.	280.35	176.-0.82E-01
2	3	2121.	92.9	85.9	12.27	2736.	253.08	179.-0.80E-01
3	3	2151.	89.1	79.3	11.63	2457.	207.90	175.-0.79E-01
4	3	2255.	81.5	55.5	8.72			

5	3	2389.	2350.	1.000	72.5	71.5	71.5	10.89	0.81	0.376	755.3	1952.	146.97	2.4	3.49	273.	1.550	178.-0.81E-01
6	3	2480.	2490.	0.995	66.9	62.7	62.7	10.32	0.88	0.417	787.4	1246.	86.77	2.5	3.47	249.	1.845	180.-0.80E-01
7	3	2522.	2532.	0.990	59.4	53.9	53.9	9.12	1.00	0.463	798.3	393.	24.38	2.5	3.16	222.	1.699	180.-0.79E-01
8	3	2460.	2460.	0.981	52.4	47.9	47.9	7.85	1.13	0.376	781.5	78.	4.37	2.5	2.80	191.	1.582	180.-0.72E-01
9	3	2385.	2385.	0.967	47.1	42.9	42.9	6.91	1.27	0.358	753.4	48.	2.45	2.5	2.42	162.	1.494	180.-0.66E-01
PRESS.= 41.27 PS= -2.9 FSWIR= 0.899 S.RT= 5.402 SUM.H.REJ=-.162E+02																		
TOTAL				C.950	223.8	92.9	92.8	13.62	C.59	0.272	222.7	1270.	1057.					-0.42E+00
1	1	894.							C.61	0.272	222.7	52.	12.					-0.53E+00
2	3	2073.	2073.	0.999	94.5	92.9	92.8	13.37	0.62	0.328	556.4	2800.	280.59	2.4	4.13	336.	2.285	174.-0.40E-01
3	3	2101.	2101.	0.998	80.7	85.1	89.0	12.87	0.65	0.370	661.1	2491.	253.40	2.3	3.51	323.	2.113	169.-0.39E-01
4	3	2056.	2056.	0.979	82.5	81.5	81.4	12.20	0.71	0.339	662.1	2436.	208.88	2.3	3.53	304.	2.043	173.-0.39E-01
5	3	2153.	2153.	0.999	73.1	72.5	72.4	11.41	0.81	0.368	711.9	1599.	151.73	2.4	3.54	284.	1.950	178.-0.40E-01
6	3	2445.	2446.	0.997	67.5	66.9	66.7	10.85	0.87	0.405	773.5	1392.	97.78	2.5	3.57	260.	1.849	180.-0.39E-01
7	3	2524.	2524.	0.977	61.8	59.4	59.1	10.10	0.96	0.461	808.4	628.	40.47	2.5	3.26	234.	1.739	180.-0.40E-01
8	3	2537.	2537.	0.874	54.7	52.4	52.2	8.92	1.09	0.423	812.2	149.	8.61	2.5	2.90	203.	1.624	180.-0.37E-01
9	3	2487.	2487.	0.758	47.2	47.1	46.8	7.84	1.21	0.371	790.4	60.	3.19	2.5	2.52	174.	1.535	180.-0.35E-01
PRESS.= 38.64 PS= -2.4 FSWIR= 0.898 S.RT= 5.174 SUM.H.REJ=-.177E+02																		
TOTAL				C.964	209.5	94.5	94.4	14.18	C.59	0.271	214.7	1304.	1083.					-0.38E+00
1	1	862.							C.61	0.271	214.7	52.	11.	2.3	4.20	348.	2.285	173.-0.37E-01
2	3	2721.	2721.	0.999	95.2	90.7	90.6	13.65	0.64	0.326	639.2	2810.	280.74	2.3	3.56	336.	2.113	169.-0.36E-01
3	3	2052.	2052.	0.994	83.7	82.6	82.5	12.92	0.70	0.336	676.4	2410.	209.41	2.3	3.58	316.	2.043	173.-0.36E-01
4	3	2160.	2160.	0.999	83.7	82.6	82.5	12.92	0.70	0.336	676.4	2410.	209.41	2.3	3.58	316.	2.043	173.-0.36E-01
5	3	2307.	2307.	1.000	74.0	73.1	73.0	12.10	0.80	0.359	725.3	2011.	154.46	2.4	3.59	295.	1.974	179.-0.37E-01
6	3	2374.	2374.	0.999	70.0	67.6	67.5	11.65	0.84	0.380	745.5	1421.	103.29	2.5	3.66	271.	1.888	180.-0.37E-01
7	3	2464.	2466.	0.944	64.1	61.8	61.6	10.74	0.92	0.429	782.6	767.	51.17	2.5	3.36	246.	1.779	180.-0.38E-01
8	3	2525.	2525.	0.818	56.9	54.7	54.6	9.88	1.04	0.456	807.1	247.	14.79	2.5	3.00	215.	1.665	180.-0.36E-01
9	3	2494.	2494.	0.808	51.3	45.2	49.1	8.76	1.15	0.382	793.1	79.	4.33	2.5	2.61	186.	1.576	180.-0.34E-01
PRESS.= 36.06 PS= -1.8 FSWIR= 0.896 S.RT= 4.973 SUM.H.REJ=-.191E+02																		
TOTAL				C.975	194.3	96.2	96.1	15.09	C.59	0.270	210.8	1328.	1102.					-0.34E+00
1	1	840.							C.61	0.270	210.8	52.	11.	2.3	4.28	359.	2.292	172.-0.34E-01
2	3	1966.	1966.	0.999	98.2	92.2	92.1	14.52	0.63	0.326	627.7	2755.	280.87	2.3	3.61	348.	2.159	171.-0.34E-01
3	3	1999.	1999.	0.999	85.1	83.7	83.6	13.74	0.69	0.333	659.0	2602.	253.71	2.3	3.63	328.	2.084	175.-0.34E-01
4	3	2107.	2107.	0.999	75.3	74.0	73.9	12.88	0.78	0.350	705.5	1993.	155.85	2.5	3.65	306.	2.007	180.-0.34E-01
5	3	2252.	2252.	0.998	72.1	70.0	69.8	12.47	0.82	0.362	718.8	1414.	105.80	2.5	3.74	283.	1.922	180.-0.34E-01
6	3	2302.	2302.	0.998	66.4	64.1	64.0	11.85	0.89	0.401	757.5	833.	57.54	2.5	3.45	258.	1.819	180.-0.35E-01
7	3	2405.	2405.	0.998	59.1	56.9	56.8	10.89	1.00	0.471	795.9	363.	22.43	2.5	3.09	227.	1.705	180.-0.34E-01
8	3	2501.	2501.	0.954	53.4	51.3	51.2	9.74	1.11	0.396	796.6	103.	5.86	2.5	2.70	198.	1.616	180.-0.32E-01
PRESS.= 33.55 PS= -1.3 FSWIR= 0.895 S.RT= 4.795 SUM.H.REJ=-.203E+02																		
TOTAL				C.983	177.8	98.2	98.1	16.09	C.59	0.269	204.8	1345.	1115.					-0.31E+00
1	1	818.							C.61	0.269	204.8	52.	10.	2.3	4.35	371.	2.337	173.-0.32E-01
2	3	1929.	1929.	0.999	100.4	98.2	98.1	15.09	0.59	0.322	602.8	2695.	281.00	2.3	3.66	360.	2.249	174.-0.32E-01
3	3	1919.	1919.	0.999	95.3	93.9	93.8	15.51	0.61	0.324	608.0	2540.	253.85	2.4	3.66	339.	2.161	178.-0.31E-01
4	3	2047.	2047.	0.999	87.0	85.1	85.0	14.67	0.68	0.330	638.0	2324.	209.88	2.4	3.68	317.	2.030	180.-0.32E-01
5	3	2193.	2193.	0.999	76.8	75.3	75.3	13.75	0.77	0.343	685.2	1963.	156.93	2.5	3.70	294.	1.957	190.-0.31E-01
6	3	2232.	2232.	0.999	74.2	72.1	72.0	13.37	0.79	0.350	693.8	1389.	106.93	2.5	3.83	270.	1.858	180.-0.31E-01
7	3	2329.	2329.	0.998	68.7	66.4	66.3	12.76	0.86	0.375	728.2	848.	60.54	2.5	3.54	270.	1.858	180.-0.33E-01
8	3	2459.	2459.	0.975	61.3	59.1	59.0	11.93	0.96	0.449	776.4	457.	29.19	2.5	3.18	239.	1.745	180.-0.32E-01
9	3	2476.	2476.	0.895	55.4	53.4	53.3	10.82	1.07	0.418	785.9	136.	7.91	2.5	2.79	210.	1.655	180.-0.31E-01
PRESS.= 31.17 PS= -0.7 FSWIR= 0.894 S.RT= 4.637 SUM.H.REJ=-.214E+02																		
TOTAL				C.990	160.2	100.4	100.3	17.20	C.59	0.268	199.1	1357.	1125.					-0.27E+00
1	1	777.							C.61	0.268	199.1	52.	9.	2.4	4.42	382.	2.417	176.-0.29E-01
2	3	1848.	1848.	0.999	103.0	96.3	96.1	16.61	0.57	0.321	583.2	2628.	281.14	2.4	3.71	371.	2.380	179.-0.29E-01
3	3	1871.	1871.	0.979	99.2	94.3	94.2	15.69	0.59	0.322	586.4	2465.	254.02	2.4	3.73	349.	2.235	180.-0.28E-01
4	3	1984.	1984.	0.999	87.2	87.0	86.9	15.69	0.66	0.327	618.4	2268.	210.03	2.5	3.75	329.	2.054	180.-0.29E-01
5	3	2135.	2135.	0.999	78.3	76.8	76.7	14.59	0.75	0.338	665.4	1930.	156.87	2.5	3.75	305.	1.991	180.-0.29E-01
6	3	2163.	2163.	0.999	76.2	74.2	74.1	14.34	0.77	0.341	669.9	1358.	107.44	2.5	3.90	302.	1.991	180.-0.29E-01
7	3	2254.	2254.	0.998	71.0	68.7	68.6	13.73	0.83	0.358	700.7	840.	61.87	2.5	3.62	281.	1.897	180.-0.30E-01
8	3	2411.	2411.	0.992	63.5	61.3	61.2	13.04	0.93	0.421	755.6	518.	34.22	2.5	3.27	251.	1.785	180.-0.30E-01
9	3	2459.	2459.	0.933	57.4	55.4	55.3	11.98	1.03	0.447	778.7	178.	10.70	2.5	2.87	221.	1.694	180.-0.29E-01

390.7	PRESS.= 28.73	PS= -0.2	FSWIR= 0.892	S.R.T= 4.498	SUM.H.REJ=-.223E+02	137.01	C.59	0.266	193.4	1366.	1132.	-0.24E+00
TOTAL		0.904				137.01	C.59	0.266	193.4	1366.	1132.	-0.24E+00
1	1	776.	143.3	103.0	102.9	10.91	C.03	0.319	563.0	2554.	281.31	-0.26E+00
2	3	1784.	106.1	99.2	99.1	17.75	C.58	0.321	569.0	2415.	254.13	179.-0.27E-01
3	3	1817.	101.7	89.2	89.1	16.75	C.65	0.325	601.5	2231.	210.12	180.-0.26E-01
4	3	1932.	90.7	89.2	89.1	16.75	C.65	0.325	601.5	2231.	210.12	180.-0.26E-01
5	3	2077.	70.8	78.3	78.2	15.37	C.75	0.336	647.1	1895.	157.06	180.-0.27E-01
6	3	2096.	78.3	76.2	76.1	15.37	C.75	0.336	647.1	1895.	157.06	180.-0.27E-01
7	3	2190.	74.2	71.0	70.9	14.76	C.80	0.346	674.7	822.	62.47	180.-0.28E-01
8	3	2347.	65.6	63.5	63.4	14.13	C.90	0.393	729.6	544.	37.07	180.-0.28E-01
9	3	2434.	59.4	57.4	57.3	13.22	1.00	0.456	767.2	227.	14.07	180.-0.27E-01
392.7	PRESS.= 26.82	PS= 0.3	FSWIR= 0.892	S.R.T= 4.376	SUM.H.REJ=-.232E+02	145.62	C.59	0.265	187.9	1371.	1136.	-0.21E+00
TOTAL		0.907				145.62	C.59	0.265	187.9	1371.	1136.	-0.21E+00
1	1	755.	127.1	106.1	105.9	10.16	C.03	0.317	543.1	2480.	281.48	-0.22E+00
2	3	1722.	109.3	101.3	101.2	18.96	C.57	0.320	554.3	2378.	254.2	180.-0.24E-01
3	3	1771.	102.9	90.7	90.6	17.89	C.64	0.324	585.2	2194.	210.21	180.-0.24E-01
4	3	1882.	92.3	81.4	81.3	16.79	C.72	0.331	627.4	1861.	157.13	180.-0.25E-01
5	3	2021.	81.4	75.8	75.7	16.40	C.73	0.332	625.4	1293.	107.88	180.-0.24E-01
6	3	2031.	80.4	73.2	73.1	15.86	C.78	0.338	650.1	802.	62.77	180.-0.25E-01
7	3	2109.	75.4	73.2	73.1	15.86	C.78	0.338	650.1	802.	62.77	180.-0.25E-01
8	3	2274.	67.7	65.6	65.5	15.24	C.87	0.370	701.8	546.	38.42	180.-0.26E-01
9	3	2392.	61.4	59.4	59.3	14.48	C.96	0.433	748.4	266.	16.98	180.-0.25E-01
394.7	PRESS.= 24.87	PS= 0.8	FSWIR= 0.891	S.R.T= 4.267	SUM.H.REJ=-.239E+02	154.57	C.59	0.264	182.7	1374.	1139.	-0.18E+00
TOTAL		0.909				154.57	C.59	0.264	182.7	1374.	1139.	-0.18E+00
1	1	735.	111.3	109.3	109.2	21.19	C.03	0.316	524.6	2412.	281.65	-0.18E+00
2	3	1664.	112.4	102.9	102.8	20.23	C.56	0.318	545.3	2343.	254.21	180.-0.22E-01
3	3	1726.	104.5	92.3	92.2	19.11	C.63	0.323	565.3	2158.	210.30	180.-0.22E-01
4	3	1833.	91.8	81.4	81.3	17.95	C.71	0.329	609.4	1828.	157.28	180.-0.23E-01
5	3	1956.	81.4	75.8	75.7	16.40	C.73	0.332	625.4	1293.	107.88	180.-0.24E-01
6	3	2031.	80.4	73.2	73.1	15.86	C.78	0.338	650.1	802.	62.77	180.-0.25E-01
7	3	2109.	75.4	73.2	73.1	15.86	C.78	0.338	650.1	802.	62.77	180.-0.25E-01
8	3	2282.	67.7	65.6	65.5	15.24	C.87	0.370	701.8	546.	38.42	180.-0.26E-01
9	3	2344.	61.4	59.4	59.3	14.48	C.96	0.433	748.4	266.	16.98	180.-0.25E-01
396.7	PRESS.= 23.06	PS= 1.3	FSWIR= 0.890	S.R.T= 4.170	SUM.H.REJ=-.245E+02	164.14	C.59	0.263	177.6	1376.	1140.	-0.15E+00
TOTAL		0.919				164.14	C.59	0.263	177.6	1376.	1140.	-0.15E+00
1	1	716.	94.9	112.4	112.3	22.70	C.03	0.314	507.2	2349.	281.82	-0.15E+00
2	3	1638.	115.5	104.5	104.5	21.60	C.56	0.317	526.0	2308.	254.39	180.-0.20E-01
3	3	1682.	106.1	93.8	93.8	20.41	C.62	0.321	553.9	2124.	210.38	180.-0.20E-01
4	3	1785.	84.5	82.9	82.8	17.19	C.70	0.327	591.0	1795.	157.37	180.-0.21E-01
5	3	1913.	84.5	82.9	82.8	17.19	C.70	0.327	591.0	1795.	157.37	180.-0.21E-01
6	3	1956.	84.5	82.9	82.8	17.19	C.70	0.327	591.0	1795.	157.37	180.-0.21E-01
7	3	2031.	80.4	73.2	73.1	15.86	C.78	0.338	650.1	802.	62.77	180.-0.22E-01
8	3	2109.	75.4	73.2	73.1	15.86	C.78	0.338	650.1	802.	62.77	180.-0.22E-01
9	3	2276.	67.7	65.6	65.5	15.24	C.87	0.370	701.8	546.	38.42	180.-0.23E-01
398.7	PRESS.= 21.39	PS= 1.8	FSWIR= 0.890	S.R.T= 4.084	SUM.H.REJ=-.250E+02	174.02	C.59	0.262	172.7	1377.	1140.	-0.13E+00
TOTAL		0.929				174.02	C.59	0.262	172.7	1377.	1140.	-0.13E+00
1	1	697.	73.0	115.5	115.4	24.29	C.03	0.313	490.9	2270.	281.99	-0.13E+00
2	3	1566.	115.5	104.5	104.5	23.03	C.55	0.316	517.5	2240.	254.48	180.-0.18E-01
3	3	1640.	106.1	95.4	95.3	21.78	C.61	0.320	539.1	2030.	210.47	180.-0.18E-01
4	3	1730.	97.0	84.5	84.4	20.50	C.68	0.325	575.2	1753.	157.46	180.-0.19E-01
5	3	1851.	84.5	82.9	82.8	17.19	C.70	0.327	591.0	1795.	157.37	180.-0.19E-01
6	3	1951.	84.5	82.9	82.8	17.19	C.70	0.327	591.0	1795.	157.37	180.-0.19E-01
7	3	2031.	80.4	73.2	73.1	15.86	C.78	0.338	650.1	802.	62.77	180.-0.20E-01
8	3	2109.	75.4	73.2	73.1	15.86	C.78	0.338	650.1	802.	62.77	180.-0.20E-01
9	3	2237.	67.7	65.6	65.5	15.24	C.87	0.370	701.8	546.	38.42	180.-0.21E-01
400.7	PRESS.= 19.86	PS= 2.2	FSWIR= 0.889	S.R.T= 4.007	SUM.H.REJ=-.255E+02	184.29	C.59	0.261	168.1	1377.	1141.	-0.11E+00
TOTAL		0.939				184.29	C.59	0.261	168.1	1377.	1141.	-0.11E+00
1	1	680.	63.2	118.6	118.4	25.96	C.03	0.311	475.5	2235.	282.15	-0.11E+00
2	3	1507.	121.6	107.8	107.7	24.53	C.49	0.315	490.5	2241.	254.57	180.-0.17E-01
3	3	1599.	109.4	97.0	96.9	23.22	C.60	0.319	524.9	2057.	210.56	180.-0.17E-01
4	3	1605.	98.6	84.5	84.4	20.50	C.68	0.325	575.2	1753.	157.46	180.-0.17E-01

5	3	1813.	1813.	6.999	97.6	86.0	85.9	21.97	0.67	0.324	559.2	1733.	157.54	2.5	4.04	394.	2.203	180.-0.17E-01
6	3	1747.	1751.	6.999	88.4	86.4	86.3	21.67	0.67	0.323	549.1	1180.	108.35	2.5	4.33	370.	2.193	180.-0.17E-01
7	3	1851.	1853.	6.999	84.1	82.0	81.9	20.97	0.70	0.326	565.4	725.	63.33	2.5	4.09	350.	2.121	180.-0.18E-01
8	3	1999.	1999.	6.999	76.0	73.9	73.8	20.28	0.77	0.333	606.4	504.	39.71	2.5	3.73	319.	2.011	180.-0.18E-01
9	3	2133.	2133.	6.999	69.1	67.2	67.1	19.67	0.85	0.349	652.0	293.	21.03	2.5	3.32	290.	1.916	180.-0.19E-01

EXPANSION PROCESS IS CALCULATED AS ONE ELEMENT

PRESSURE = 15.88 BATA
 AV. TEMPERATURE = 1463.0K DEG
 AV. EQUI. RATIO = 0.590
 AV. ENTHALPY = 515.11 CAL/G
 TOTAL MASS = 0.70786

EXHAUST NOX

NOX CONCEN. = 1377.00 PPM
 TOTAL MASS = 0.173E-01 G

TIME SEC	P ATA	T K	V CM**3	WGRK PS	CYL.MAS G	HEAT TRANSFER CAL/A	FSHR	S-RT *RPM
402.7	19.47	1536.	195.	2.53	0.798	-0.500E+00	-0.275E+02	0.888
404.7	17.20	1509.	276.	3.04	0.798	-0.470E+00	-0.204E+02	0.887
406.7	16.04	1503.	217.	3.43	0.798	-0.443E+00	-0.312E+02	0.887
408.7	14.99	1559.	229.	3.81	0.798	-0.419E+00	-0.328E+02	0.886
410.7	14.03	1534.	261.	4.17	0.798	-0.396E+00	-0.344E+02	0.885
412.7	13.15	1511.	253.	4.51	0.798	-0.376E+00	-0.359E+02	0.885
414.7	12.36	1486.	265.	4.83	0.798	-0.357E+00	-0.373E+02	0.884
416.7	11.63	1468.	278.	5.14	0.798	-0.342E+00	-0.387E+02	0.883
418.7	10.95	1448.	291.	5.43	0.798	-0.324E+00	-0.400E+02	0.883
420.7	10.35	1423.	304.	5.71	0.798	-0.310E+00	-0.412E+02	0.882
422.7	9.79	1410.	317.	5.98	0.798	-0.297E+00	-0.424E+02	0.881
424.7	9.28	1392.	330.	6.23	0.798	-0.284E+00	-0.436E+02	0.881
426.7	8.81	1375.	344.	6.47	0.798	-0.273E+00	-0.447E+02	0.880
428.7	8.38	1359.	357.	6.70	0.798	-0.263E+00	-0.457E+02	0.880
430.7	7.98	1341.	371.	6.91	0.798	-0.253E+00	-0.467E+02	0.879
432.7	7.61	1324.	384.	7.12	0.798	-0.244E+00	-0.477E+02	0.879
434.7	7.27	1314.	398.	7.31	0.798	-0.235E+00	-0.486E+02	0.878
436.7	6.95	1300.	412.	7.50	0.798	-0.228E+00	-0.495E+02	0.877
438.7	6.66	1286.	425.	7.67	0.798	-0.220E+00	-0.504E+02	0.877
440.7	6.39	1274.	439.	7.84	0.798	-0.213E+00	-0.513E+02	0.876
442.7	6.14	1261.	452.	8.00	0.798	-0.207E+00	-0.521E+02	0.876
444.7	5.91	1250.	466.	8.15	0.798	-0.201E+00	-0.529E+02	0.875
446.7	5.69	1238.	479.	8.29	0.798	-0.196E+00	-0.537E+02	0.875
448.7	5.48	1227.	492.	8.42	0.798	-0.190E+00	-0.545E+02	0.874
450.7	5.30	1217.	505.	8.55	0.798	-0.185E+00	-0.552E+02	0.874
452.7	5.13	1207.	519.	8.67	0.798	-0.181E+00	-0.559E+02	0.873
454.7	4.96	1197.	531.	8.79	0.798	-0.176E+00	-0.566E+02	0.873
456.7	4.81	1189.	544.	8.90	0.798	-0.172E+00	-0.573E+02	0.872
458.7	4.67	1179.	556.	9.00	0.798	-0.169E+00	-0.580E+02	0.872
460.7	4.53	1170.	568.	9.10	0.798	-0.164E+00	-0.586E+02	0.871
462.7	4.41	1162.	580.	9.19	0.798	-0.161E+00	-0.593E+02	0.871
464.7	4.29	1154.	593.	9.28	0.798	-0.157E+00	-0.599E+02	0.870
466.7	4.14	1147.	603.	9.36	0.798	-0.155E+00	-0.605E+02	0.870
468.7	4.04	1139.	612.	9.44	0.798	-0.152E+00	-0.611E+02	0.869
470.7	3.92	1132.	624.	9.51	0.798	-0.149E+00	-0.617E+02	0.869
472.7	3.83	1126.	637.	9.59	0.798	-0.146E+00	-0.623E+02	0.868
474.7	3.61	1116.	647.	9.65	0.798	-0.144E+00	-0.629E+02	0.868
476.7	3.73	1113.	657.	9.71	0.798	-0.141E+00	-0.635E+02	0.867
478.7	3.65	1107.	667.	9.77	0.798	-0.139E+00	-0.640E+02	0.867
480.7	3.61	1103.	673.	9.81	0.798	-0.137E+00	-0.644E+02	0.866

EXHAUST VALVE OPEN

OUTPUT DATA		P ATA	T K	V CM**3	WCRK PS	CYL. MAS G	HEAT TRANSFER		AEFE CM**2	GWE G/S
TIME DEC	DATA						CAL/A	CAL		
482.0	3.54	1098.	683.	9.96	9.96	C.798	-0.127E+00	-0.649E+02	0.00	-0.06
484.0	3.48	1092.	692.	9.91	9.91	C.798	-0.125E+00	-0.654E+02	0.01	-0.18
486.0	3.42	1087.	701.	9.96	9.96	C.798	-0.123E+00	-0.659E+02	0.01	-0.30
488.0	3.36	1082.	709.	10.01	10.01	C.798	-0.121E+00	-0.663E+02	0.01	-0.42
490.0	3.31	1078.	718.	10.05	10.05	C.798	-0.120E+00	-0.668E+02	0.01	-0.53
492.0	3.26	1073.	725.	10.09	10.09	C.797	-0.119E+00	-0.673E+02	0.02	-0.63
494.0	3.21	1069.	733.	10.13	10.13	C.797	-0.117E+00	-0.678E+02	0.02	-0.74
496.0	3.16	1065.	740.	10.16	10.16	C.797	-0.115E+00	-0.682E+02	0.05	-1.15
498.0	3.12	1062.	747.	10.20	10.20	C.797	-0.114E+00	-0.687E+02	0.09	-2.69
500.0	3.08	1056.	754.	10.23	10.23	C.796	-0.113E+00	-0.691E+02	0.13	-4.30
502.0	3.04	1052.	760.	10.26	10.26	C.795	-0.111E+00	-0.696E+02	0.17	-5.87
504.0	3.00	1045.	766.	10.28	10.28	C.794	-0.110E+00	-0.700E+02	0.22	-7.47
506.0	2.96	1045.	772.	10.31	10.31	C.792	-0.108E+00	-0.705E+02	0.47	-12.25
508.0	2.91	1042.	777.	10.33	10.33	C.788	-0.107E+00	-0.709E+02	0.78	-23.11
510.0	2.86	1035.	782.	10.35	10.35	C.782	-0.105E+00	-0.713E+02	1.09	-33.92
512.0	2.80	1029.	787.	10.37	10.37	C.775	-0.103E+00	-0.717E+02	1.39	-44.31
514.0	2.73	1023.	791.	10.39	10.39	C.766	-0.100E+00	-0.721E+02	1.70	-54.22
516.0	2.65	1017.	795.	10.40	10.40	C.755	-0.097E+00	-0.725E+02	2.26	-67.46
518.0	2.59	1009.	799.	10.42	10.42	C.740	-0.094E+00	-0.729E+02	2.87	-85.75
520.0	2.49	1002.	803.	10.43	10.43	C.723	-0.090E+00	-0.732E+02	3.47	-102.66
522.0	2.39	996.	806.	10.44	10.44	C.703	-0.084E+00	-0.736E+02	4.08	-118.47
524.0	2.29	988.	808.	10.45	10.45	C.681	-0.081E+00	-0.739E+02	4.68	-132.14
526.0	2.17	979.	811.	10.46	10.46	C.658	-0.077E+00	-0.742E+02	5.21	-142.99
528.0	2.05	966.	813.	10.46	10.46	C.632	-0.072E+00	-0.745E+02	5.74	-151.15
530.0	1.94	949.	815.	10.46	10.46	C.606	-0.067E+00	-0.748E+02	6.27	-157.73
532.0	1.82	932.	816.	10.46	10.46	C.579	-0.061E+00	-0.751E+02	6.80	-162.68
534.0	1.70	916.	817.	10.47	10.47	C.551	-0.056E+00	-0.754E+02	7.29	-165.24
536.0	1.59	902.	818.	10.47	10.47	C.524	-0.051E+00	-0.757E+02	7.84	-162.64
538.0	1.49	892.	819.	10.47	10.47	C.498	-0.047E+00	-0.761E+02	8.32	-156.54
540.0	1.39	874.	819.	10.47	10.47	C.474	-0.042E+00	-0.765E+02	8.76	-148.26
542.0	1.31	861.	820.	10.47	10.47	C.451	-0.039E+00	-0.769E+02	9.12	-124.39
544.0	1.23	845.	820.	10.47	10.47	C.430	-0.035E+00	-0.761E+02	9.45	-107.27
546.0	1.17	828.	820.	10.47	10.47	C.412	-0.032E+00	-0.763E+02	9.72	-87.93
548.0	1.11	825.	820.	10.47	10.47	C.397	-0.030E+00	-0.764E+02	9.98	-67.28
550.0	1.07	822.	820.	10.47	10.47	C.386	-0.029E+00	-0.765E+02	10.21	-45.67
552.0	1.05	817.	820.	10.47	10.47	C.378	-0.026E+00	-0.764E+02	10.45	-22.98
554.0	1.04	814.	820.	10.47	10.47	C.375	-0.025E+00	-0.764E+02	10.61	-5.01
556.0	1.04	813.	820.	10.47	10.47	C.374	-0.025E+00	-0.764E+02	10.75	-7.20
558.0	1.04	813.	820.	10.47	10.47	C.373	-0.025E+00	-0.764E+02	10.79	-7.33
560.0	1.04	813.	820.	10.47	10.47	C.371	-0.025E+00	-0.764E+02	10.79	-7.33
562.0	1.04	813.	820.	10.47	10.47	C.370	-0.025E+00	-0.764E+02	10.79	-7.33
564.0	1.04	812.	820.	10.46	10.46	C.369	-0.025E+00	-0.764E+02	10.79	-7.33
566.0	1.04	812.	820.	10.46	10.46	C.367	-0.024E+00	-0.764E+02	10.79	-7.33
568.0	1.04	811.	820.	10.46	10.46	C.365	-0.024E+00	-0.764E+02	10.79	-7.33
570.0	1.04	811.	820.	10.46	10.46	C.363	-0.024E+00	-0.764E+02	10.79	-7.33
572.0	1.04	811.	820.	10.46	10.46	C.361	-0.024E+00	-0.764E+02	10.79	-7.33
574.0	1.04	811.	820.	10.46	10.46	C.359	-0.024E+00	-0.764E+02	10.79	-7.33
576.0	1.04	809.	820.	10.46	10.46	C.356	-0.024E+00	-0.764E+02	10.79	-7.33
578.0	1.04	809.	820.	10.46	10.46	C.354	-0.023E+00	-0.764E+02	10.79	-7.33
580.0	1.04	809.	820.	10.46	10.46	C.351	-0.023E+00	-0.764E+02	10.79	-7.33
582.0	1.04	809.	820.	10.46	10.46	C.348	-0.023E+00	-0.764E+02	10.79	-7.33
584.0	1.04	809.	820.	10.46	10.46	C.345	-0.023E+00	-0.764E+02	10.79	-7.33
586.0	1.04	807.	820.	10.46	10.46	C.342	-0.023E+00	-0.764E+02	10.79	-7.33
588.0	1.04	807.	820.	10.46	10.46	C.339	-0.022E+00	-0.764E+02	10.79	-7.33
590.0	1.04	806.	820.	10.46	10.46	C.335	-0.022E+00	-0.764E+02	10.79	-7.33
592.0	1.04	806.	820.	10.46	10.46	C.332	-0.022E+00	-0.764E+02	10.79	-7.33
594.0	1.04	806.	820.	10.46	10.46	C.328	-0.022E+00	-0.764E+02	10.79	-7.33

596.0	1.04	905.	692.	10.46	0.324	-0.220E-01	-0.787E+02	9.79	-23.09
598.0	1.04	805.	693.	10.46	0.320	-0.219E-01	-0.788E+02	9.79	-23.56
599.0	1.04	804.	673.	10.45	0.316	-0.215E-01	-0.789E+02	9.79	-24.84
600.0	1.04	804.	664.	10.45	0.312	-0.213E-01	-0.790E+02	9.79	-25.70
604.0	1.04	904.	653.	10.45	0.307	-0.210E-01	-0.790E+02	9.79	-26.55
605.0	1.04	903.	643.	10.45	0.303	-0.208E-01	-0.791E+02	9.79	-27.39
608.0	1.04	903.	633.	10.45	0.298	-0.205E-01	-0.792E+02	9.79	-28.22
610.0	1.04	902.	622.	10.45	0.293	-0.202E-01	-0.793E+02	9.79	-29.03
612.0	1.05	902.	611.	10.45	0.288	-0.199E-01	-0.794E+02	9.79	-29.82
614.0	1.05	902.	599.	10.45	0.283	-0.197E-01	-0.795E+02	9.79	-30.59
616.0	1.05	901.	588.	10.45	0.278	-0.194E-01	-0.795E+02	9.79	-31.35
618.0	1.05	901.	576.	10.44	0.273	-0.191E-01	-0.796E+02	9.79	-32.07
620.0	1.05	900.	564.	10.44	0.267	-0.188E-01	-0.797E+02	9.79	-32.77
622.0	1.05	800.	551.	10.44	0.262	-0.185E-01	-0.798E+02	9.79	-33.45
624.0	1.05	800.	539.	10.44	0.256	-0.182E-01	-0.798E+02	9.79	-34.09
626.0	1.05	799.	526.	10.44	0.250	-0.179E-01	-0.799E+02	9.79	-34.70
628.0	1.05	799.	513.	10.44	0.244	-0.176E-01	-0.800E+02	9.79	-35.27
630.0	1.05	798.	500.	10.44	0.238	-0.172E-01	-0.800E+02	9.79	-35.80
632.0	1.05	798.	487.	10.44	0.232	-0.169E-01	-0.801E+02	9.79	-36.29
634.0	1.05	797.	474.	10.43	0.226	-0.166E-01	-0.802E+02	9.79	-36.74
636.0	1.05	797.	461.	10.43	0.220	-0.163E-01	-0.802E+02	9.79	-37.14
638.0	1.05	795.	447.	10.43	0.214	-0.160E-01	-0.803E+02	9.79	-37.49
640.0	1.05	795.	434.	10.43	0.207	-0.156E-01	-0.804E+02	9.79	-37.78
642.0	1.05	795.	420.	10.43	0.201	-0.153E-01	-0.804E+02	9.79	-38.03
644.0	1.05	794.	406.	10.42	0.195	-0.150E-01	-0.805E+02	9.79	-38.21
646.0	1.05	794.	393.	10.42	0.188	-0.146E-01	-0.805E+02	9.79	-38.34
648.0	1.05	793.	380.	10.42	0.182	-0.143E-01	-0.806E+02	9.79	-38.41
650.0	1.05	793.	366.	10.42	0.176	-0.140E-01	-0.807E+02	9.79	-38.41
652.0	1.05	792.	352.	10.42	0.169	-0.137E-01	-0.807E+02	9.79	-38.21
654.0	1.05	792.	339.	10.42	0.163	-0.133E-01	-0.808E+02	9.79	-38.21
656.0	1.05	792.	325.	10.42	0.156	-0.130E-01	-0.808E+02	9.79	-38.01
658.0	1.05	791.	312.	10.42	0.150	-0.126E-01	-0.809E+02	9.75	-37.70
660.0	1.05	790.	299.	10.41	0.144	-0.124E-01	-0.809E+02	9.72	-37.35
662.0	1.05	790.	286.	10.41	0.138	-0.121E-01	-0.810E+02	9.61	-36.59
664.0	1.05	789.	273.	10.41	0.132	-0.118E-01	-0.810E+02	9.45	-36.26
666.0	1.05	789.	261.	10.41	0.126	-0.115E-01	-0.811E+02	9.28	-35.72
668.0	1.05	788.	248.	10.41	0.120	-0.112E-01	-0.811E+02	9.12	-35.13
670.0	1.05	787.	236.	10.41	0.114	-0.109E-01	-0.811E+02	8.96	-34.48
672.0	1.05	786.	224.	10.41	0.109	-0.106E-01	-0.812E+02	8.66	-33.61
674.0	1.05	785.	211.	10.40	0.103	-0.104E-01	-0.812E+02	8.32	-32.69
676.0	1.05	785.	200.	10.40	0.098	-0.101E-01	-0.813E+02	7.98	-31.83
678.0	1.05	784.	191.	10.40	0.093	-0.098E-01	-0.813E+02	7.64	-30.92
680.0	1.05	784.	180.	10.40	0.088	-0.096E-01	-0.813E+02	7.29	-29.55
682.0	1.05	783.	170.	10.40	0.083	-0.094E-01	-0.814E+02	6.80	-28.74
684.0	1.05	782.	161.	10.40	0.078	-0.092E-01	-0.814E+02	6.27	-27.49
686.0	1.05	782.	151.	10.40	0.074	-0.090E-01	-0.815E+02	5.74	-26.28
688.0	1.05	782.	142.	10.40	0.070	-0.089E-01	-0.815E+02	5.21	-25.02
690.0	1.05	781.	134.	10.39	0.066	-0.087E-01	-0.815E+02	4.58	-23.69
692.0	1.05	781.	125.	10.39	0.062	-0.085E-01	-0.816E+02	4.08	-22.16
694.0	1.05	781.	118.	10.39	0.059	-0.083E-01	-0.816E+02	3.47	-20.51
696.0	1.05	781.	111.	10.39	0.055	-0.081E-01	-0.816E+02	2.87	-18.75
698.0	1.05	781.	105.	10.39	0.053	-0.080E-01	-0.817E+02	2.26	-16.70
700.0	1.10	782.	99.	10.39	0.050	-0.078E-01	-0.817E+02	1.70	-14.46
702.0	1.12	782.	94.	10.39	0.048	-0.077E-01	-0.817E+02	1.39	-12.87
704.0	1.13	785.	89.	10.39	0.046	-0.076E-01	-0.818E+02	1.07	-11.41
706.0	1.15	787.	84.	10.38	0.045	-0.075E-01	-0.818E+02	0.78	-9.41
708.0	1.18	792.	81.	10.38	0.044	-0.074E-01	-0.818E+02	0.47	-6.94
710.0	1.22	793.	77.	10.38	0.043	-0.073E-01	-0.819E+02	0.22	-4.02

EXHAUST TEMPERATURE= 911.9KCEG

*SECTION OF THE FRICTION LOSS**

WISC AND PUMPS= 77.6425/CM**2

GAV BEAR = 101.3100/CM**2

BEARING = 140.8450/CM**2

PLUMPY = 43.481G/CM**2
 VISCOS PISTON = 366.137G/CM**2
 RING TENSION = 115.044G/CM**2
 RING GAS PRESS = 7.335G/CM**2

 TOTAL LOSS = 851.814G/CM**2

PIMLP= -67.65G/CM**2 PSIA= -0.11HP
 PEMEP= 345.07G/CM**2 PSEX= 0.57HP
 AIMEP= 6240.0G/CM**2 IP= 10.38HP AISFC= 171.64G/HP.HR
 BMEP= 5188.0G/CM**2 BHP= 8.96HP BSFC= 198.78G/8HP.HR

HEAT REJECTION= CAL/MIN
 TOTAL H. RCJ =0.8189E+05
 CYL. LINER =0.2251E+05
 PISTON TOP =0.1673E+05
 PISTON CUP =0.2094E+05
 CYL. FRAC =0.1617E+05
 INT. VALVE =0.7223E+04
 EXH. VALVE =0.1322E+04

HEAT REJ./FUEL = 0.277

PEAK CYL PRESS= 52.9AT367.5DEG. CA